

-8-

Therefore, there is no validity to Ford's claim about a lack of a detergent resulting in an unrepresentative baseline for emission measurements. —

Photographs of the fuel injectors removed from cars D-3 and D-4 illustrate the absence of fuel injector deposits (Attachment 3). As illustrated, at the end of 50,000 miles of operation none of the injectors have significant deposits in the pintle area. The black specks depicted on injectors D-3 (#1) and D-4 (#6) are probably carbon residue which broke away from the edge area.

The absence of intake valve deposits is depicted in the photographs of Car C-6 (Attachment 4). This vehicle had operated a total of 75,000 miles. As illustrated, the level of deposits is very low and not unlike that of a high quality detergent gasoline. For comparison purposes, a photo is provided of the intake valves from a test using a commercial gasoline containing a detergent.

Regarding the lack of light duty truck data, existing LDT standards are much higher than passenger vehicles (Table V). Although we do not have data from a truck, we do have the high speed vehicle data which indicates no plugging and good conversion efficiency in a close-coupled system with a relatively large engine.

TABLE V

U.S. Emission Standards

Light-Duty Truck

(gm/mi)

<u>Year</u>	<u>HC</u>	<u>CO</u>	<u>NOx</u>
Post-1985	0.8	10.0	2.3

IV. Ford Comments on HiTEC 3000 HC Effect

Ford has questioned why the adverse effects of HC emissions that were demonstrated in studies conducted in the late 1970's with 1/8 and 1/16 gm Mn/US gallon are not so readily apparent in the most recent Ethyl test program at 1/32 gm Mn/gallon.

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It is a well known fact that since 1978 emission control and engine management technology has dramatically improved. Since the 1978 studies were completed, automobile emission control systems have been equipped with three-way catalytic converters. The three-way catalytic converter combined with lambda closed-loop control is the most effective pollutant-reduction system presently available.²⁰ The evolution from open loop carburetor systems to closed loop electronic fuel injection systems has greatly reduced the variability in air/fuel ratio.

The chemistry of the exhaust gas is most appropriate to reactions at the point of stoichiometry.²¹ A prerequisite is that the air-fuel mixture supplied to the engine, and thereby the exhaust is at the stoichiometric ratio.

The improvement in emission control technology is apparent when the average hydrocarbon conversion efficiency of the catalytic converters from the 1978 CRC data is compared to the recently submitted Ethyl fleet data. At 50,000 miles the HC conversion efficiency of the CRC data averaged approximately 77 percent compared to 85.9 percent for the Ethyl fleet.

The overall improvement in tailpipe emissions is further substantiated by the decrease in average in-use hydrocarbon emission levels. The EPA has reported average HC emissions of approximately 2.5 gm/mile in the 1977-79 era, and approximately 0.7 gm/mile in the 1980-82 period.²² General Motors has reported continued improvements in their fleet from 0.67 gm/mile in 1981 to 0.28 gm/mile in 1986.

²⁰Automotive Electric/Electronic Systems, Robert Bosch.

²¹Developments in Emission Control Technology for Vehicles: A Challenge for Catalysts, The Science of the Total Environment, 93 (1990). See Figure 8, p. 236.

²²U.S. Light Duty Vehicle Fleet Emissions Performance and the Emissions Impact of Technology Changes, SAE Paper 881681.

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In SAE paper 881682, General Motors states that the reasons for the improvement were:

Improved fuel metering mainly due to increased use of fuel injection;

Improvements in the high mileage performance of catalytic converters;

Continuous improvement in control algorithms, strategies, and calibrations, and;

Improved system and component reliability.²³

Because of these vast improvements in emission control technologies, the emission results of studies conducted on vehicles equipped with outdated technology are not relevant to this discussion.

V. Ford Comments on NOx Reduction

Ford states "There appears to be no definitive explanation for the NOx reduction," but acknowledges that Mn_3O_4 does coat the interior of the exhaust system and that Mn_3O_4 does "indeed have the ability to catalytically decompose NOx." The only statement they offer to refute the assertion by Ethyl that Mn_3O_4 is responsible for the NOx reduction is "Catalytic decomposition of NOx by Mn_3O_4 is known to be too slow to be practical at the NOx levels found in automotive exhaust." Ethyl's explanation for the NOx reduction is supported, however, by a Japanese patent abstract²⁴ which states "The title active catalyst consists of a monolithic catalyst support coated with an activated Al_2O_3 contg. Co [cobalt] oxide and Mn oxide ...". This particular invention showed the following automobile exhaust conversion:

²³GM's In-use Emission Performance Past, Present, Future, SAE Paper 881682.

²⁴Exhaust Gas Treatment Catalyst Containing Cobalt and Manganese Oxides, Japanese Patent 63185453, August 1, 1988.

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<u>Co-Catalyst</u>	<u>Catalyst</u>	<u>Pollutant Conversion %</u>		
		HC	CO	NOx
Mn, Co, Al	Pt, Rh	60	92	98
Al	Pt, Rh	24	79	65

This result shows that combinations of Mn_3O_4 can affect improvements of NOx conversion (in this case 33 percent better). In a second Japanese patent²⁵, manganese is claimed as one of a list of metallic salts (which would be reduced to the oxide during calcining) that promote increased NOx removal. A third Japanese patent²⁶ also claims Manganese as a catalytic agent exhibiting enhanced NOx removal.

Ethyl's waiver request included a report from Dr. Roy Harrison which stated that the reaction temperatures and residence times in automobile exhaust systems were of the right order of magnitude to convert NOx. This information, together with the patent information noted above, clearly shows that the catalytic properties of Mn_3O_4 plausibly explains the reduction in NOx emissions observed in the Ethyl test program.

VI. Chrysler Comments on Catalyst Plugging

Relying on very limited and only partially documented information from current catalytic converters and pre-1981 SAE papers, Chrysler claims the use of HiTEC 3000 will cause catalyst plugging. Chrysler quotes SAE Papers 770655 and 780004 as relevant to catalyst plugging. As noted in response to Ford's comments, these studies were conducted on vehicles with outdated emission control systems, and at a dosage level for the additive up to 400% greater than that under consideration.

²⁵Automobile Exhaust Gas Purging Catalyst, Japanese Patent 58119343, July 15, 1983.

²⁶Automobile Exhaust Gas Purging Catalyst, Japanese Patent 59139939, August 11, 1984.

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Chrysler Canada provided Ethyl with several used catalysts removed from customer cars. These units were removed by the dealer service organizations for either noise or driveability problems if the dealer felt these units might be affecting driveability. All but a few of the catalysts were intact. These intact units would be expected to function properly and could not have been the cause of the "driveability" problem. All of the intact units have a dust coating of manganese oxide which would be expected. The amount of manganese coating varies, and differences may be due to the type of owner driving. None of these units would be considered to be "plugged." A few of the catalysts had broken or melted monoliths indicating excessive thermal stress. Manganese analysis was made on several of the units. In general the first inch of catalyst contained 1 - 5% manganese. Ethyl believes that this may be a normal range of manganese deposits for catalysts operated on the level of manganese found in Canadian gasoline.

In the Ethyl waiver submission, data are presented for a pair of close-coupled Ford Crown Victorias operated under high-speed conditions. This test was conducted to specifically address automobile industry concerns for catalyst plugging. Back pressure data on both cars remained constant at 8 psi indicating no catalyst plugging.

Chrysler submitted a quotation from the Johnson-Matthey paper, "the Effect of Fuel and Oil Additives on Automobile Catalysts."²⁷ The authors of that paper state that MMT is not expected to be used in European fuel due to adverse effects on catalysts and its toxicity in the environment. This statement is made in the absence of any of their own data and without any references to articles associated with environmental issues. In the body of the paper the authors acknowledge:

"Data generated during the Coordinating Research Council's MMT Field Test Program showed no occurrence of catalyst plugging." and

"A field test undertaken by Environment Canada has shown that 1983-85 model year cars operating on unleaded petrol containing MMT will meet the 1988 Canadian emissions standard of 0.41 g/mile hydrocarbon."²⁸

²⁷See Chrysler submission, p. 2.

²⁸The Effect of Fuel and Oil Additives on Automobile Catalyst Performance, Johnson-Matthey Platinum Metals Review, Vol. 34, No. 1, January 1990.

The study referred to in Ethyl of Canada's 1978 report, like other studies of the period, was conducted under "severe duty" engine dynamometer testing at high manganese concentrations and did not reflect current experience as shown in Ethyl's waiver application.

The Ford reference (SAE 890582) cited by Chrysler has previously been reviewed in this Appendix.

The selective data cited by Chrysler, therefore, does not refute the results of Ethyl's test program -- i.e., that HiTEC 3000 does not cause catalyst plugging at the concentration level requested in this waiver application.

VII. Chrysler Comments on HC Emissions

With respect to the Additive's impact on HC emissions, Chrysler refers to several publications from 1977.²⁹ As discussed earlier, data on vehicles from that period are not relevant to this waiver request. Since 1977, catalyst and automotive technology have improved significantly, resulting in major reductions in tailpipe emissions. Further, much of the earlier data were obtained at manganese concentrations that are 200% to 400% higher than the concentration requested in the current waiver. Thus, conclusions regarding HC emissions that are drawn from the 1977 CRC data will not be valid for current production vehicles.

Similarly, data from SAE paper 770655 and CARB staff Report 77-9-3 are based on operating 1977 automobiles using fuel containing high manganese concentrations.

²⁹Chrysler Corporation Technical Response to Environmental Protection Agency, July 20, 1990, p. 5.

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While it is important in any scientific investigation to review all existing data, it is necessary to put older data into proper context. The data from 1977 have been superceded by Ethyl's current fleet study. Ethyl's data on current model cars demonstrate that tailpipe hydrocarbon emissions from fuels containing 0.03125 gm Mn/gallon as HiTEC 3000 are nearly as low as from clear fuels.

Chrysler contends that this small difference in hydrocarbon emissions, 0.010 to 0.018 gm/mile, will present greater problems in the future when the HC emission standard is lowered to 0.25 gm/mile. As engine and emission control technology improves, it is realistic to assume that catalyst conversion efficiency also will rise, similar to that exhibited when one compares conversion efficiency data from the 1978 CRC test program to that generated by the Ethyl test program (i.e. an increase in average conversion efficiency from 77 to 85.9 percent. The small HC difference found in the current program could be reduced even more by future emission technology.

As previously discussed, Environment Canada studied the effect of HiTEC 3000 on vehicle emission systems. The working group from CGSB, which contained representatives from the Motor Vehicle Manufacturers' Association and the Automotive Importers of Canada, supported the continued use of HiTEC 3000 (MMT) as an octane enhancer. Additionally, MVMA and AIC indicated that warranty claims were no higher in Canada than in the U.S. where manganese was not used in unleaded gasoline.

VIII. U.S. Catalyst Inspections

Neither Ford nor Chrysler presented any data comparing catalyst converter durability in Canada to similar data in the U.S. to support their claims. Consequently, Ethyl conducted an informal survey of vehicle maintenance firms in Baton Rouge, Louisiana. The comments from these firms indicate that converter replacements are not uncommon in the U.S. In fact, the automobile industry acknowledged in the CGSB report that warranty claims occur about as often in the U.S. as in Canada.³⁰

The catalysts shown in Attachment 5 were removed from automobiles in consumer service by a muffler shop in Baton Rouge, Louisiana. The 40 catalysts collected from this shop, which has three outlets in Baton Rouge, were removed during period of approximately one month during 1990, from cars which had been driven more than 50,000 miles. No data on mileage, fueling, or specific malfunction was collected. The catalysts were removed because of malfunctions which were diagnosed (by the owner and/or the muffler shop, or another auto repair shop) as indicating problems with the catalyst. Typically, the car would not accelerate as it should and/or had lost the ability to operate at a reasonable speed.

³⁰Canadian General Standards Board Report, April 1986.

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Photographs of the catalytic converters are an inadequate substitute for the data generated from a controlled test program, nevertheless, they can illustrate the existence of problems in the U.S. as seen in the photographs of seven (7) of these catalysts. Photo #1 appears to be normal, Photos #3, 4 and 5 indicate various levels of plugging while Photos #2, 6 and 7 indicate varying levels of over temperature operation. These catalysts along with another 33 catalysts were selected at random. This information further confirms that the Additive does not cause catalyst plugging.

As previously mentioned, the lack of routine maintenance, misfueling, excessive oil consumption, and engine misfiring can and do cause catalyst problems. The use of the Additive does not.

IX. Conclusion

All automotive company commentators relied predominantly on research studies conducted over a decade ago on vehicles equipped with outdated emission control technology to support their concern/opposition to Ethyl's waiver application. Neither Ford nor Chrysler (who submitted most of the information) attempts to dispute directly the test results reported by Ethyl in support of its waiver application. For the reasons noted above, the studies cited by Ford and Chrysler do not refute the results of Ethyl's extensive test program. The Agency should, therefore, grant Ethyl's waiver application.

ATTACHMENT 1

ETHYL CORPORATION**INTER-OFFICE**

TO: Kevin L. Fast **ADDRESS:** FAX 202/778-2201

FROM: Ben F. Fort **ADDRESS:** BRT-6

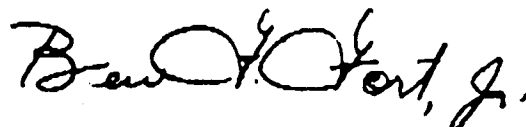
SUBJECT: Louisiana State Police **DATE:** August 7, 1990
Experience with Catalyst
Replacement

The severity of service for police vehicles is much higher than ordinary vehicle usage. In our search for examples of catalyst failure, the Louisiana State Police were contacted to determine their experience with catalyst failure.

The first contact was on June 7, 1990 with a state trooper in the research group who described several instances of exhaust system failure on cars driven 40,000 to 60,000 miles. Some of the failures were mufflers and some were catalysts. He suggested that I contact the maintenance group for additional information.

The maintenance contact told me that about nine months ago almost 400 cars with high mileage (about 60,000 to 80,000 miles) were decommissioned and sold. Unfortunately, the maintenance records are discarded when vehicles are sold. However, he related that most of those cars were '85 and '86 models, and they were replacing catalysts "right and left" after 30,000 to 40,000 miles of service. The state police use a local muffler shop to replace catalysts. A replacement program was discussed to secure police car catalysts for examination. Contact with the muffler shop revealed that catalysts are replaced frequently and not just on police vehicles. In fact, they had a "stockpile" of used catalysts currently available. The ready availability of catalysts led us to abandon the plan for additional police vehicle catalysts to concentrate on the readily available replaced catalysts. The maintenance records from the state police are available for future use and will show surprisingly high catalyst replacement rates for the new fleet now in service.

Sincerely,

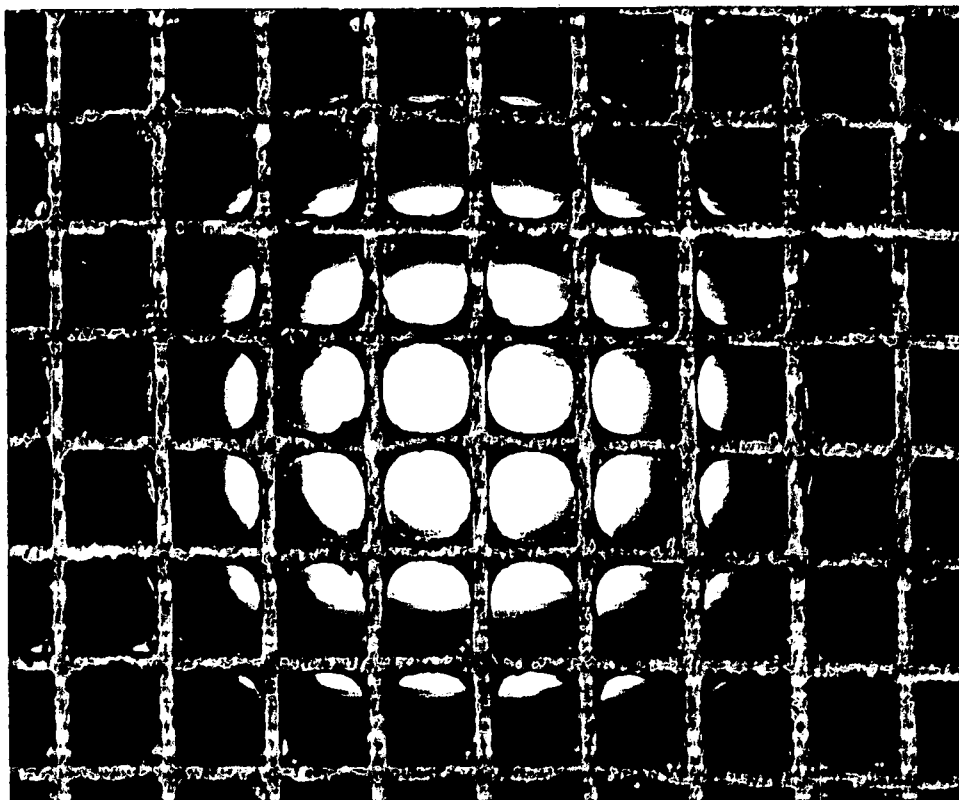


Ben F. Fort, Jr., Ph.D.
Senior Mathematics
and Statistical Associate

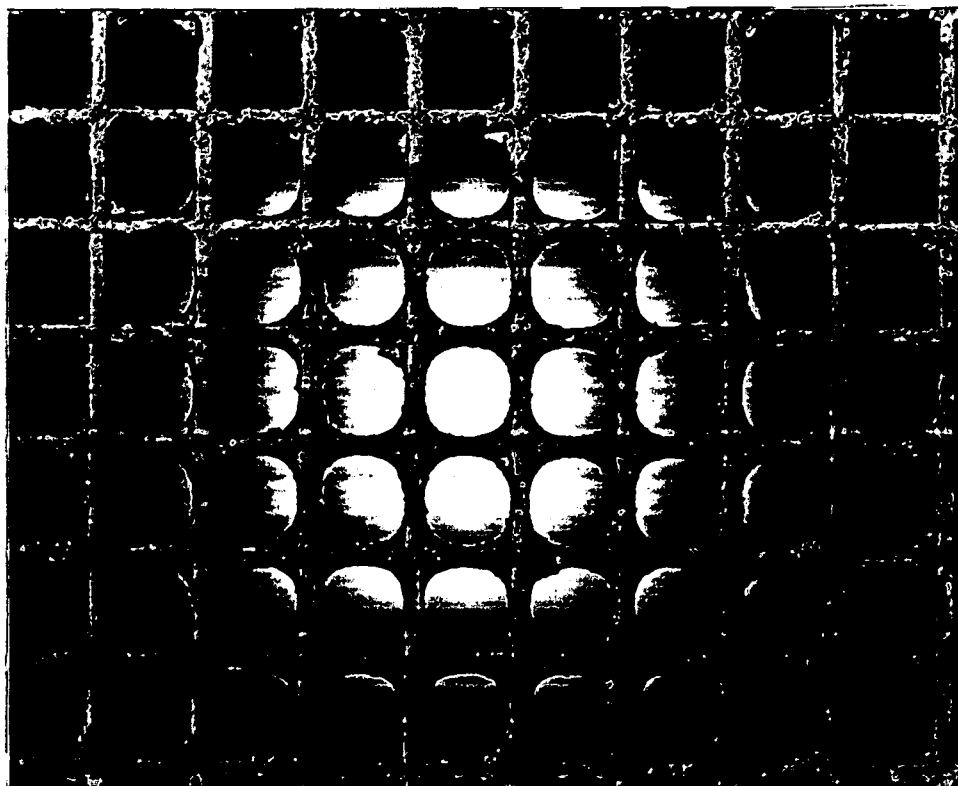
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ATTACHMENT 2

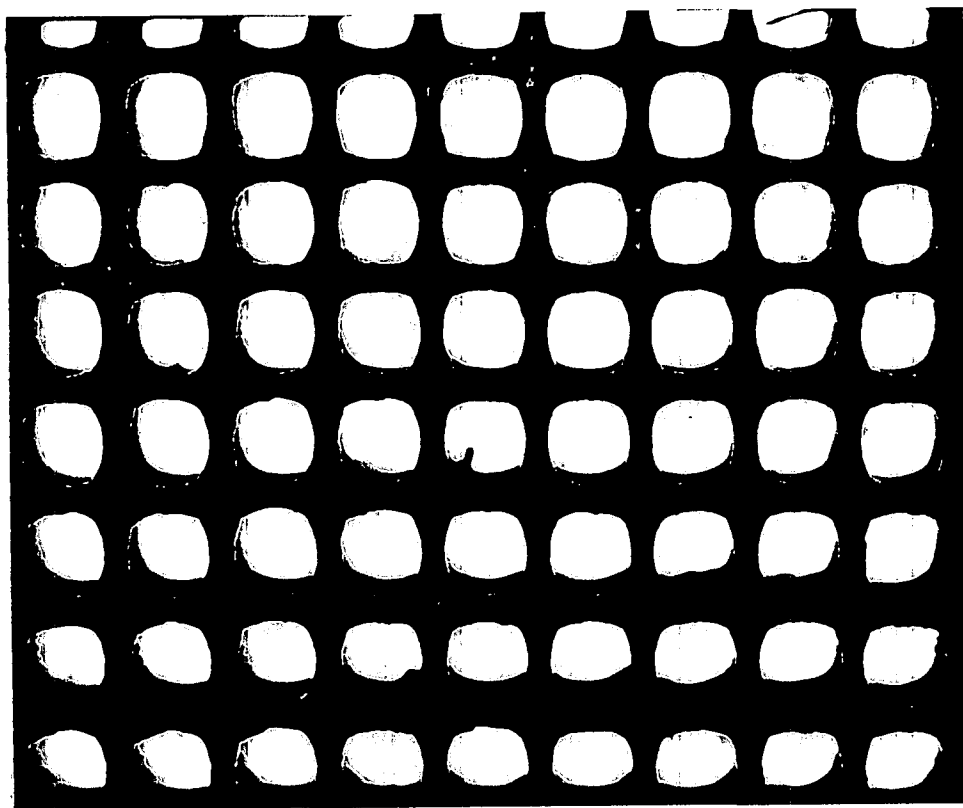
1986 3.0L FORD TAURUS
102,000 MILES
MIDDLE, 1-1/2"



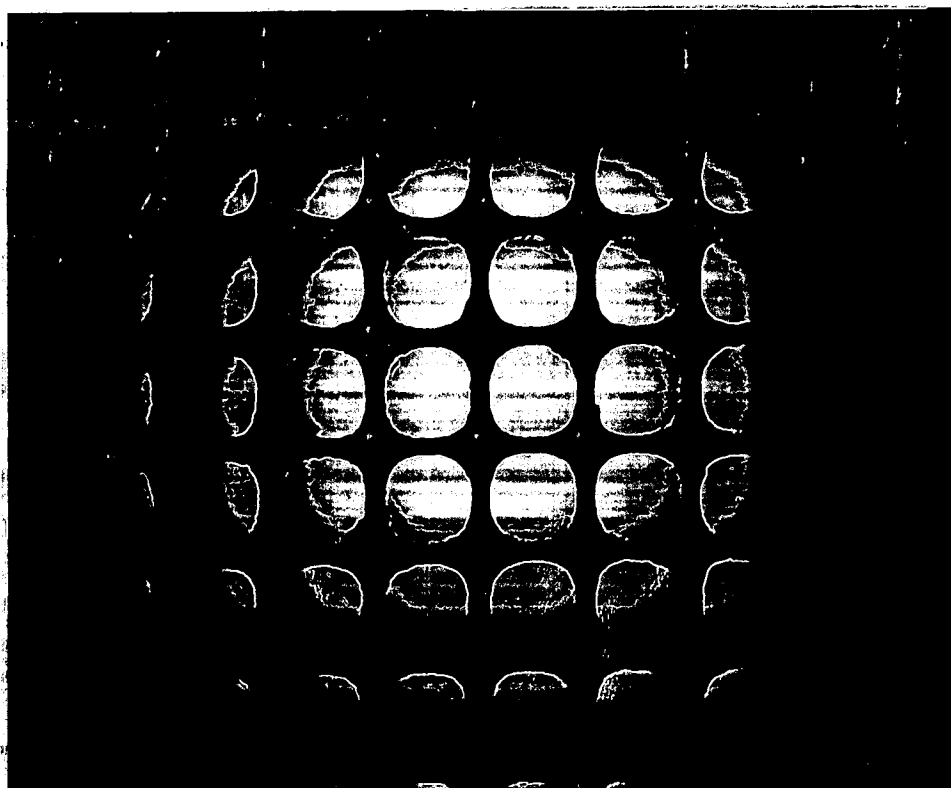
1986 3.0L FORD TAURUS
102,000 MILES
REAR, 1-1/2"



1986 3.0L FORD TAURUS
102,000 MILES
INLET FACE, FIRST 1/2"

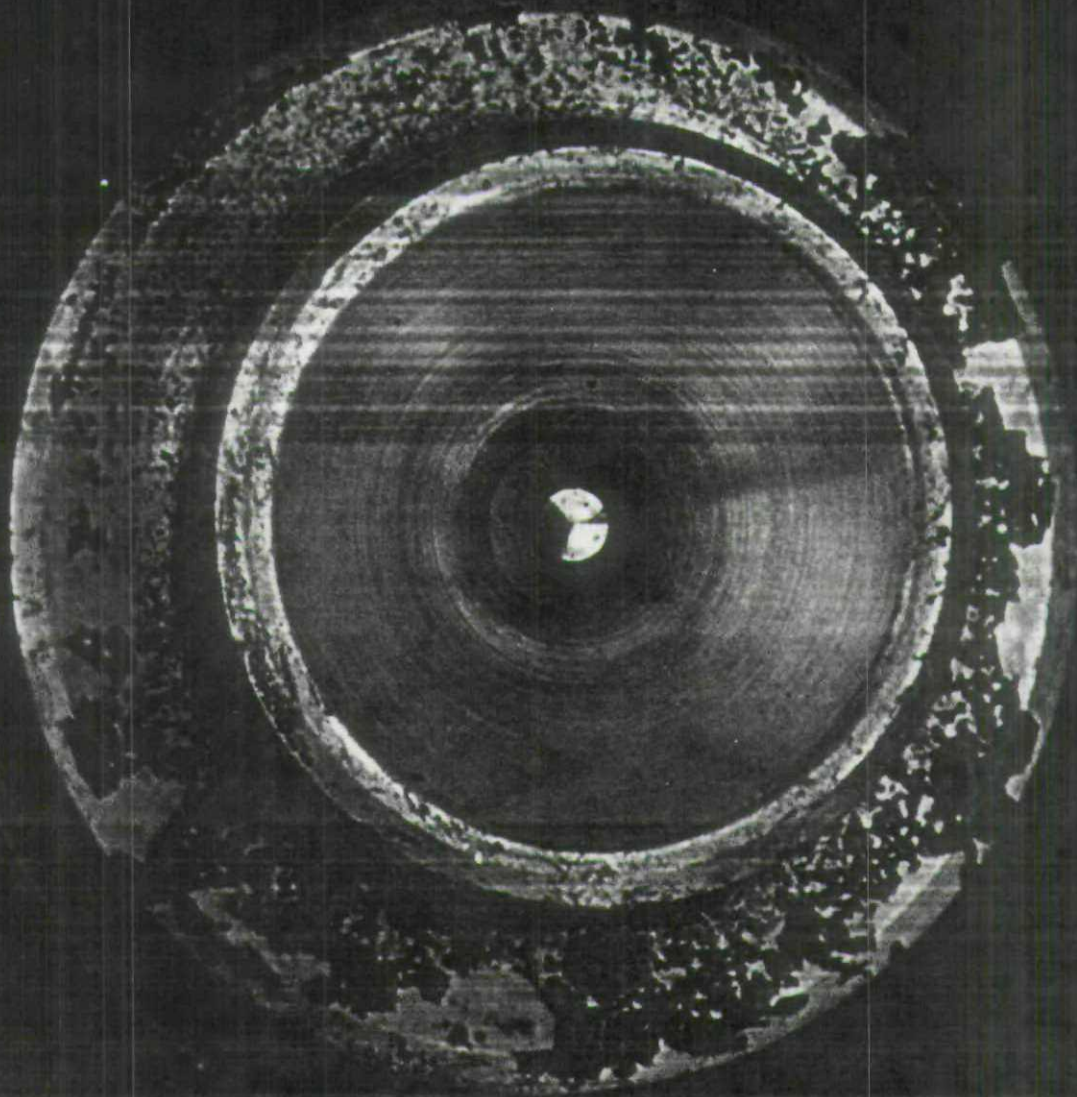


1986 3.0L FORD TAURUS
102,000 MILES
INLET, SECOND 1-1/2"

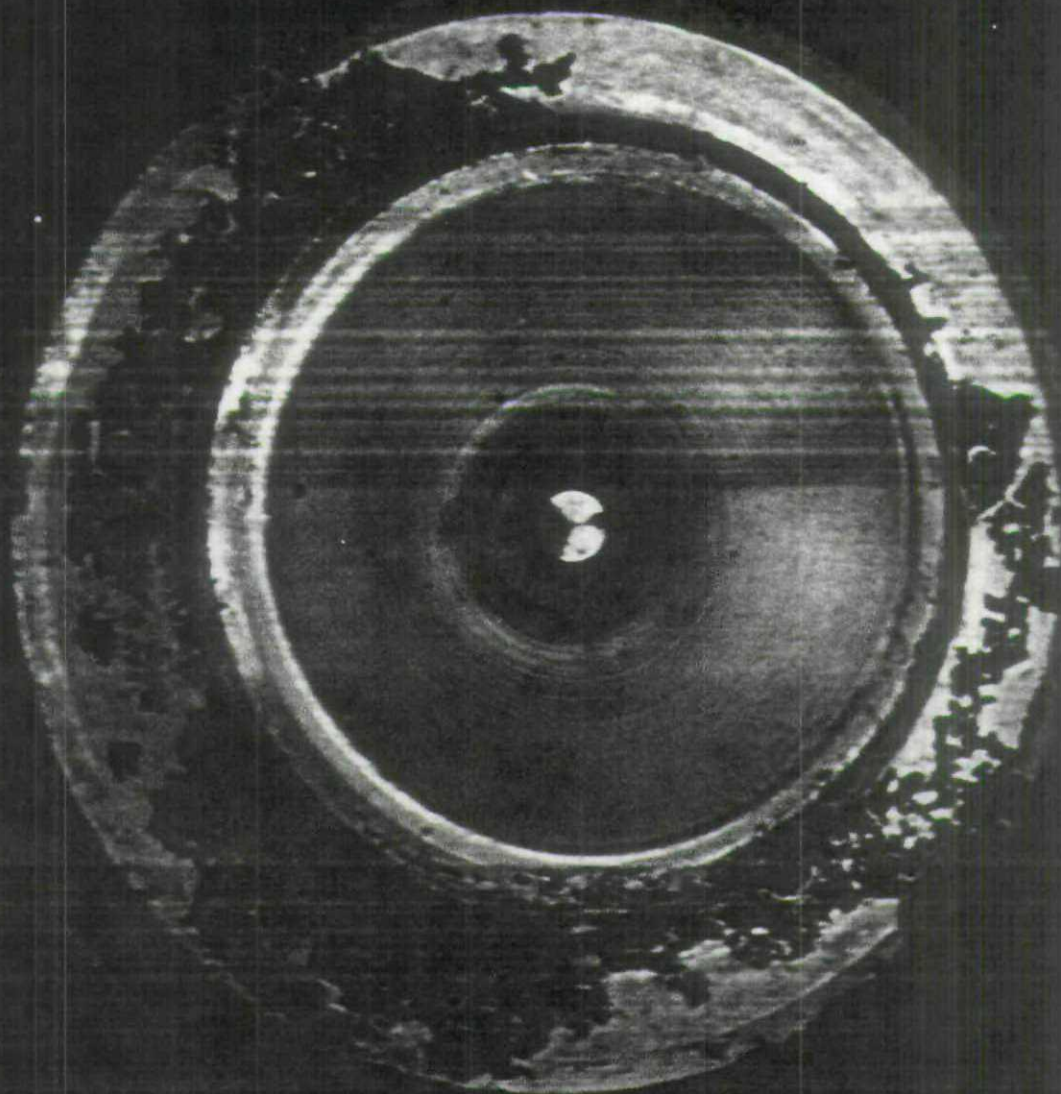


ATTACHMENT 3

CAR D-3
FUEL INJECTOR #2
50,000 MILES



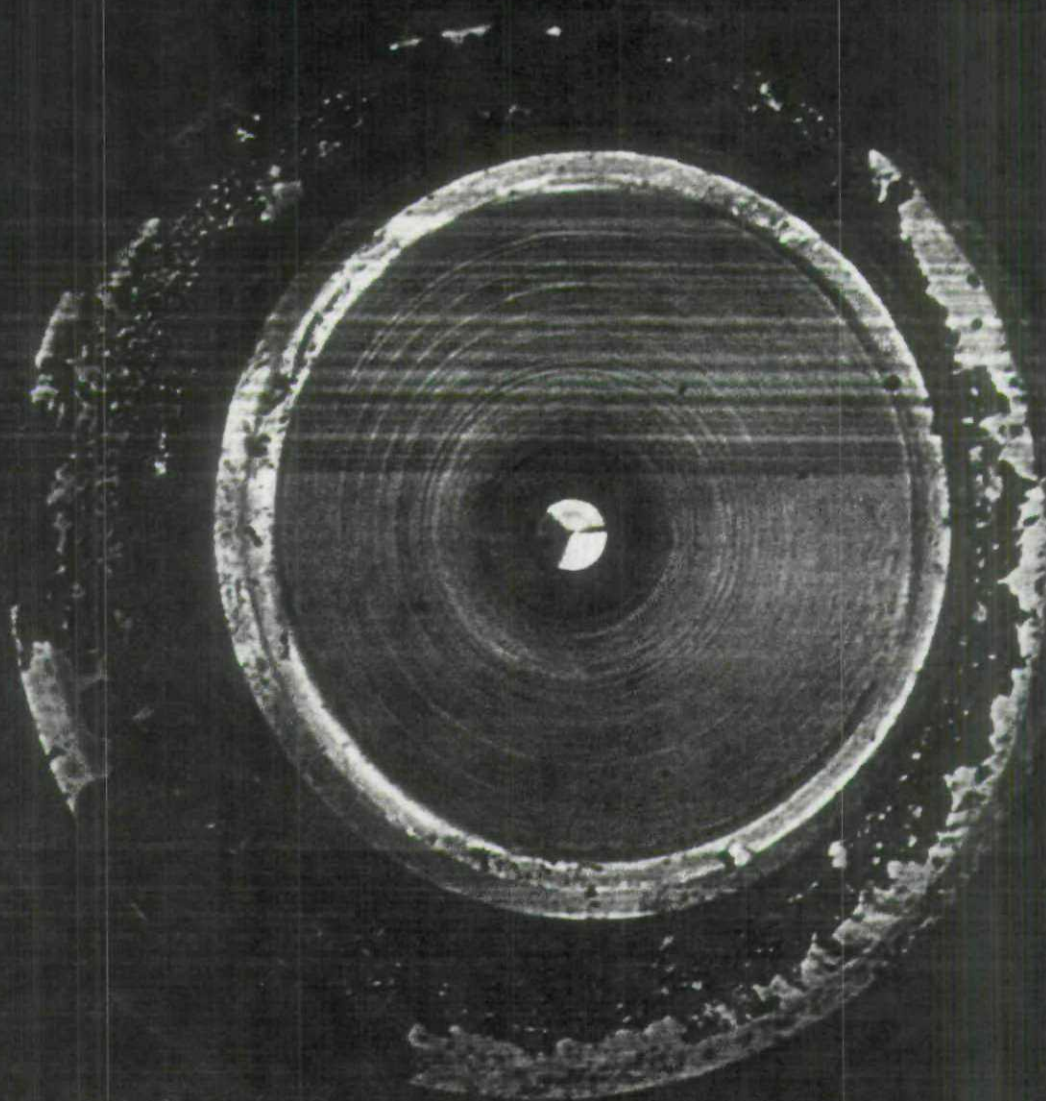
CAR D-3
FUEL INJECTOR #1
50,000 MILES



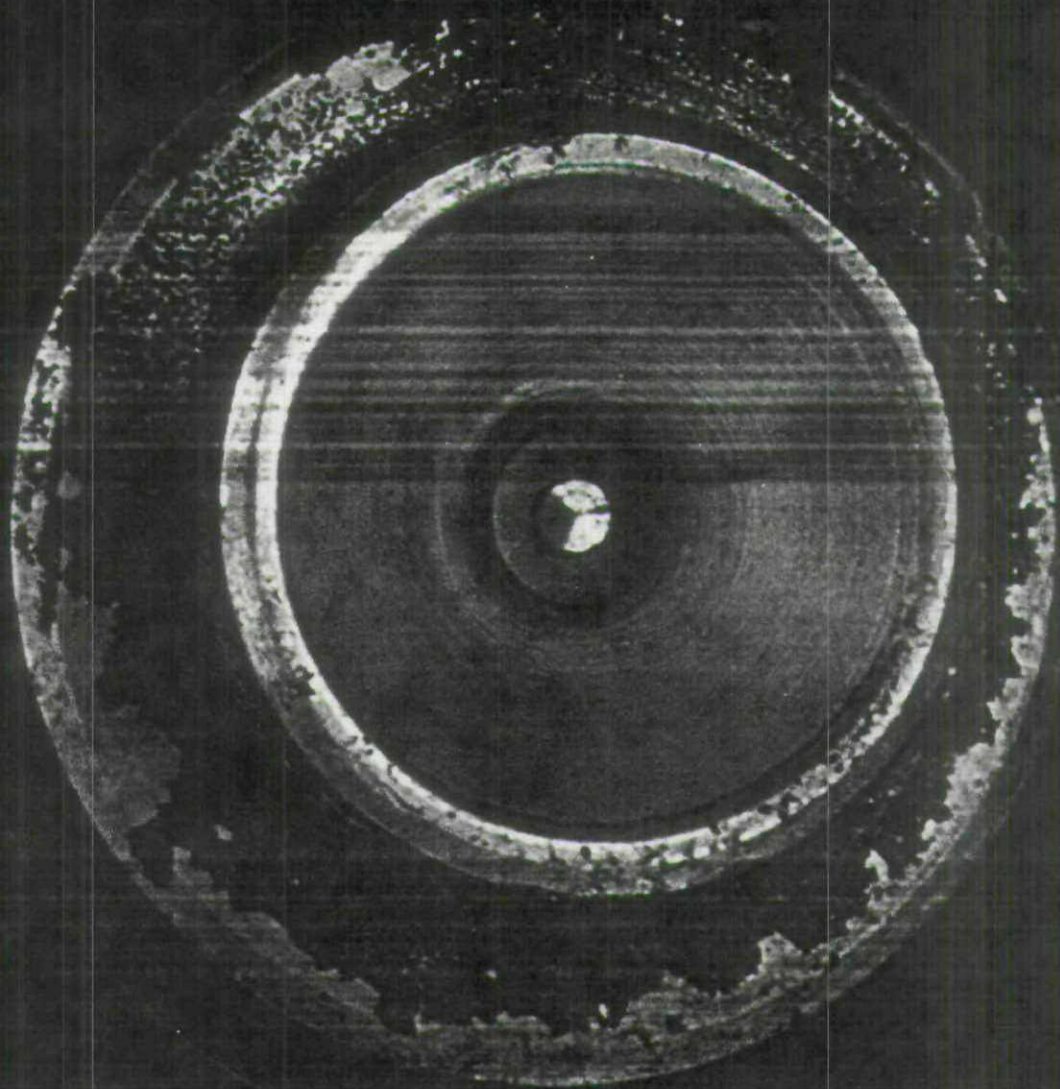
CAR D-3
FUEL INJECTOR #3
50,000 MILES



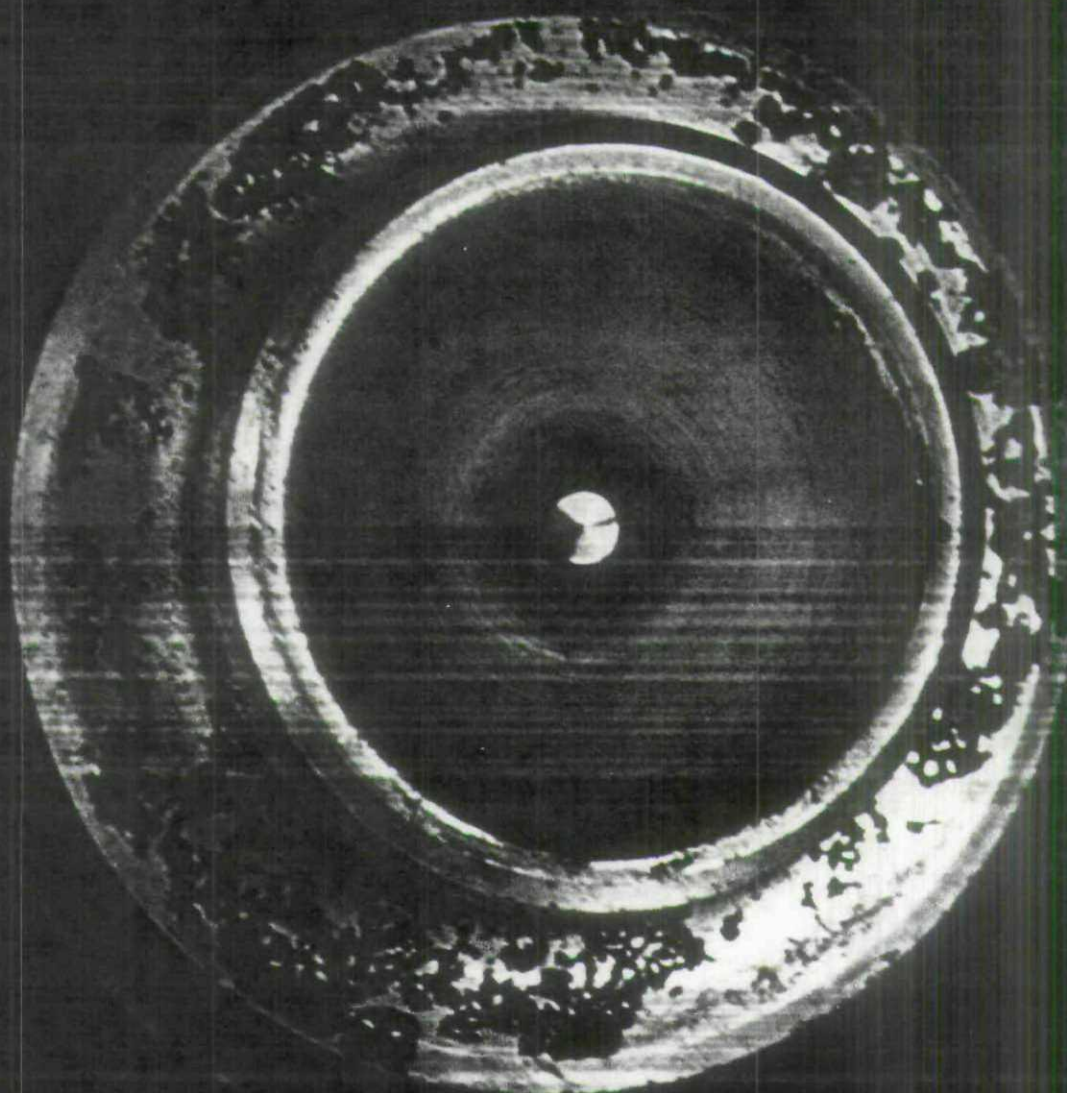
CAR D-3
FUEL INJECTOR #4
50,000 MILES



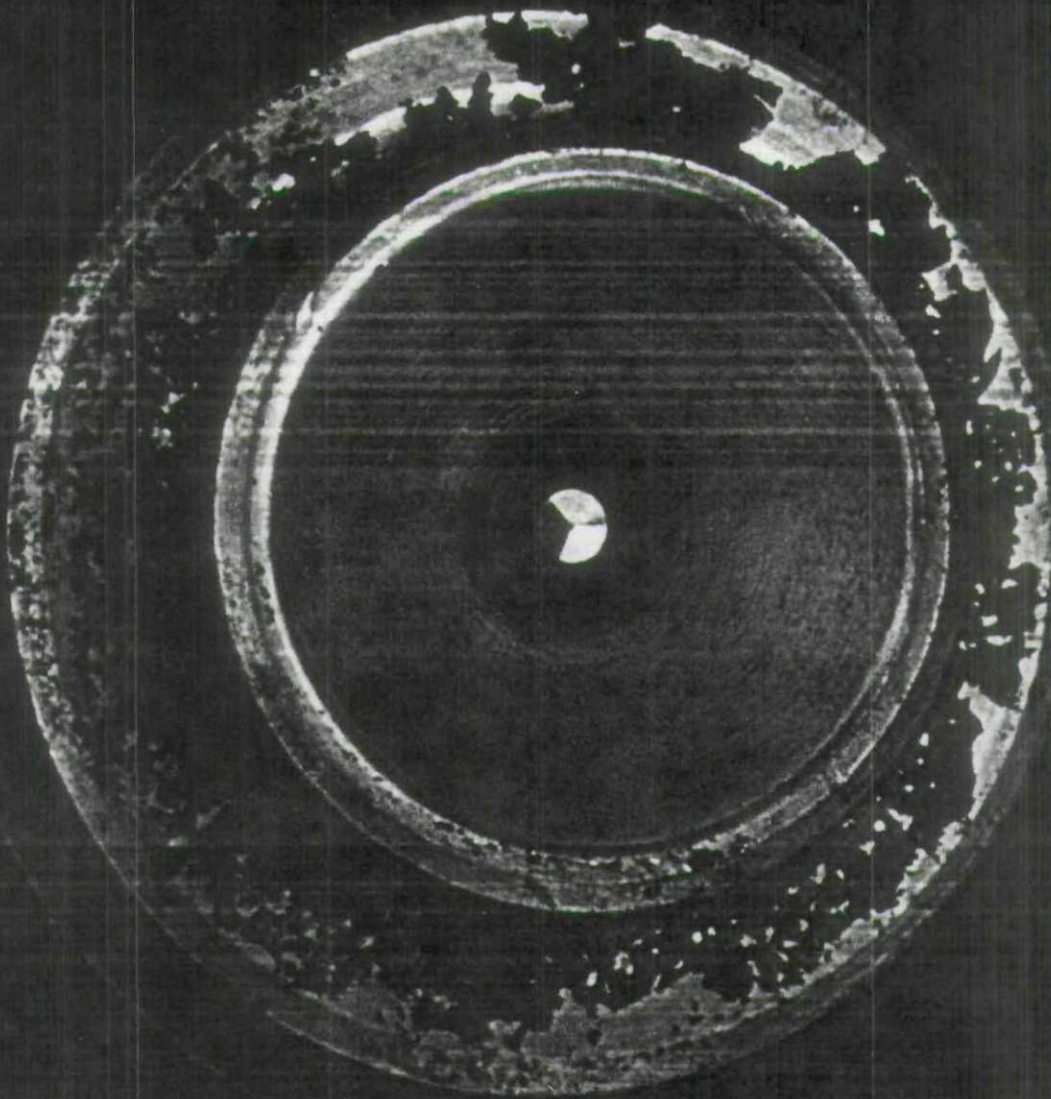
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FUEL INJECTOR #6
50,000 MILES



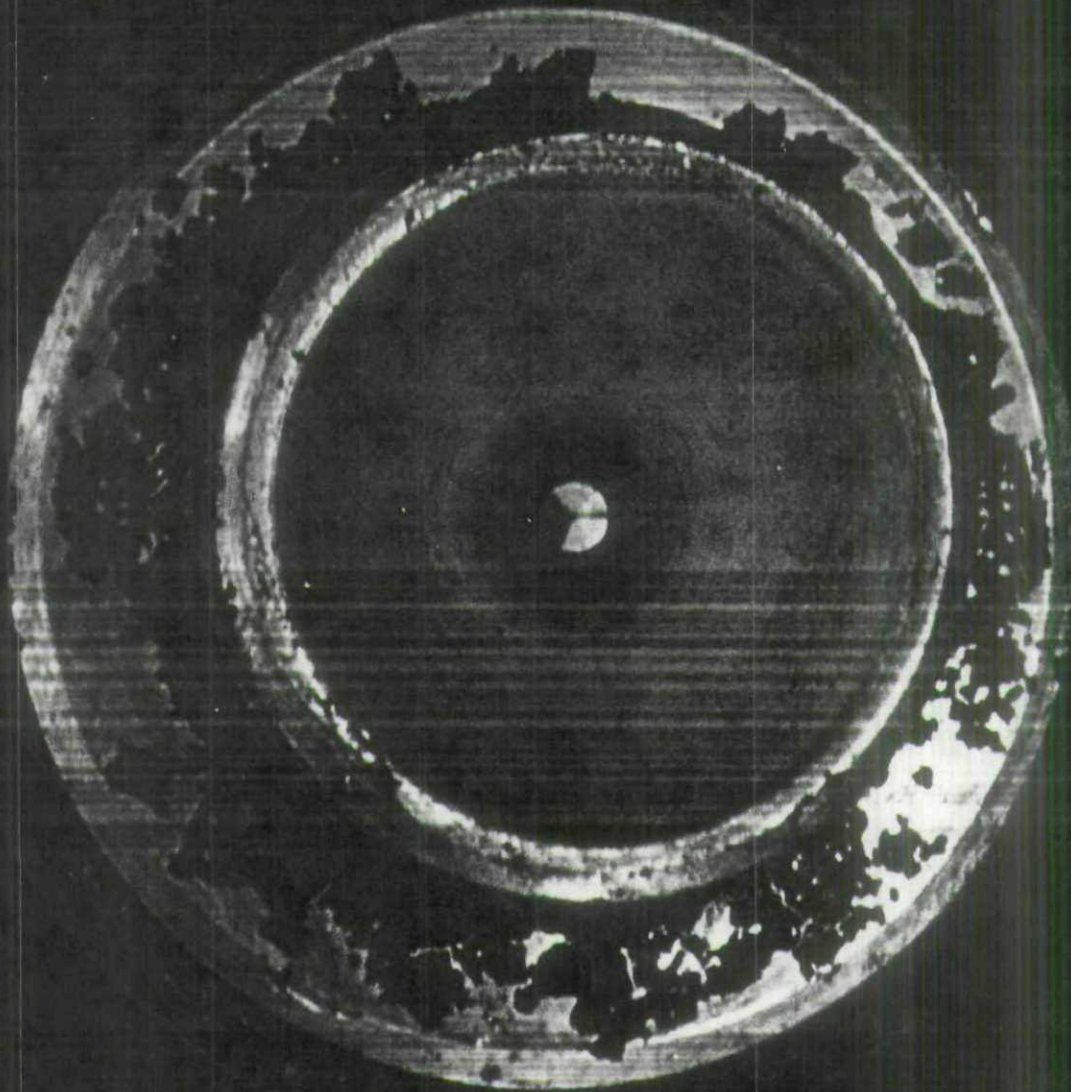
CAR D-3
FUEL INJECTOR #5
50,000 MILES



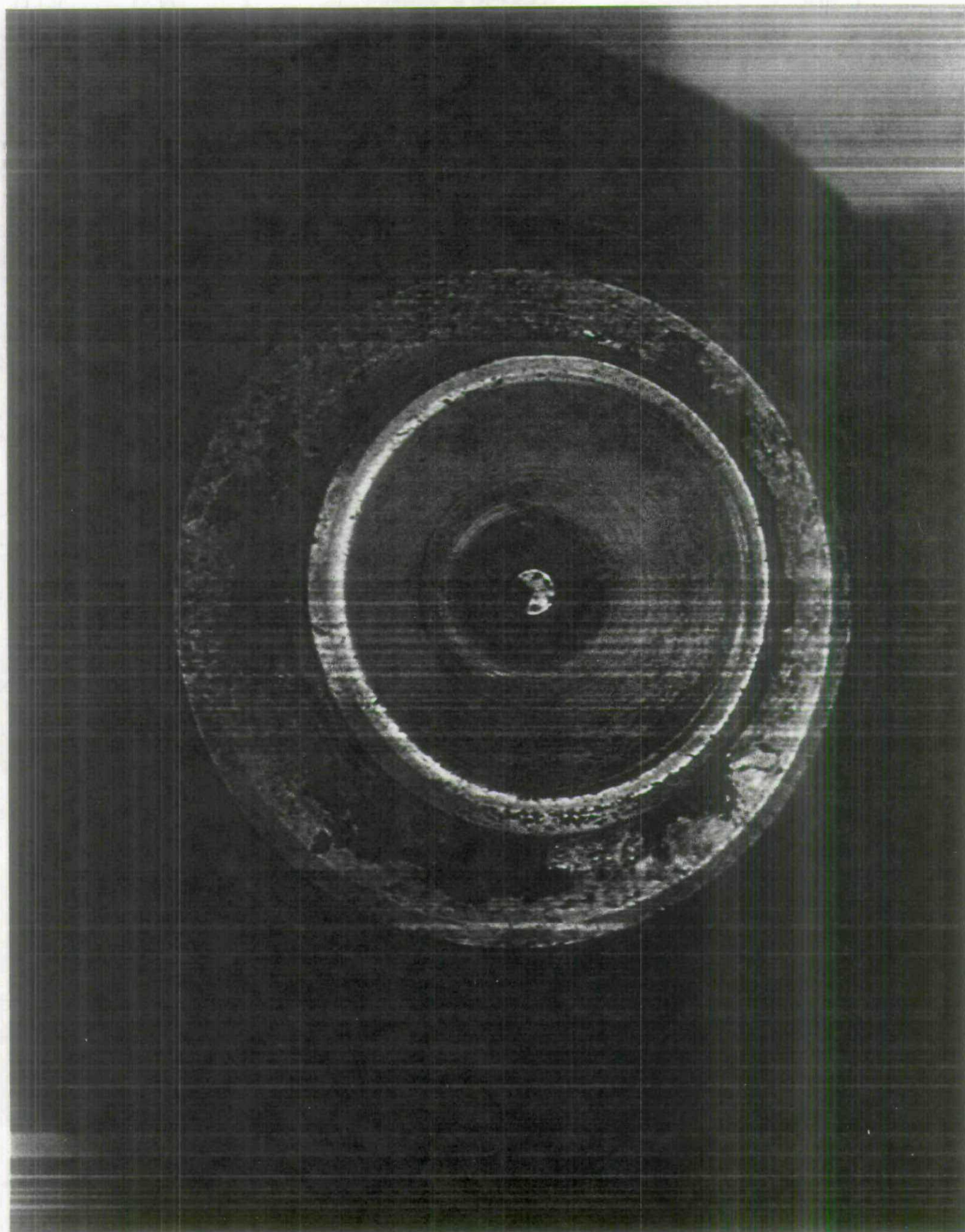
CAR D-4
FUEL INJECTOR #2
50,000 MILES



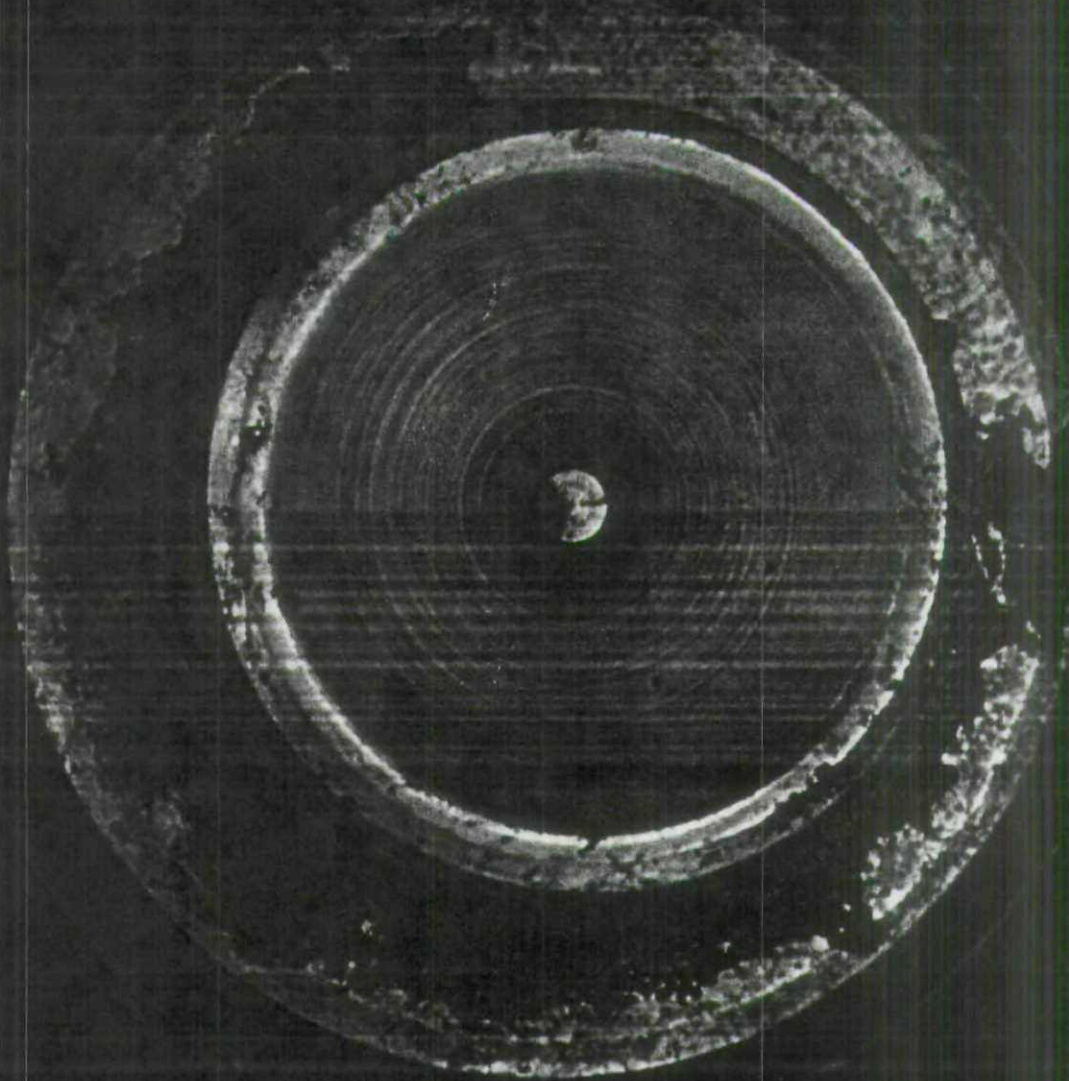
CAR D-4
FUEL INJECTOR #1
50,000 MILES



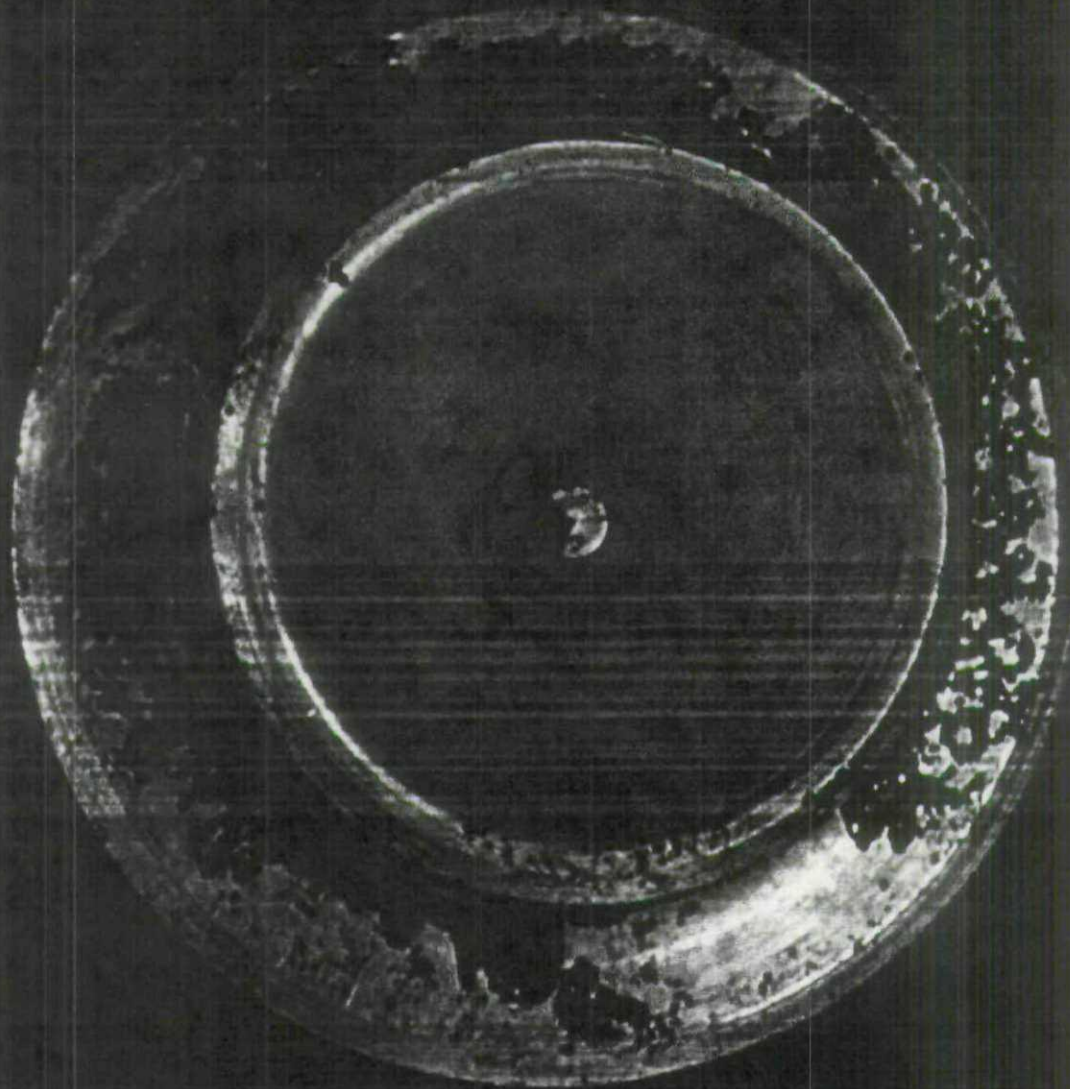
CAR D-4
FUEL INJECTOR #3
50,000 MILES



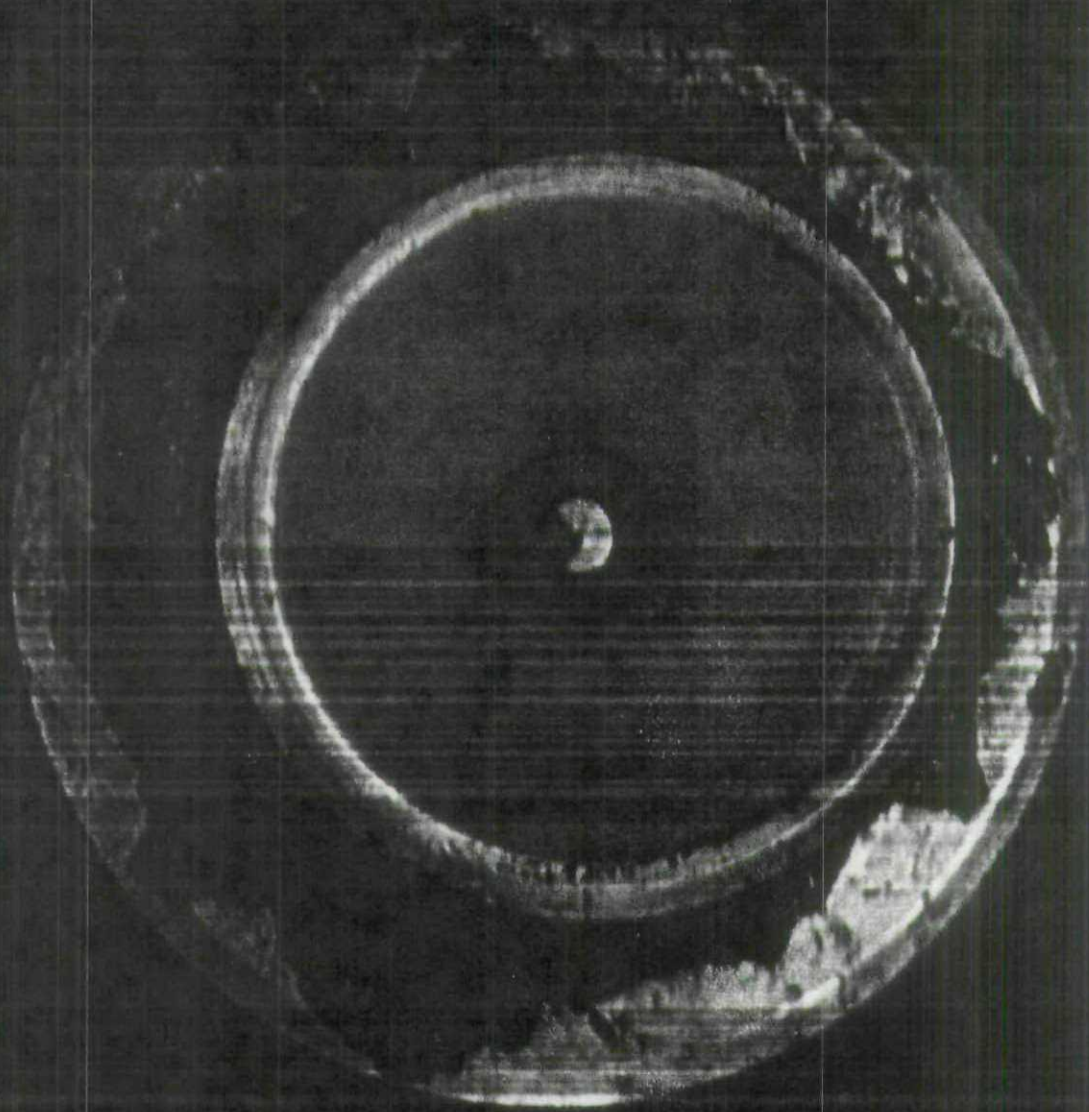
CAR D-4
FUEL INJECTOR #4
50,000 MILES



CAR D-4
FUEL INJECTOR #5
50,000 MILES

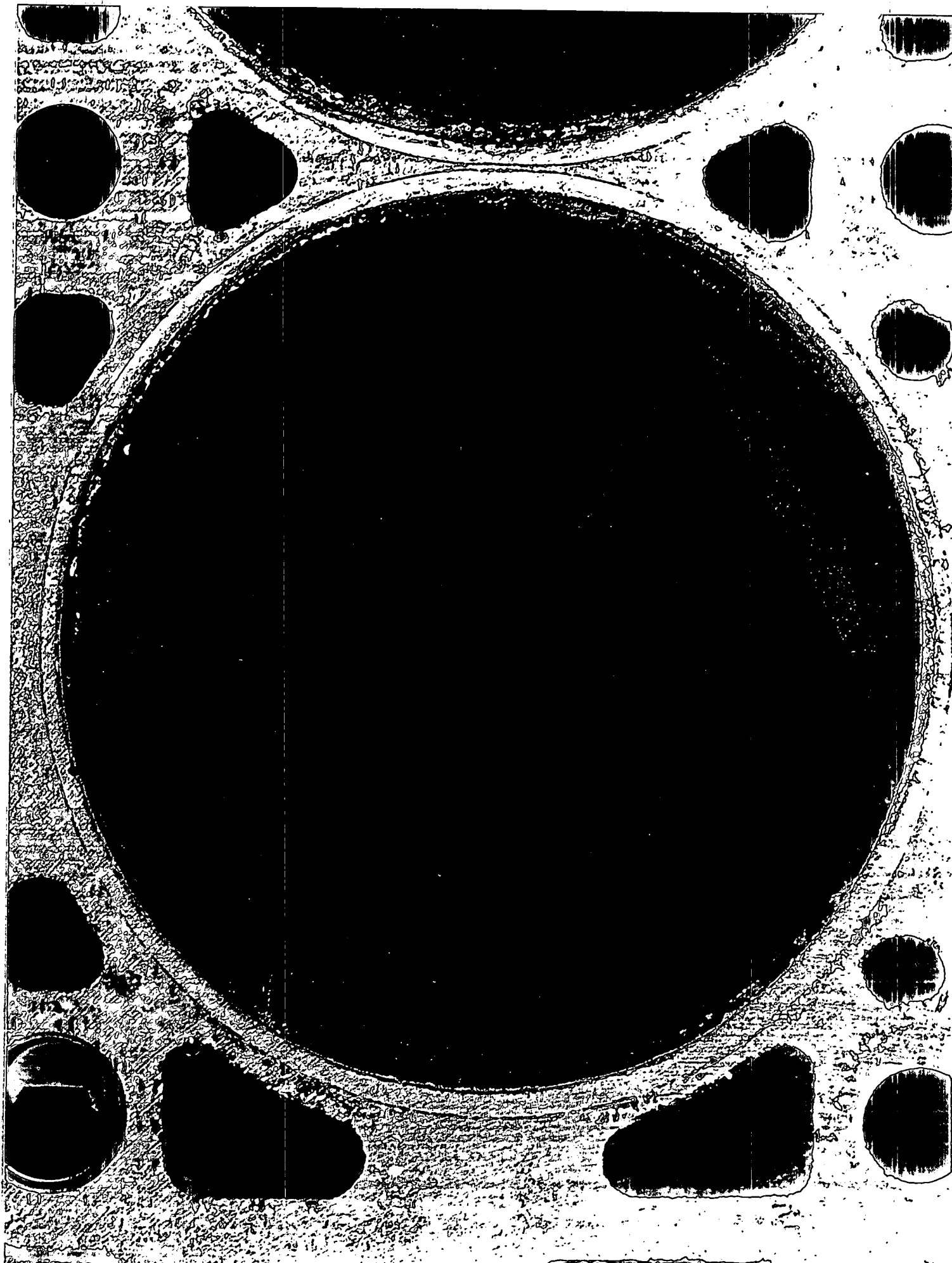


CAR D-4
FUEL INJECTOR #6
50,000 MILES

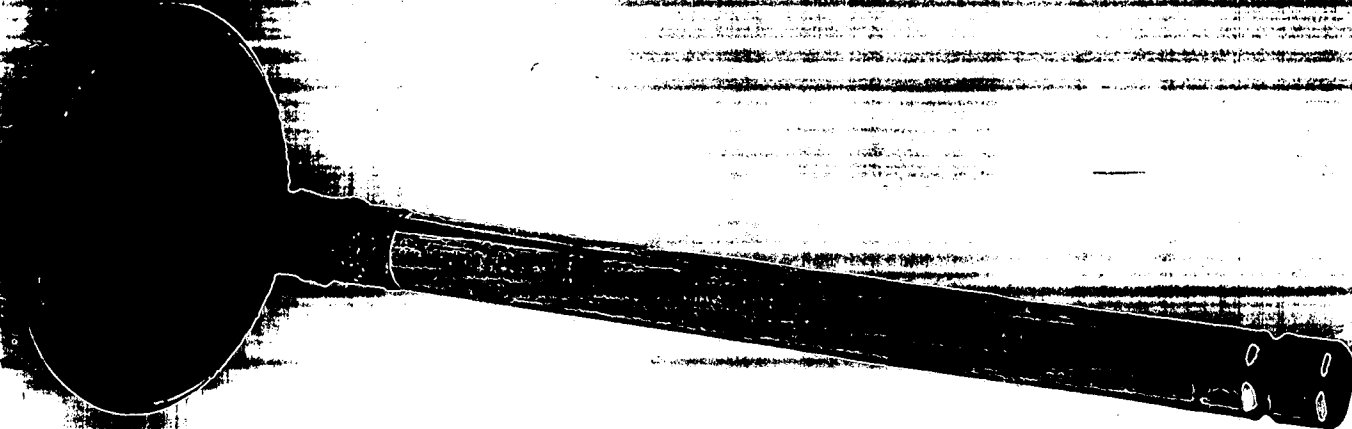
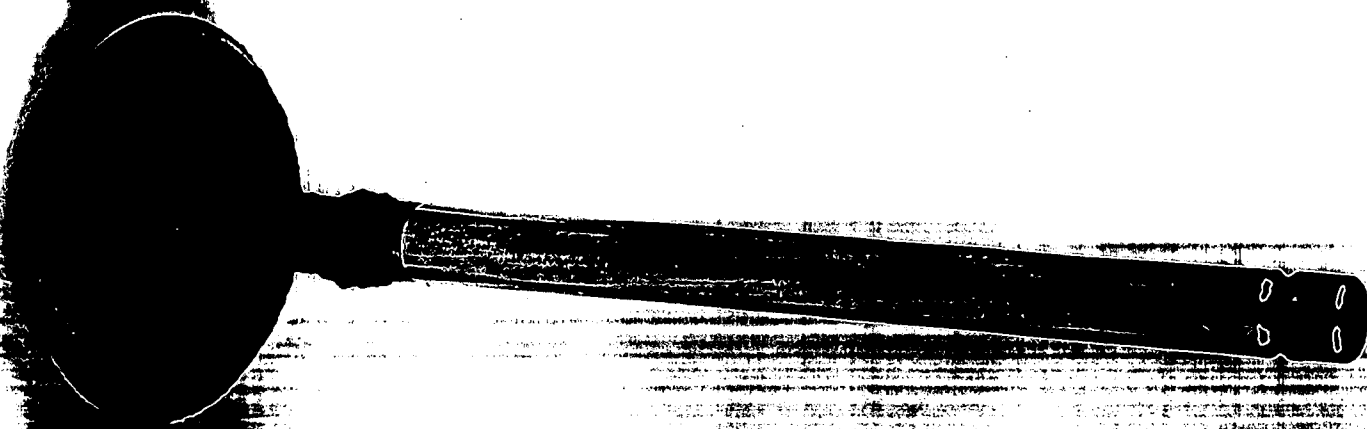
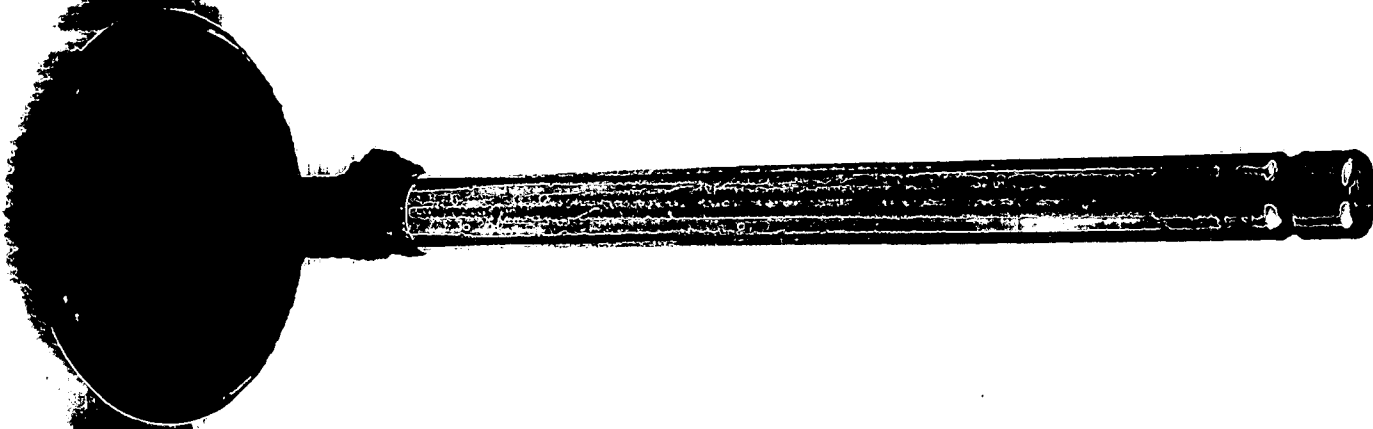
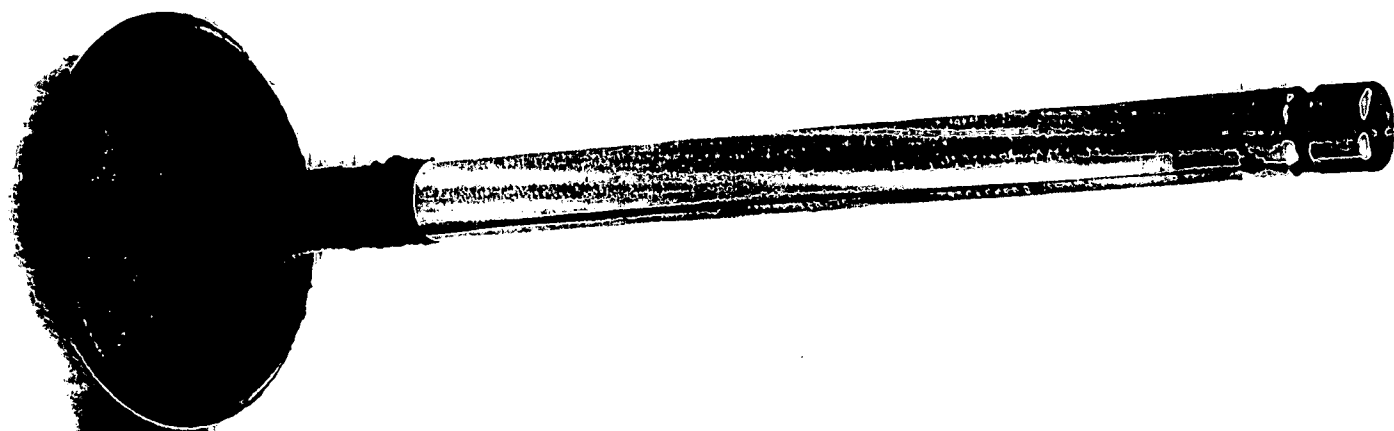


ATTACHMENT 4

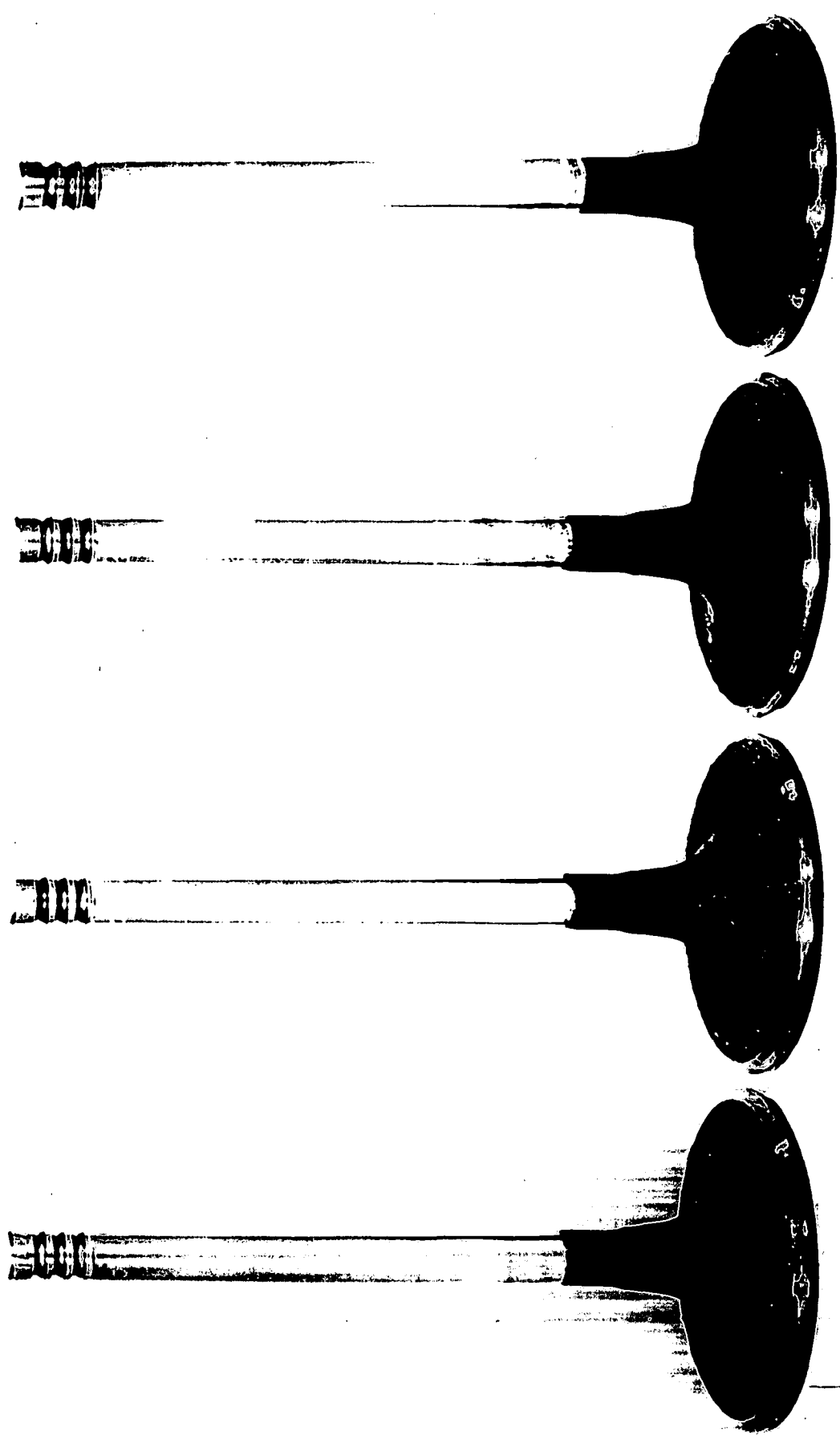
CAR C-6
CYLINDER HEAD



CAR C-6
INTAKE VALVES

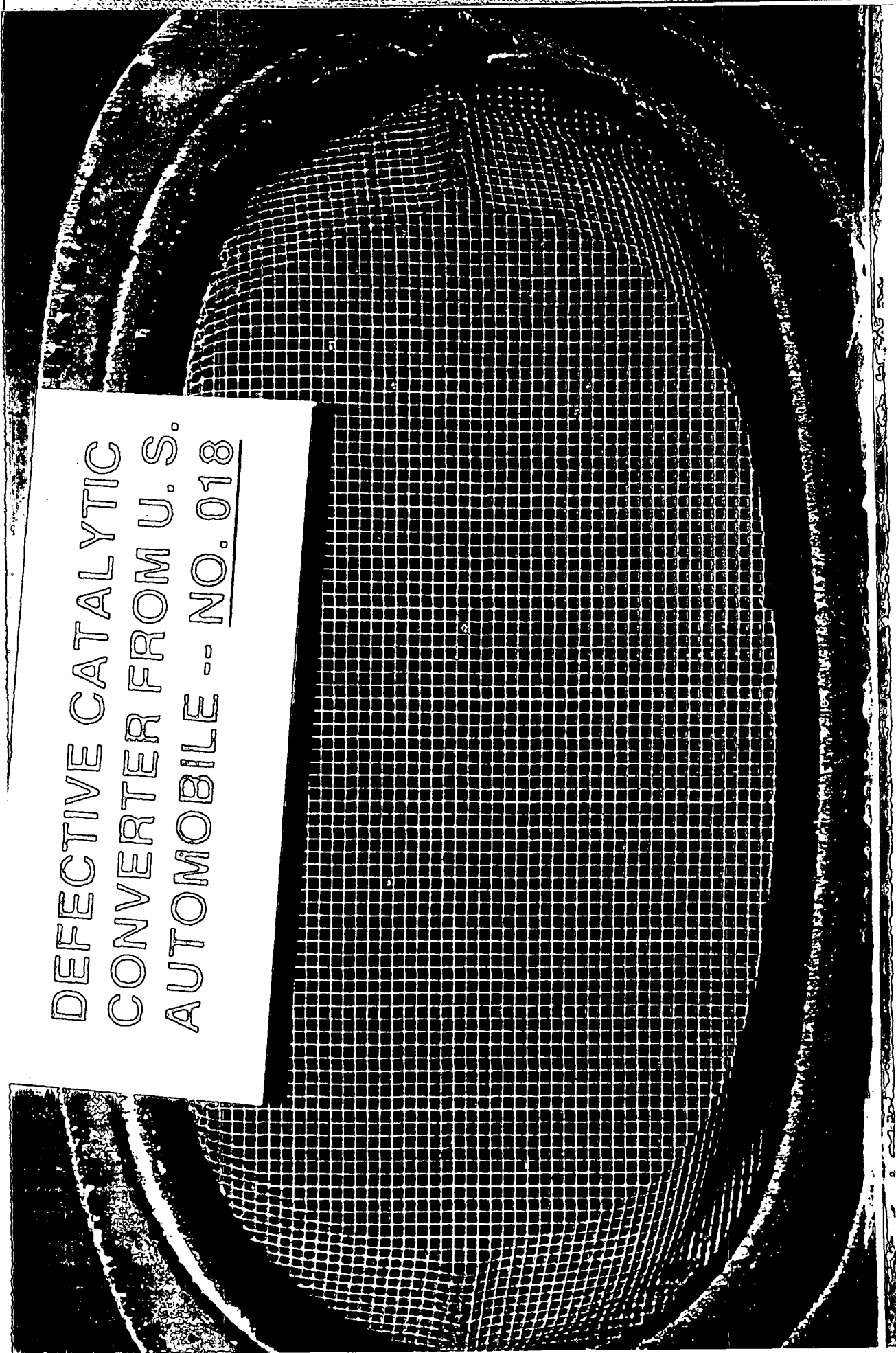


COMMERCIAL GASOLINE

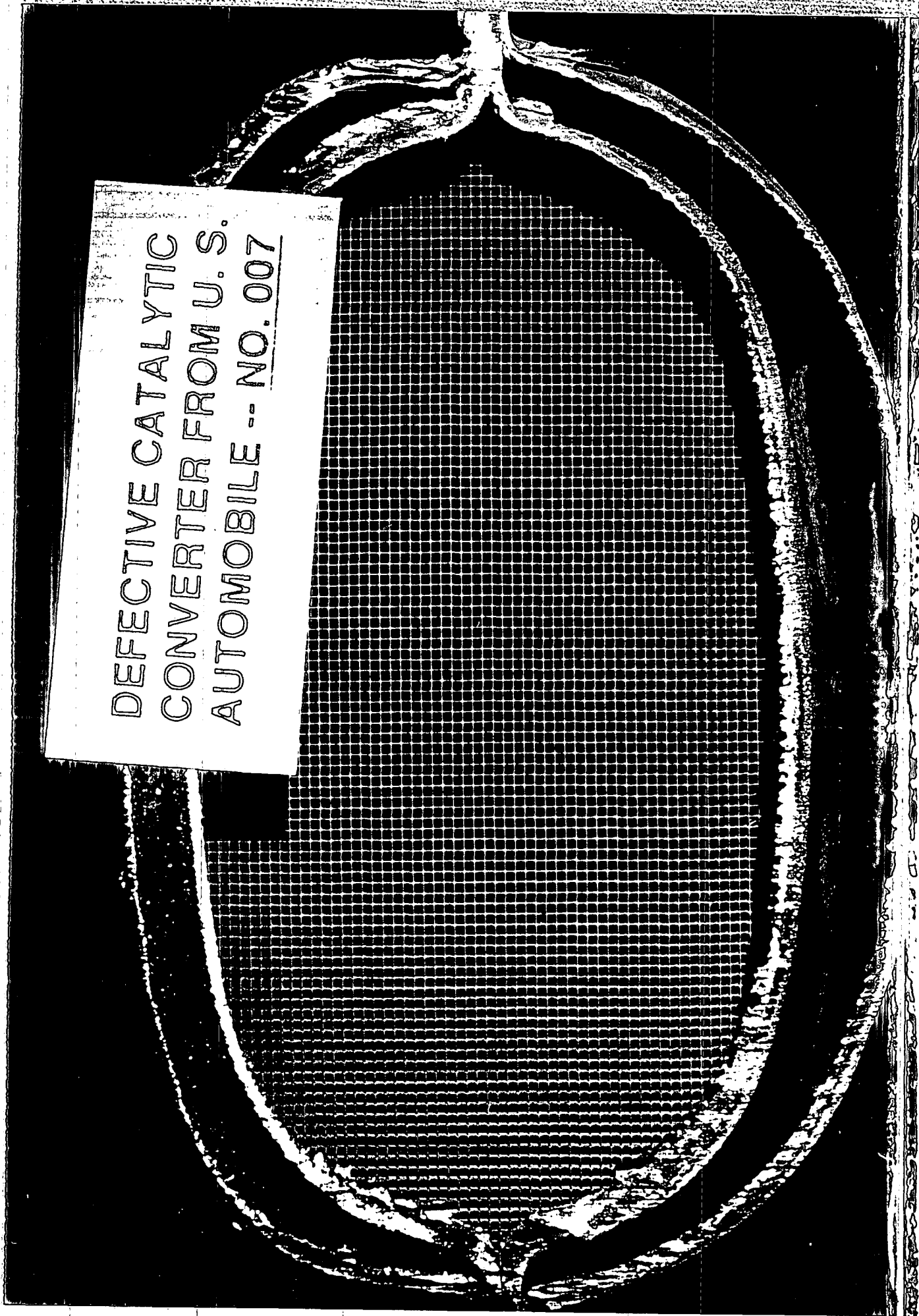


ATTACHMENT 5

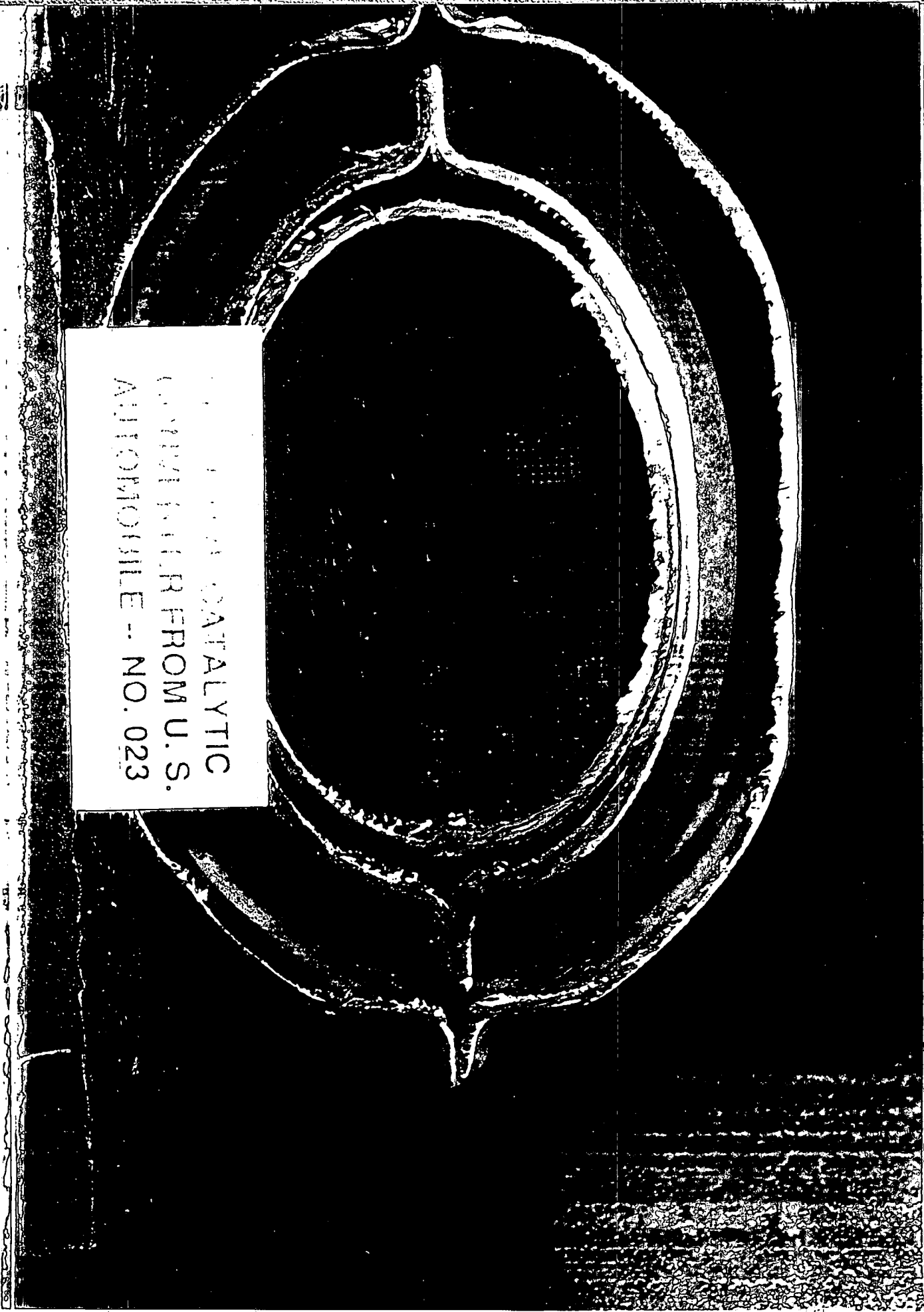
DEFECTIVE CATALYTIC
CONVERTER FROM U. S.
AUTOMOBILE -- NO. 018



DEFECTIVE CATALYTIC
CONVERTER FROM U. S.
AUTOMOBILE -- NO. 007



DEFECTIVE CATALYTIC
CONVERTER FROM U. S.
AUTOMOBILE -- NO. 018

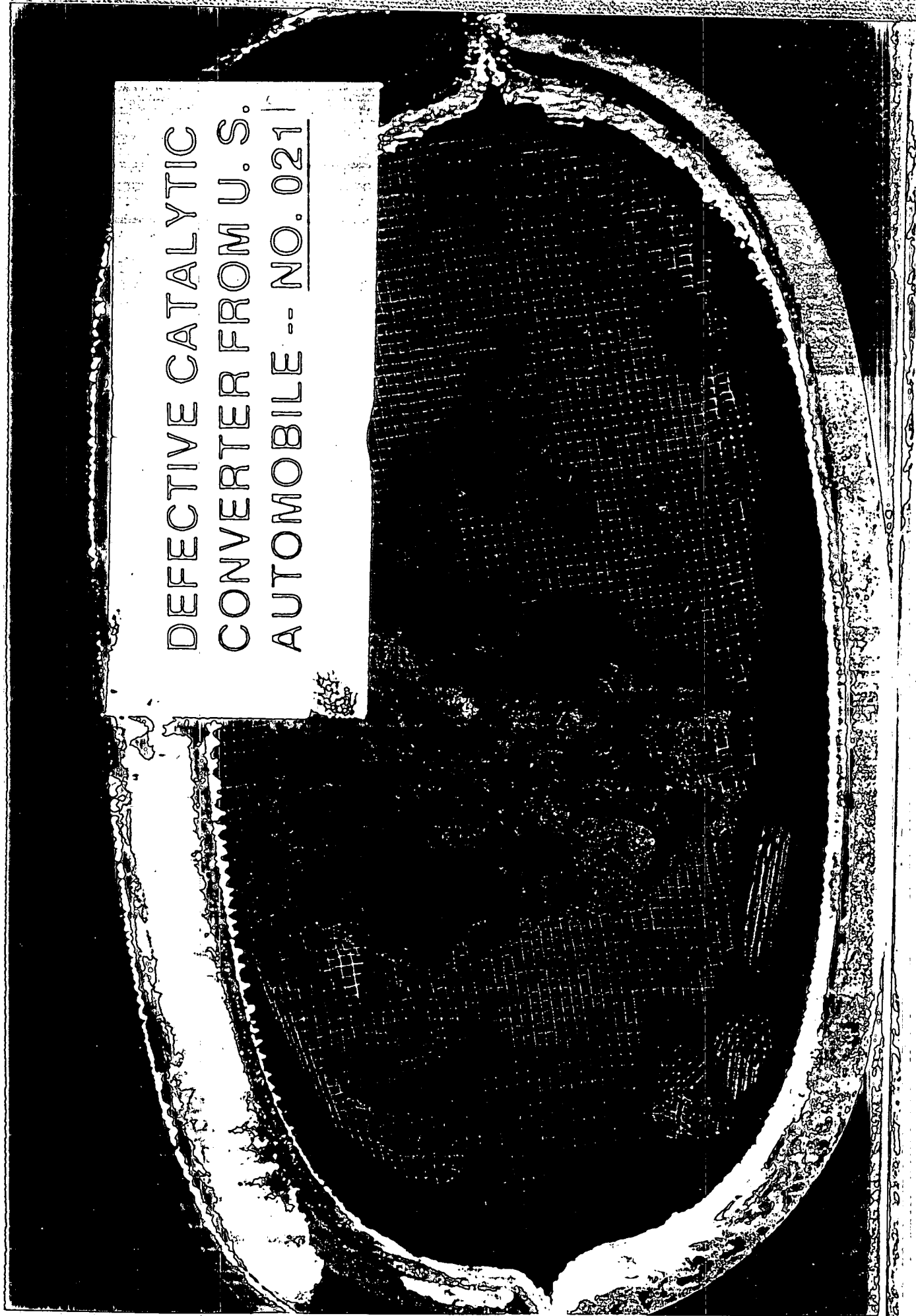


1964 CATALYTIC
CONVERTER FROM U.S.
AUTOMOBILE -- NO. 023

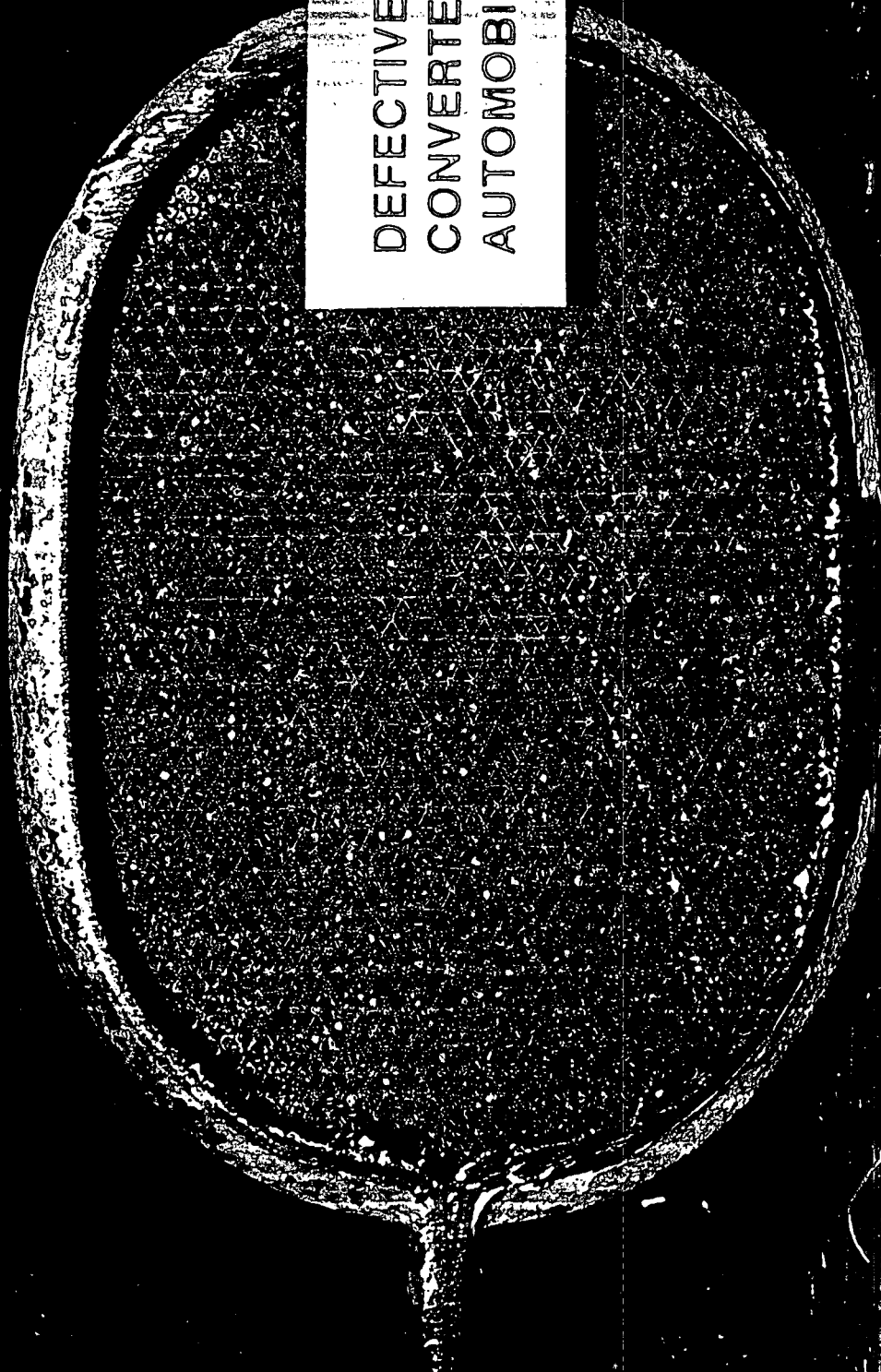
DEFECTIVE CATALYTIC
CONVERTER FROM U. S
AUTOMOBILE -- NO. 019




DEFECTIVE CATALYTIC
CONVERTER FROM U. S.
AUTOMOBILE -- NO. 021



DEFECTIVE CATALYTIC
CONVERTER FROM U. S.
AUTOMOBILE -- NO. 015



A circular, defective catalytic converter is shown. It has a mesh screen covering the front, and the interior is dark and textured, suggesting a honeycomb structure. The converter is placed on a dark, textured surface.

DEFECTIVE CATALYTIC
CONVERTER FROM U.S.
AUTOMOBILE -- NO. 012

3



TO: Ethyl Corporation

FROM: Systems Applications, Inc.

SUBJECT: Analysis of Ford's Submittal to the EPA, Attachment 5

DATE: 9 August 1990

In response to Ethyl Corporation's HiTEC 3000 waiver application, comments were received by the EPA from Ford Motor Company. These comments, dated 23 July 1990, represent Ford's review of Ethyl's waiver request and detail, in part, Ford's findings in regards to the effects of HiTEC 3000 on vehicle emissions and emission control systems.

Of particular interest is Attachment 5 of the Ford submittal. In this attachment, Ford provides results of their analysis of the percent effect of HiTEC 3000 (MMT) over baseline, an evaluation of the effect of HiTEC 3000 on engine-out and tailpipe emissions at 50K and 75K, a plot of the percent difference between Ethyl's baseline data and Ford's certification emission data, and finally, a graphical analysis of the effects of HiTEC 3000 on vehicle emissions by vehicle group. Ford states as a note on the cover of Attachment 5 that the figures and tables contained in their report were derived from test data provided by Ethyl. It is assumed from this note that the data set analyzed by Ford was ETHYL4S2, the main data set used in the statistical work performed by Systems Applications.

The purpose of this memorandum is twofold. First, this memo provides an evaluation of the analysis conducted by Ford as contained in Attachment 5 of their submittal to the EPA in response to Ethyl's HiTEC 3000 waiver application. In an attempt to confirm Ford's reported results, efforts were made to duplicate the procedures used by Ford in their analysis. Second, to address the questions raised by Ford in their submittal regarding the effect of HiTEC 3000 on catalyst converter performance, an



Ethyl Corporation

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evaluation of the statistical significance of the conversion efficiencies of all vehicle model groups (with the exception of vehicle group F) was also performed. The results of both analyses are summarized below.

Evaluation of Ford's analysis

To evaluate the results reported by Ford, Table 1 (Percent effect of HiTEC 3000 over baseline) and Figures 4 through 27 (Effects of HiTEC 3000 on vehicle emissions by vehicle group) were compared with the data in ETHYL4S2. Although in general our evaluation of the table and figures confirmed the results reported in the Attachment, significant errors in Ford's analysis of vehicle groups C and H were encountered. In addition, the results reported for vehicle groups H and I in Table 1 have apparently been switched by Ford. Furthermore, small errors in Table 1 results for vehicle group H exist. As a note, Figures 1 through 3 were not evaluated because of the unavailability of Ford's certification emissions data.

Figures 4 through 27

Specific analysis of Figures 4 through 6 (vehicle group C) show completely inaccurate results when compared with ETHYL4S2. This is particularly true for NOx. When compared with the mean emission effects reported in Table 1, it can be seen that the NOx percent effect averaged over range is smaller (greater negative value) than every value reported in Figure 6; in fact all percentage differences in Figure 6 should be negative. This is confirmed by the plotted results shown in Attachment 2A of Ethyl's waiver application (p. B-55).



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In addition to the inaccuracies shown for vehicle group C, small errors in the reported results for vehicle group H (Figures 19 to 21) also exist. These errors relate to the results shown for the intervals at 30K and 35K miles. In Ford's analysis, the NOx effect at 30K and 35K are reported to be 15 and 5 percent respectively. In actuality, the data contained in ETHYL4S2 shows the actual effect to be 6 percent at 30K and 17.5 percent at 35K.

Table 1

The reported results contained in Table 1 of Ford's Attachment 5 were also evaluated by comparison to ETHYL4S2. From this evaluation, it is clear that the results shown for vehicle groups H and I are switched. In addition, small errors in the results for vehicle group H exist. No other discrepancies between results reported by Ford and those calculated by Systems Applications for this evaluation were encountered.

One additional point should be made about the results detailed by Ford in Table 1. At the bottom of this table, Ford's shows a calculated average percent difference in the effect of HiTEC 3000 over baseline. From our evaluation, it appears that this is an unweighted average. Because of Ford's use of an unweighted average percent effect, the results shown give a slightly distorted view of the effect of HiTEC 3000. By taking an unweighted average, Ford suggests that it is appropriate to assume that all vehicle groups in the fleet program are represented equally in the national fleet. As can be seen in Attachment 2A of Ethyl's waiver application (p. 5), this is clearly not the case. It is therefore more appropriate to evaluate the effect of HiTEC 3000 on a weighted average basis as was done in the waiver application.



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page 4

On the attached, we have provided a revised Table 1 showing the correct results for vehicle groups H and I. In addition, we have calculated and shown the percent effect of HiTEC 3000 over baseline on a weighted average basis.

Engine out analysis

Using a similar approach to the methodology used to evaluate Ford's analysis in Table 1 and Figures 4 through 27, the results shown in Table 2 were also compared with data from ETHYL4S2. In our evaluation of Table 2, we were unable to reproduce any of the results shown by Ford. The results provided in the table are quite inconsistent with the data in ETHYL4S2 and with Ford's Figures 10 through 12 and 25 through 27 (vehicle groups E and T respectively). The values for 50,000 mile engine-out emissions depend on how the multiple observations for each vehicle are averaged. The methods used by Ford were unknown to us and may offer some explanation for the difficulties we encountered in obtaining duplicate values.

In addition to analyzing Ford's Table 2, an additional analysis on engine-out and tailpipe emissions for each vehicle (except D3) was performed. This analysis involved the calculation of conversion efficiencies. The conversion efficiency at a given mileage was defined as 1 minus the ratio of average tailpipe to average engine-out emissions. To determine the average tailpipe emissions for each vehicle, we used the averages from the ETHYL4S2 data (first two emissions tests only). For engine-out emissions, two or more tests were carried out at 50,000 miles (before and after the component changes). In addition, two tests were always carried out at 75,000 miles. No engine-out tests were performed on vehicle group F at 50,000 or 75,000 miles due to the coupling of the catalyst to the engine manifold preventing the insertion of an emission probe. No engine-out tests were performed on vehicle group



Ethyl Corporation

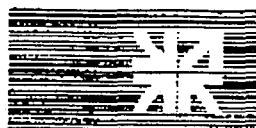
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I at 75,000 miles. To be consistent with the decision to omit 50,000 mile post-component change tailpipe emissions tests for the main working data set, we chose to use only the first two engine out tests at 50,000 miles for computing average engine-out emissions.

The conversion efficiencies were computed for each vehicle and pollutant at 50,000 and 75,000 miles. Averages across vehicles for each model group and fuel combination are reported in the attached tables. In these tables we also report results of statistical tests evaluating whether the HiTEC 3000 effect is beneficial against the null hypothesis that there is no effect or an adverse effect. In these tests, a low significance level (below about five percent) is strong evidence that the effect of HiTEC 3000 is beneficial with regard to conversion efficiencies. The tests performed parallel the statistical approach used in analyzing the integrated emissions in the waiver application (Appendix 2A, tables D-22 to D-24) with the exception that the integrated emissions for a vehicle were replaced by the conversion efficiency.

The overall results are as follows: For HC, there is no statistically significant effect at 50,000 miles (beneficial or adverse) but the effect at 75,000 miles is significantly beneficial (six percent level) using the most powerful weighted average test. For CO the reverse pattern appears: the effect is not significant at 75,000 miles but is significant (seven percent level) at 50,000 miles. For NO_x the effect is highly statistically significant at both mileages (two and zero percent levels). In each case the effect is either significantly beneficial or not adverse. There is no evidence of an adverse effect on conversion efficiencies.



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Table 1. Percent effect of MMT over baseline (averaged over range).

Model	Emissions (0 - 75K miles)			Emissions (0 - 50K miles)		
	HC	CO	NOx	HC	CO	NOx
C	21.44	8.77	-27.17	23.60	8.44	-22.32
D	5.62	-2.08	7.61	11.05	1.42	12.40
E	8.28	5.07	-7.11	14.04	12.58	-5.33
F	3.01	-34.61	-26.98	0.27	-29.94	-20.44
G	22.67	2.36	-4.69	23.16	-1.26	-1.62
H	2.34	-7.77	-0.82	-0.39	-9.42	13.04
I	5.79	-3.47	-15.75	4.90	-0.65	-7.78
T	8.51	-1.34	-28.12	12.41	4.79	-30.54
Unweighted Average % Dif.	9.71	-4.13	-12.88	11.13	-1.75	-7.82
Weighted Average % Dif.	8.17	-5.74	-13.78	8.53	-3.67	-7.34

Ethyl Corporation HiTEC 3000 Fleet Testing Program

50,000 Miles Conversion Efficiency Test Pollutant Hydrocarbons

Model	Conversion Efficiency 50,000 miles			----- Test Statistic	Rank Mean	Sum Test Sig.Level (%)(b)	T-test Sig.Level (%)(b)
	EEE	HT3	Sign				
D	0.765	0.720	-	4.0	3.0	80.00	82.23
E	0.873	0.891	+	2.0	4.5	20.00	13.22
T	0.830	0.851	+	1.0	4.5	10.00	3.53
C	0.888	0.877	-	7.0	4.5	90.00	83.28
G	0.896	0.893	-	6.0	4.5	80.00	59.75
H	0.896	0.894	-	5.0	4.5	65.00	55.73
I	0.906	0.919	+	0.0	4.5	5.00	6.54
Weighted Average(c)	0.879	0.883	+				26.13
Total				25.0	30.0	19.73	

EPA Sign Test: Observation of 3 '+' sign(s) in 7 trials rejects the hypothesis of no beneficial HiTEC 3000 effect at the 77.34 percent significance level(b).

EPA Overall Rank Sum Test: The hypothesis of no beneficial HiTEC 3000 effect is rejected at the 19.73 percent significance level(b).

Weighted Average Test: The hypothesis of no beneficial HiTEC 3000 effect is rejected at the 26.13 percent significance level(b).

Notes:

- Each figure is the mean of the conversion efficiencies at 50,000 miles for each fuel.
 - The lower the significance level, the greater the evidence of a beneficial HiTEC 3000 effect.
 - The weights for the weighted averages are proportional to 1988 sales figures.
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Ethyl Corporation HiTEC 3000 Fleet Testing Program

50,000 Miles Conversion Efficiency Test
Pollutant Carbon Monoxide

Model	Conversion Efficiency 50,000 miles			----- Rank Sum Test ----- Test Mean Sig.Level Statistic	----- Sig.Level (%)(b)	T-test Sig.Level (%)(b)	
	EEE	HT3	Sign				
D	0.606	0.593	-	5.0	3.0	90.00	85.37
E	0.489	0.538	+	0.0	4.5	5.00	1.34
T	0.610	0.647	+	2.0	4.5	20.00	22.97
C	0.706	0.654	-	7.0	4.5	90.00	84.66
G	0.690	0.738	+	4.0	4.5	50.00	22.53
H	0.712	0.742	+	2.0	4.5	20.00	12.35
I	0.786	0.790	+	4.0	4.5	50.00	35.38
Weighted Average(c)	0.678	0.696	+				6.87
Total				24.0	30.0	15.35	

EPA Sign Test: Observation of 5 '+' sign(s) in 7 trials rejects the hypothesis of no beneficial HiTEC 3000 effect at the 22.66 percent significance level(b).

EPA Overall Rank Sum Test: The hypothesis of no beneficial HiTEC 3000 effect is rejected at the 15.35 percent significance level(b).

Weighted Average Test: The hypothesis of no beneficial HiTEC 3000 effect is rejected at the 6.87 percent significance level(b).

Notes:

- Each figure is the mean of the conversion efficiencies at 50,000 miles for each fuel.
 - The lower the significance level, the greater the evidence of a beneficial HiTEC 3000 effect.
 - The weights for the weighted averages are proportional to 1988 sales figures.
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Ethyl Corporation HiTEC 3000 Fleet Testing Program

50,000 Miles Conversion Efficiency Test Pollutant Nitrogen Oxides

Model	Conversion Efficiency 50,000 miles			----- Test Statistic	Rank Mean	Sum Test Sig.Level (%)(b)	T-test Sig.Level (%)(b)
	EEE	HT3	Sign				
D	0.778	0.714	-	6.0	3.0	100.00	99.52
E	0.780	0.789	+	3.0	4.5	35.00	33.29
T	0.795	0.827	+	2.0	4.5	20.00	8.95
C	0.832	0.891	+	0.0	4.5	5.00	6.61
G	0.734	0.729	-	5.0	4.5	65.00	56.76
H	0.606	0.684	+	2.0	4.5	20.00	12.10
I	0.759	0.778	+	4.0	4.5	50.00	21.29
Weighted Average(c)	0.731	0.767	+				2.13
Total				22.0	30.0	8.66	

EPA Sign Test: Observation of 5 '+' sign(s) in 7 trials rejects the hypothesis of no beneficial HiTEC 3000 effect at the 22.66 percent significance level(b).

EPA Overall Rank Sum Test: The hypothesis of no beneficial HiTEC 3000 effect is rejected at the 8.66 percent significance level(b).

Weighted Average Test: The hypothesis of no beneficial HiTEC 3000 effect is rejected at the 2.13 percent significance level(b).

Notes:

- Each figure is the mean of the conversion efficiencies at 50,000 miles for each fuel.
 - The lower the significance level, the greater the evidence of a beneficial HiTEC 3000 effect.
 - The weights for the weighted averages are proportional to 1988 sales figures.
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Ethyl Corporation HiTEC 3000 Fleet Testing Program

75,000 Miles Conversion Efficiency Test Pollutant Hydrocarbons

Model	Conversion Efficiency 75,000 miles			----- Rank Sum Test ----- Test Mean Sig.Level Statistic (%) (b)	T-test Sig.Level (%) (b)		
	EEE	HT3	Sign				
D	0.729	0.742	+	3.0	3.0	60.00	38.69
E	0.855	0.867	+	5.0	4.5	65.00	31.20
T	0.823	0.857	+	0.0	4.5	5.00	0.07
C	0.868	0.864	-	6.0	4.5	80.00	60.80
G	0.860	0.864	+	5.0	4.5	65.00	37.82
H	0.852	0.856	+	4.0	4.5	50.00	37.09
Weighted Average(c)	0.844	0.854	+				5.73
Total				23.0	25.5	32.20	

EPA Sign Test: Observation of 5 '+' sign(s) in 6 trials rejects the hypothesis of no beneficial HiTEC 3000 effect at the 10.94 percent significance level(b).

EPA Overall Rank Sum Test: The hypothesis of no beneficial HiTEC 3000 effect is rejected at the 32.20 percent significance level(b).

Weighted Average Test: The hypothesis of no beneficial HiTEC 3000 effect is rejected at the 5.73 percent significance level(b).

Notes:

- Each figure is the mean of the conversion efficiencies at 75,000 miles for each fuel.
 - The lower the significance level, the greater the evidence of a beneficial HiTEC 3000 effect.
 - The weights for the weighted averages are proportional to 1988 sales figures.
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Ethyl Corporation HiTEC 3000 Fleet Testing Program

75,000 Miles Conversion Efficiency Test Pollutant Carbon Monoxide

Model	Conversion Efficiency 75,000 miles			----- Test Statistic	Rank Mean	Sum Test Sig.Level (%)(b)	T-test Sig.Level (%)(b)
	EEE	HT3	Sign				
D	0.567	0.575	+	2.0	3.0	40.00	35.22
E	0.467	0.478	+	5.0	4.5	65.00	41.45
T	0.583	0.668	+	0.0	4.5	5.00	0.27
C	0.557	0.537	-	5.0	4.5	65.00	60.24
G	0.658	0.599	-	8.0	4.5	95.00	92.23
H	0.672	0.685	+	3.0	4.5	35.00	33.44
Weighted Average(c)	0.600	0.613	+				23.95
Total				23.0	25.5	32.20	

EPA Sign Test: Observation of 4 '+' sign(s) in 6 trials rejects the hypothesis of a beneficial HiTEC 3000 effect at the 34.38 percent significance level(b).

EPA Overall Rank Sum Test: The hypothesis of no beneficial HiTEC 3000 effect is rejected at the 32.20 percent significance level(b).

Weighted Average Test: The hypothesis of no beneficial HiTEC 3000 effect is rejected at the 23.95 percent significance level(b).

Notes:

- Each figure is the mean of the conversion efficiencies at 75,000 miles for each fuel.
- The lower the significance level, the greater the evidence of a beneficial HiTEC 3000 effect.
- The weights for the weighted averages are proportional to 1988 sales figures.

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Ethyl Corporation HiTEC 3000 Fleet Testing Program

75,000 Miles Conversion Efficiency Test Pollutant Nitrogen Oxides

Model	Conversion Efficiency 75,000 miles			----- Rank Sum Test ----- Test Statistic	Mean	----- Sig.Level (%)(b)	T-test Sig.Level (%)(b)
	EEE	HT3	Sign				
D	0.769	0.740	-	5.0	3.0	90.00	82.93
E	0.780	0.806	+	4.0	4.5	50.00	25.87
T	0.794	0.841	+	0.0	4.5	5.00	0.54
C	0.756	0.839	+	0.0	4.5	5.00	2.22
G	0.695	0.637	-	7.0	4.5	90.00	90.38
H	0.625	0.766	+	0.0	4.5	5.00	0.01
Weighted Average(c)	0.714	0.780	+				0.00
Total				16.0	25.5	3.95	

EPA Sign Test: Observation of 4 '+' sign(s) in 6 trials rejects the hypothesis of beneficial HiTEC 3000 effect at the 34.38 percent significance level(b).

EPA Overall Rank Sum Test: The hypothesis of no beneficial HiTEC 3000 effect is rejected at the 3.95 percent significance level(b).

Weighted Average Test: The hypothesis of no beneficial HiTEC 3000 effect is rejected at the 0.00 percent significance level(b).

Notes:

- Each figure is the mean of the conversion efficiencies at 75,000 miles for each fuel.
 - The lower the significance level, the greater the evidence of a beneficial HiTEC 3000 effect.
 - The weights for the weighted averages are proportional to 1988 sales figures.
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Analysis of the Ford Submitted Data

As a part of their comments Ford Motor Company submitted detailed compositional analysis and microreactor conversion efficiency data for two series of catalysts removed from Canadian automobiles. The first series of 11 catalysts were removed from 10 Ford of Canada employees cars that had no reported/detectable mechanical or operational problems. The second series of 26 catalysts were from 13 Canadian automobiles with operational problems repaired by Ford dealers.

The microreactor used for determining the catalyst activity employs a small "button" (1/2" diameter x 1/2" high cylinder) removed from the approximate center of the monolith. The sampling technique removes a 1/2" diameter "button" from the monolith inlet, middle and outlet. The inlet "button" is then used in the microreactor procedure to determine conversion efficiency for the three regulated pollutants hydrocarbons, carbon monoxide and nitrogen oxide. Each of the three buttons is analyzed by the B.E.T. adsorption technique to determine the surface area and by XRF technique to determine the metals content. The inlet, middle and outlet sample results show "profiles" of surface area and composition in the gas flow direction. The profiles for contamination (Pb, Zn, Ba, etc.) concentrations generally show much higher levels on the inlet sample than either the middle or outlet sample. If, as generally accepted, these contaminants adversely affect catalyst activity, a regression analysis should separate the individual relationships without the "noise" of other effect to confuse the issue. It cannot be emphasized too often nor too strongly that the collection of catalysts are not representative of the population of automobiles in service since 13 of 23 automobiles were known to have catalyst related deficiencies. The 10 automobiles from Ford employees may or may not have been in need of repair. This question was examined by a separate analysis of these automobiles. The number of observations is reduced and it is difficult to see any additional information from this analysis.

The microreactor procedure determined conversion efficiencies at a gas inlet temperature of approximately 550°C for redox ratios from about 0.8 to 1.85. The reason for evaluating such fuel rich regions (R much greater than 1) is not clear. The primary region of interest is about R = 1. Data analyses were conducted for redox ration of 1.0. There were some differences in the significance levels of variables but overall: 1) the expected poisons (Ba, Zn and Pb) showed varying degrees of catalyst poisoning; 2) when the levels of catalyst metals varied significantly the effects were noticeable on catalyst efficiency ¹ (Ce, Ni are particularly of note); 3) Manganese does not reduce the

¹This is important because it indicates that the analysis is sensitive enough to find intentional changes to catalyst formulations made by manufacturer.

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conversion efficiency for hydrocarbon, carbon monoxide or nitrogen oxide, and in fact shows moderate improvement for hydrocarbon and carbon monoxide.

The data analysis results for redox ratio = 1.0 gave variables and significance levels as shown in Table 1. The hydrocarbon results show Lead and Zinc to be highly significant poisons (denoted by the negative sign of the coefficient) and surface area and manganese to be significant positive correlates. Carbon monoxide results reveal that Barium, Iron, Miles, and Zinc significantly reduce conversion efficiency and Surface Area, Nickel, Cerium, and Manganese increase conversion efficiency. Barium and Lead significantly reduce, while Surface Area, Nickel and Sulfur significantly increase nitrogen oxide conversion efficiency. The regression models explained large fractions of the error varying from about 0.80 for the nitrogen oxide regression to about 0.90 for the hydrocarbon regression. The Nickel and Cerium are believed to be part of the catalyst wash coat formulations (as opposed to Lead e.g. which is a contaminant). These components appeared in the catalysts at two distinct levels and it is not clear if this represents some predictable catalyst phenomenon or is indicative of changed catalyst formulation. In either event the regression technique was capable of detecting the significance of the changes. The positive effect of Sulfur in nitrogen oxide conversion efficiency is surprising but may be an artifact because of the many zero levels of sulfur reported. Figure 1 shows the percent increase in HC (hydrocarbon) conversion efficiency for each significant regression variable as listed on the y-axis. The units of measure for each regression variable and its minimum and maximum values are also shown along the y-axis. The average is shown on the x-axis as the mid tick mark flanked on each side by the 95% confidence limits. To illustrate how to use these somewhat complex but highly informative charts consider the data for manganese. The y-axis data shows that the units of measure for the Mn variable is wt.%; the minimum wt.% in the data is 0.05 and the maximum wt.% is 6.3. The average percent increase in HC conversion efficiency is about 28 with lower and upper 95% confidence limits of about 0 and 55, respectively. X-axis values greater than zero indicate improved catalyst conversion efficiency and values less than zero indicate degraded catalyst conversion efficiency. A cursory glance shows that Manganese and Surface Area improve conversion efficiency and Lead and Zinc degrade conversion efficiency.

Figure 2 shows main effects for carbon monoxide. Manganese, Cerium, Nickel and Surface Area improve conversion efficiency while Barium, Iron, Zinc, and Miles on Car degrade conversion efficiency.

Figure 3 shown main effects for nitrogen oxide. Sulfur, Nickel and Surface Area improve conversion efficiency and Barium and Lead degrade conversion efficiency.

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TABLE 1

Regression Summaries for Redox Ratio = 1

<u>Independent Variable</u>	<u>Variable ID</u>	<u>Coeff. Value</u>	<u>Standard Error</u>	<u>Significance Level</u>
Hydrocarbon*	Intercept	70.66	8.80	-
	Surface Area**	1.02	0.40	0.021
	Lead	-17.04	4.23	0.001
	Zinc	-91.75	21.60	0.001
	Manganese	4.46	2.08	0.046

R-sq. = 0.806; RMS Error = 6.794

Carbon Monoxide*

Intercept	87.83	5.55	-
Surface Area**	0.48	0.19	0.022
Nickel	14.50	3.39	0.001
Cerium	2.85	0.77	0.002
Barium	-14.51	6.87	0.053
Iron	-20.88	9.47	0.045
Zinc	-19.31	8.76	0.045
Manganese	3.57	0.93	0.002
Miles	-0.000283	0.000071	0.001

R-sq. = 0.739; RMS Error = 2.144

Nitrogen Oxide*

Intercept	90.06	31.95	-
Surface Area**	2.26	0.94	0.028
Nickel	49.46	14.07	0.003
Barium	-127.23	56.55	0.001
Lead	144.55	11.69	0.001
Sulfur	232.12	103.77	0.039

R-sq. = 0.647; RMS Error = 18.23

* - The independent variables are in conversion efficiency for the stated pollutant.

** - B.E.T. values in sq. m per gram.

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Figures 4, 5, 6, and 7 show hydrocarbon conversion efficiencies for each of the significant regression variables. Every plot is adjusted with the regression model for each of the remaining variables. This results in a depiction of the relationship independent of the scatter introduced by other variables. Zinc, shown in Figure 4, shows that the data is evenly distributed over the range of dependent variables (i.e. not concentrated in clusters). The Lead plot (Figure 5) is different from Zinc in that most of the data is clustered at values less than about 0.25 with only three points at 1.2 and greater which would suggest a higher influence on slope for these points. Surface Area and Manganese plots (Figures 6 and 7) show acceptable distribution like the Zinc curve. The general conclusion is that except for Lead, the dataset was well-conditioned to detect the relationships between the regression variables.

Figures 8 through 15 show adjusted plots for Carbon Monoxide for each one of the significant regression variables. The "clustering" of the data for Nickel and Cerium are seen graphically in Figures 8 and 11, respectively. This is assumed to indicate changes in catalyst formulation rather than in service effect.

Figures 16 through 20 show adjusted plots for nitrogen oxide for each one of the significant regression variables. The plot with lead (Figure 16) exhibits once again the large leverage of the three data points at lead values greater than 1.2. The clustering of the data for Nickel are evident in Figure 17. The effect of Sulfur is somewhat surprising but is greatly influenced by the large number of zero values reported for Sulfur. Expectation would be that the effect would vanish if sufficient numbers of samples were included.

Conclusions:

The microreactor measures of activity when combined with the composition data for the inlet samples provide the tools for determining what components actually degrade or improve catalyst conversion efficiency. The regression analysis provides the means for separating the effects for separate components. It is remarkable that in such random collections of catalysts the results can be correlated as well as is shown. The accepted poisons (PB, Zn and sometimes FE) indeed show up as degrading catalyst conversion efficiency and the known promoters (Ni, CE and Surface Area) are shown as improving conversion efficiency. Manganese is not shown to degrade catalyst conversion efficiency. Similar results are seen when the integrated conversion efficiency is used as the independent variable. These results were not reported herein but are available if they are desired.

FIGURE 1

Mulreg FORT1233, Model FORT12332
Main Effects on Response HC
(with 95% Confidence Intervals)

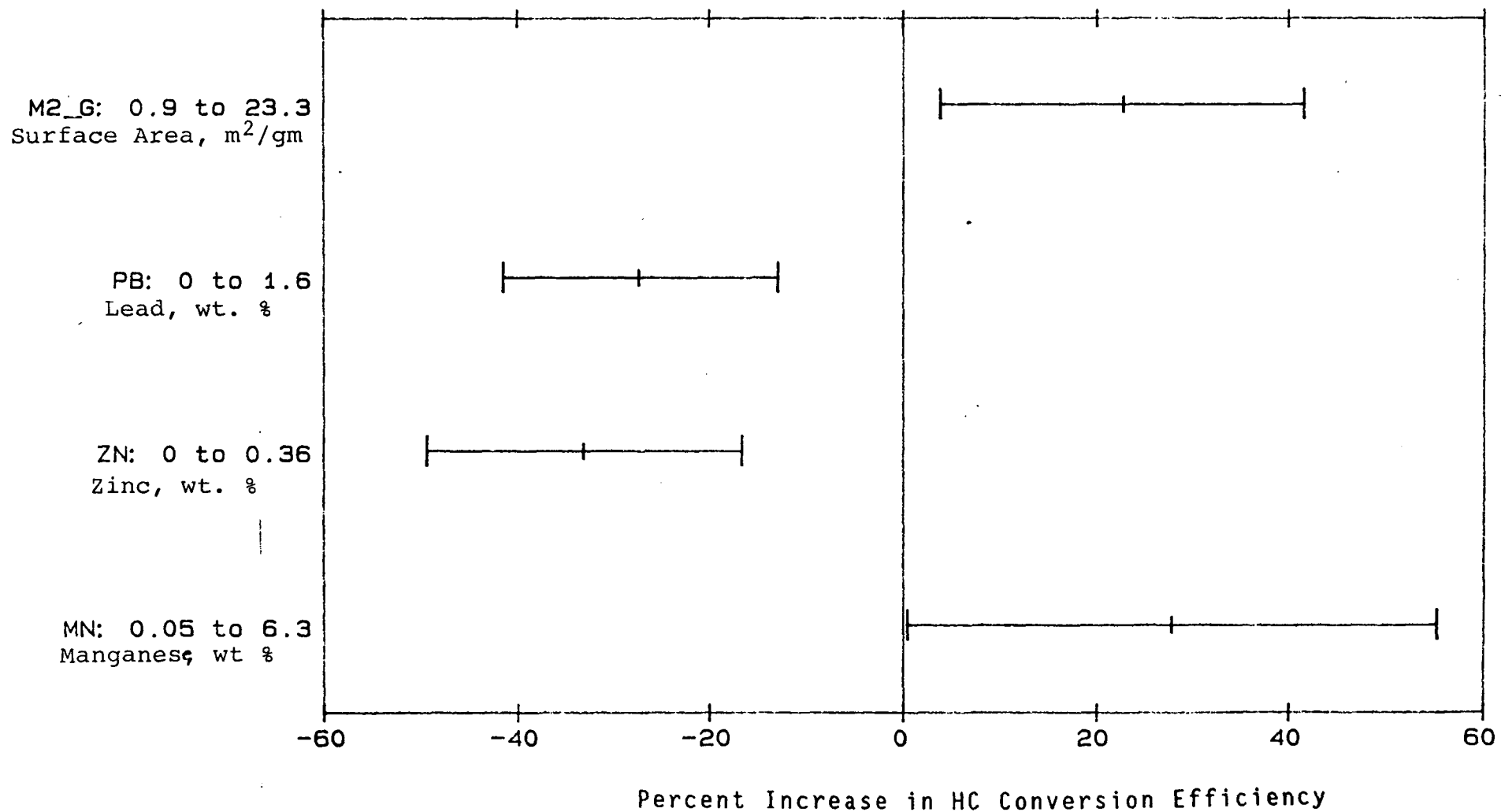


FIGURE 2

Mulreg FORT1233, Model FORT12333
Main Effects on Response CO
(with 95% Confidence Intervals)

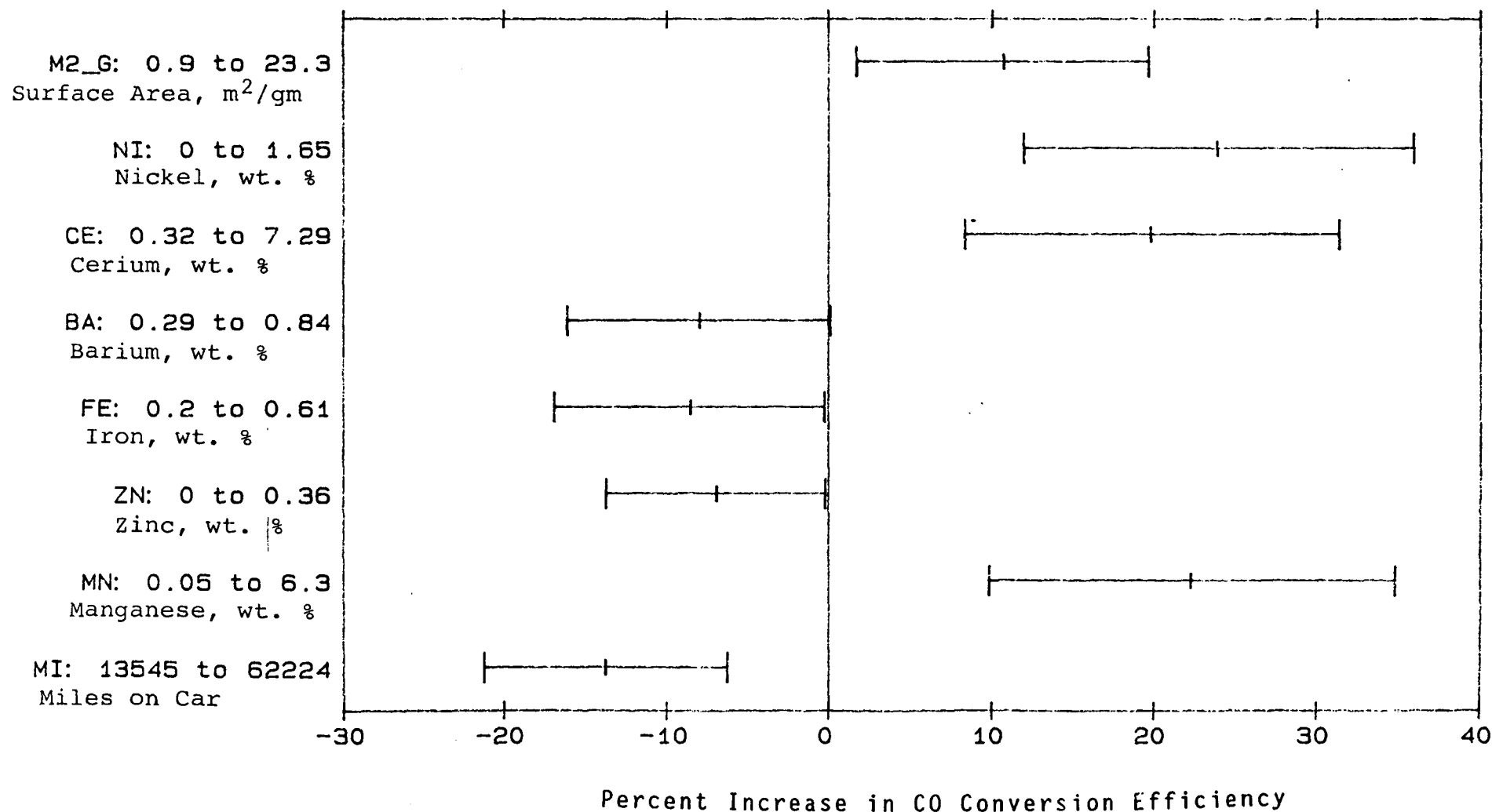


FIGURE 3

Mulreg FORT1233, Model FORT12331_COPY
Main Effects on Response NOX
(with 95% Confidence Intervals)

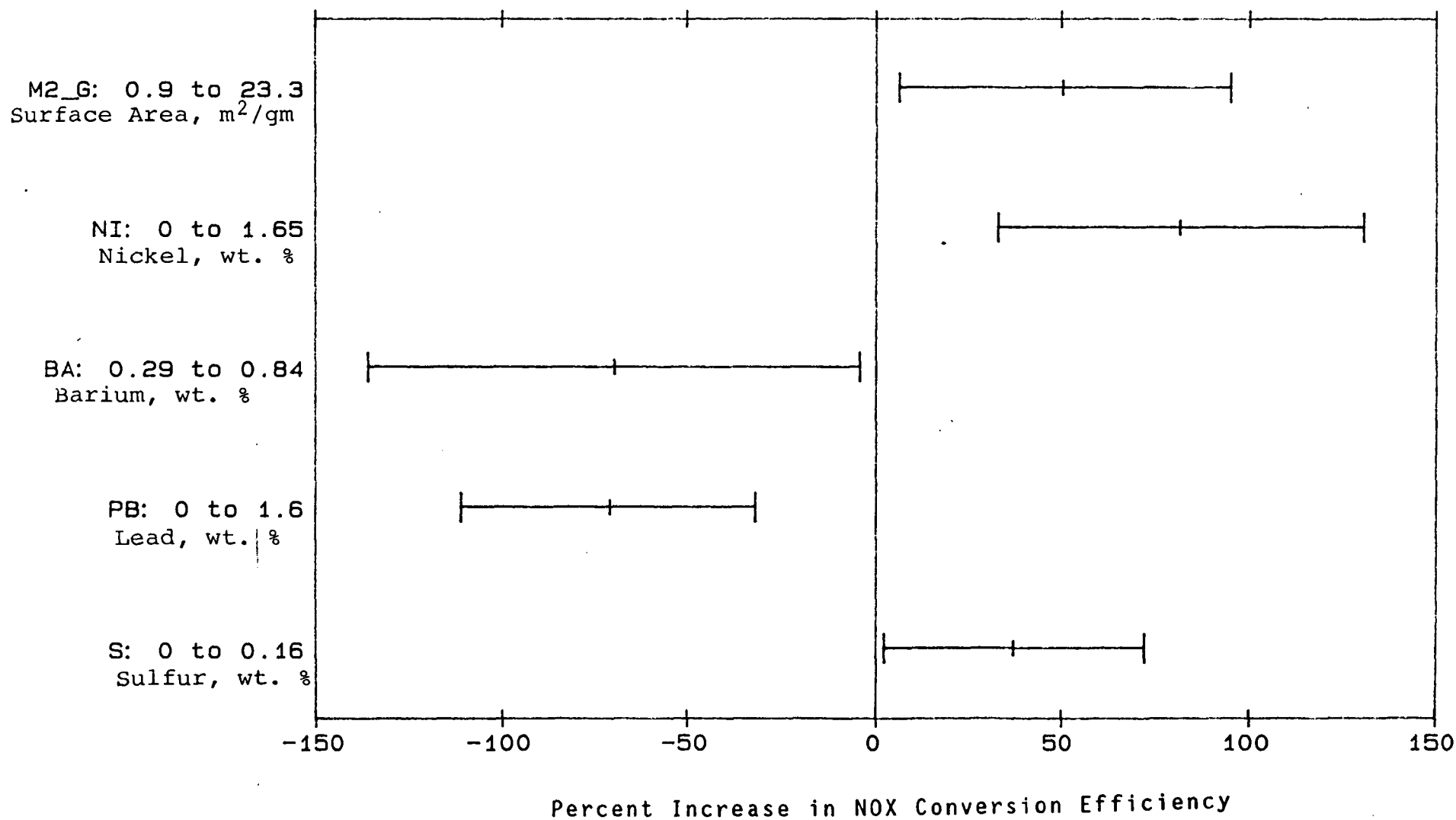


FIGURE 4

Graph: 49369

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HC vs ZN, Adjusted for Remaining Predictors
Using Mulreg FORT1233, Model FORT12332

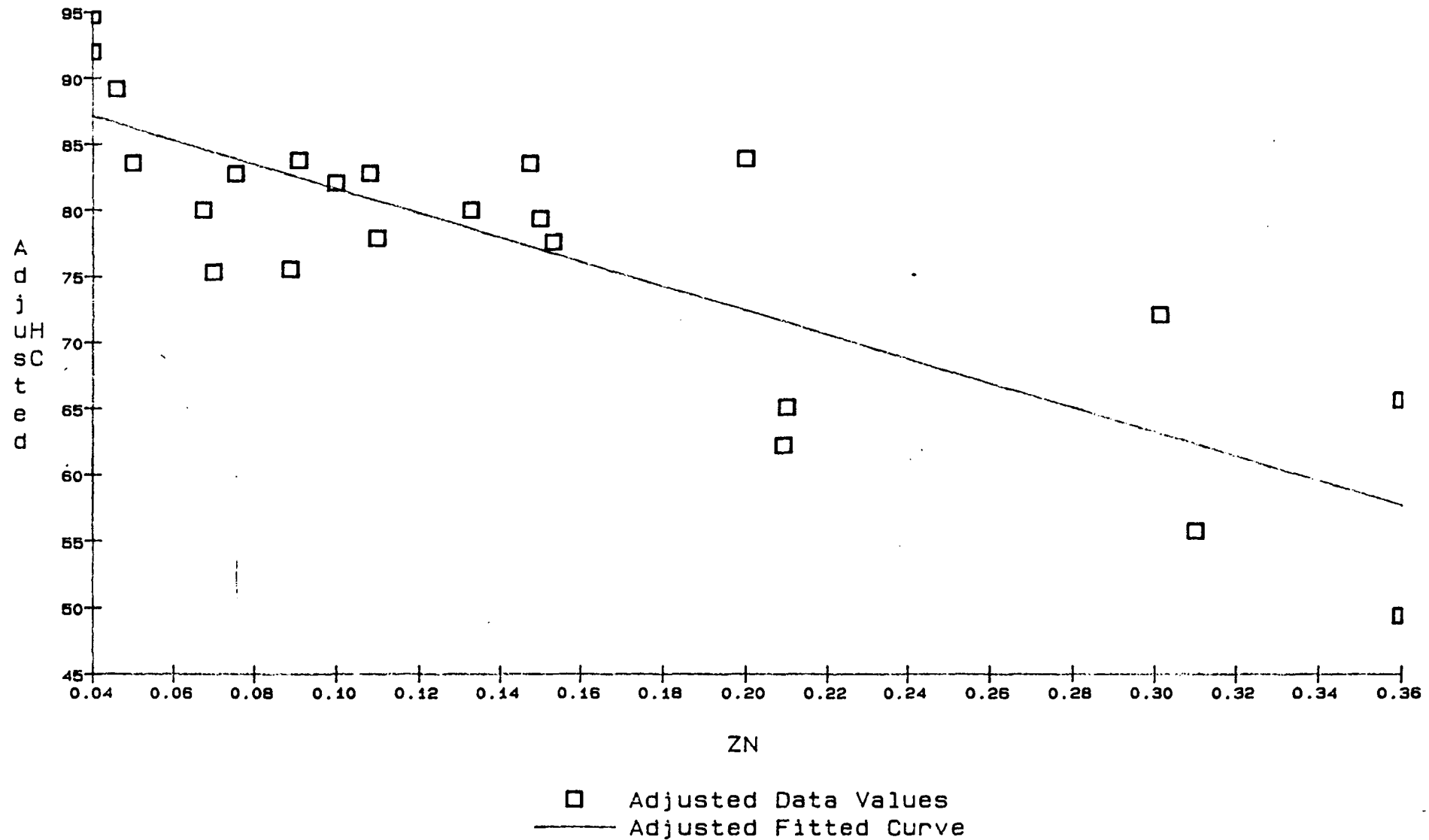


FIGURE 5

Graph: 49378

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HC vs PB, Adjusted for Remaining Predictors
Using Mulreg FORT1233, Model FORT12332

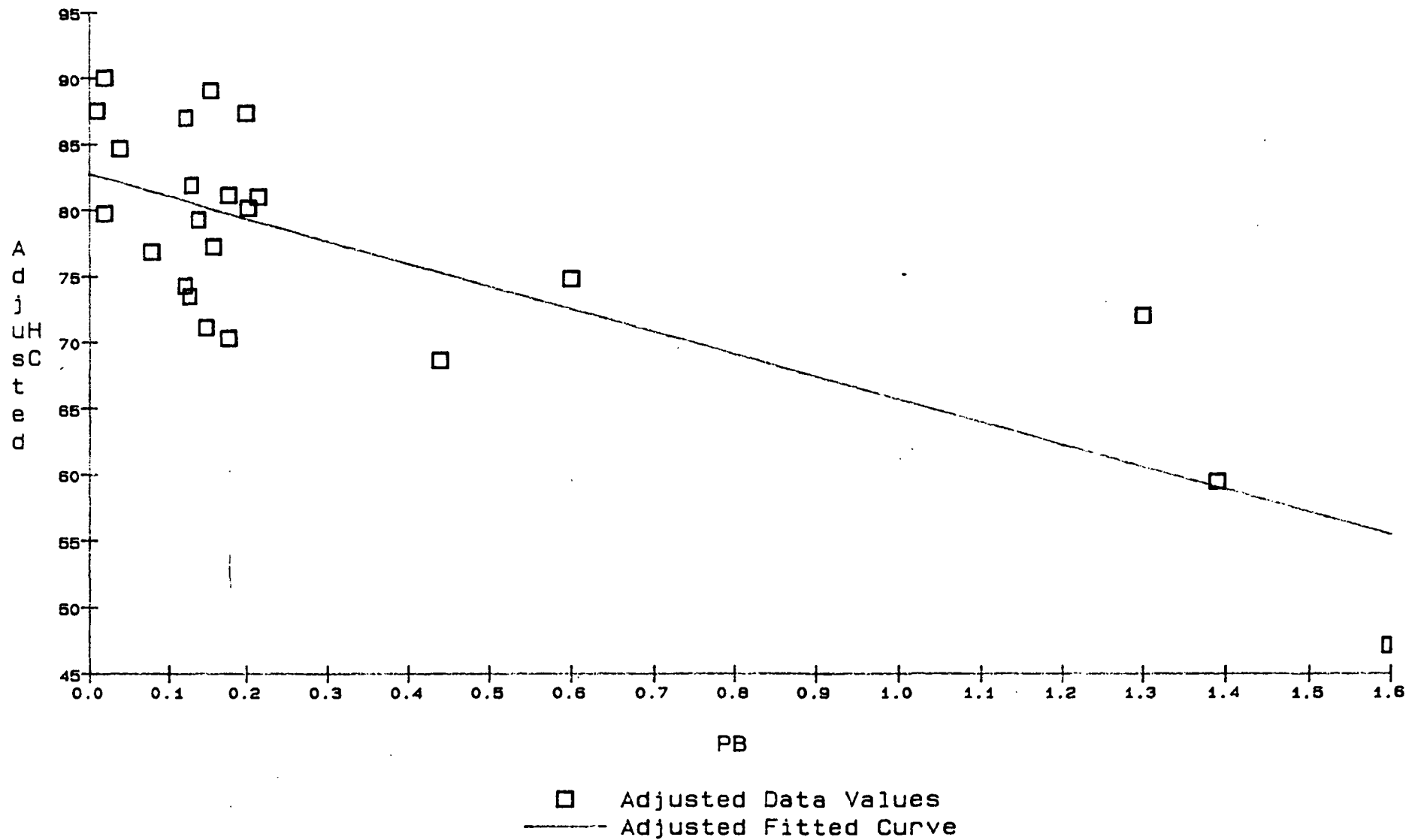


FIGURE 0

Graph: 49387

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HC vs M2_G, Adjusted for Remaining Predictors.
Using Mulreg FORT1233, Model FORT12332

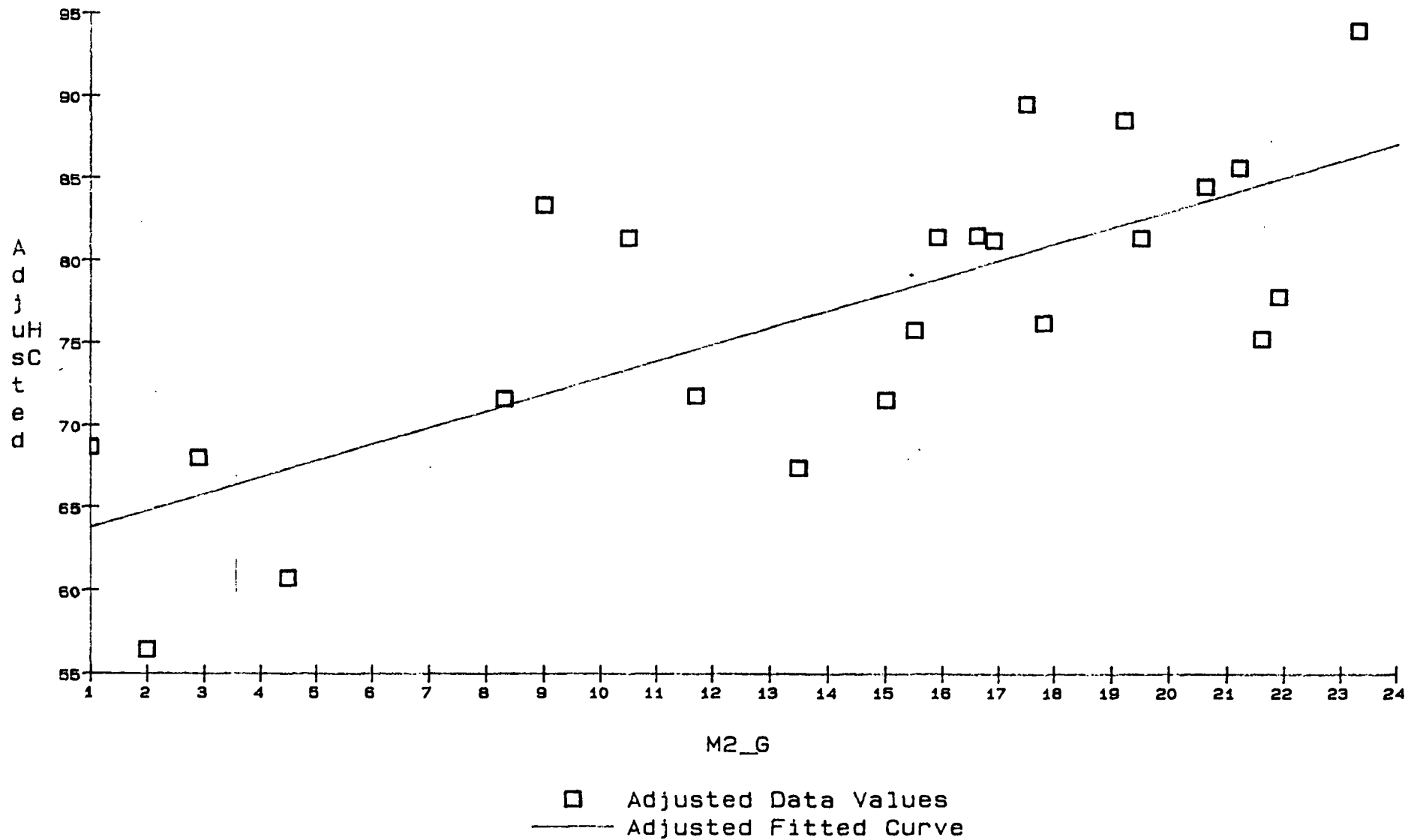


FIGURE /

Graph: 49360

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HC vs MN, Adjusted for Remaining Predictors
Using Mulreg FORT1233, Model FORT12332

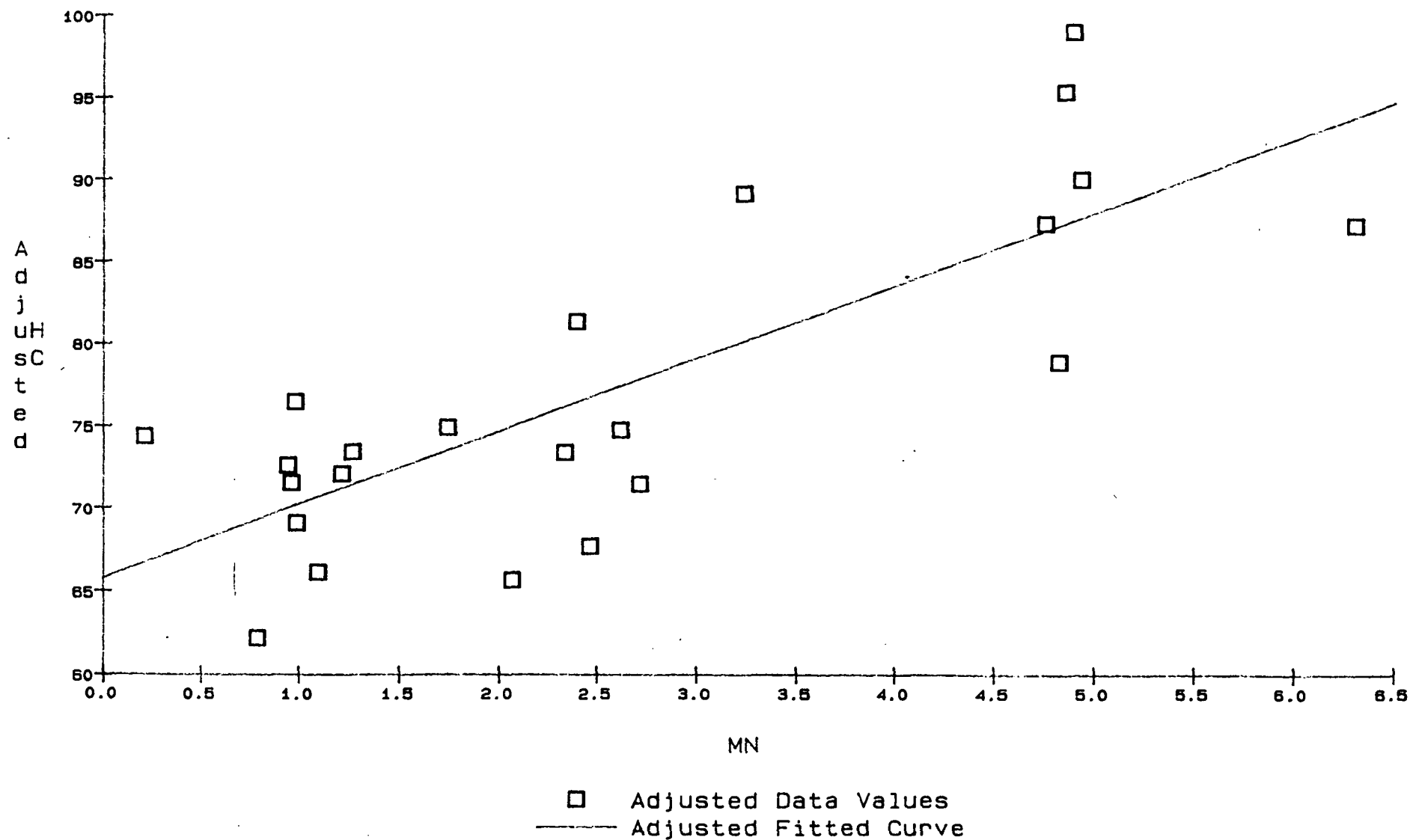


FIGURE 8

Graph: 49388

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CO vs NI, Adjusted for Remaining Predictors
Using Mulreg FORT1233, Model FORT12333

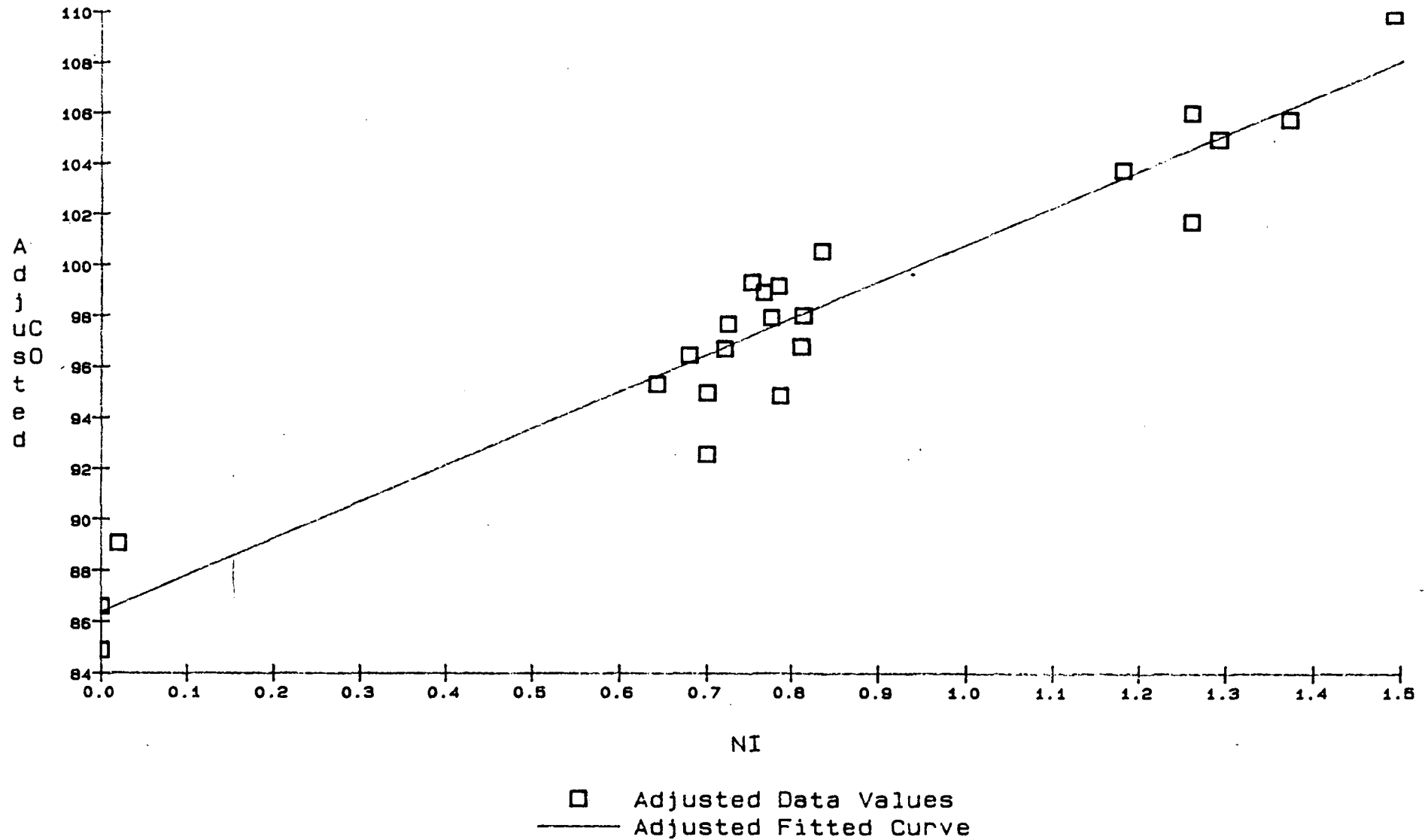


FIGURE 9

Graph: 49370

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CO vs MILES. Adjusted for Remaining Predictors
Using Mulreg FORT1233, Model FORT12333

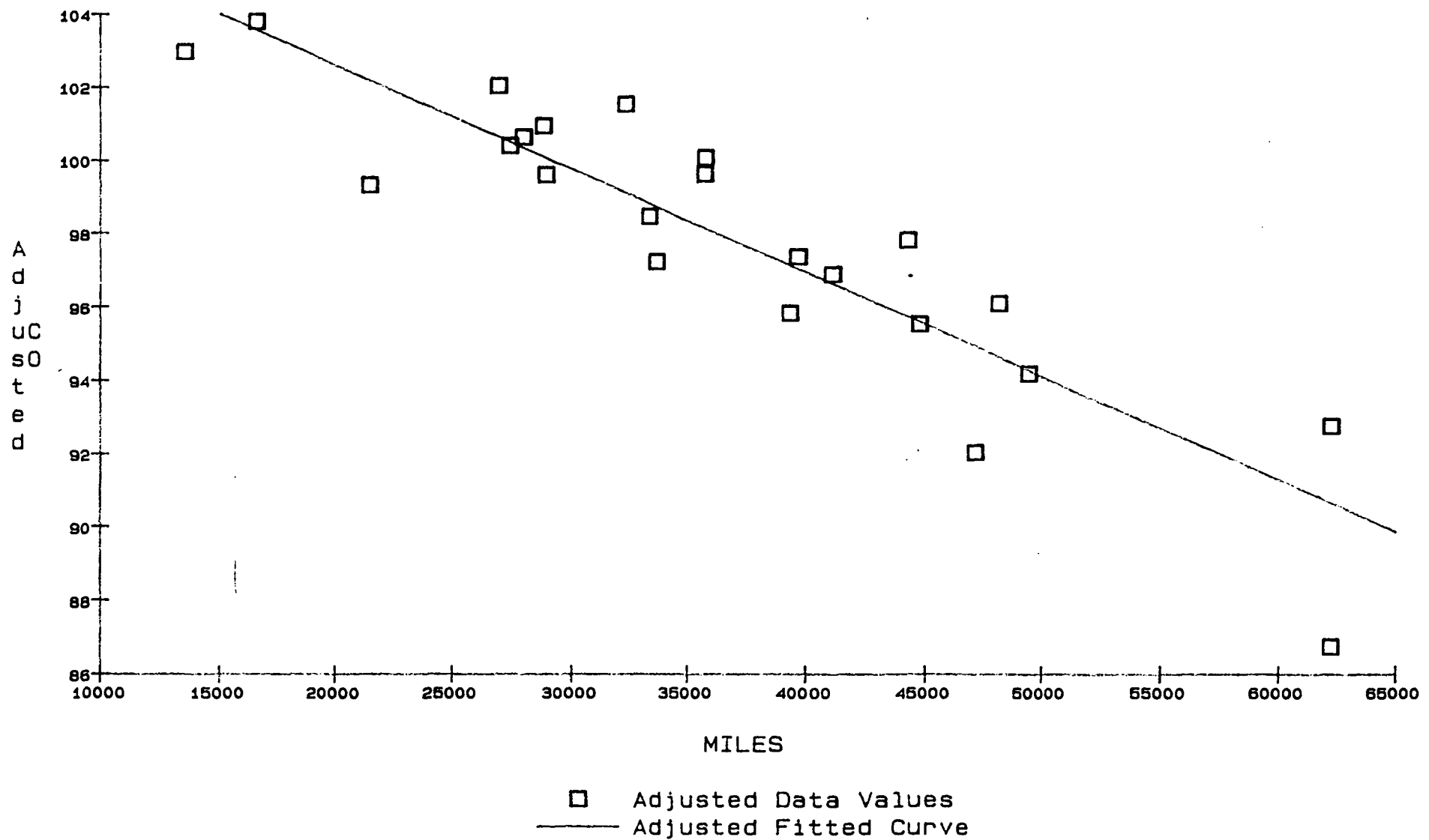


FIGURE 10

Graph: 49361

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CO vs MN, Adjusted for Remaining Predictors
Using Mulreg FORT1233, Model FORT12333

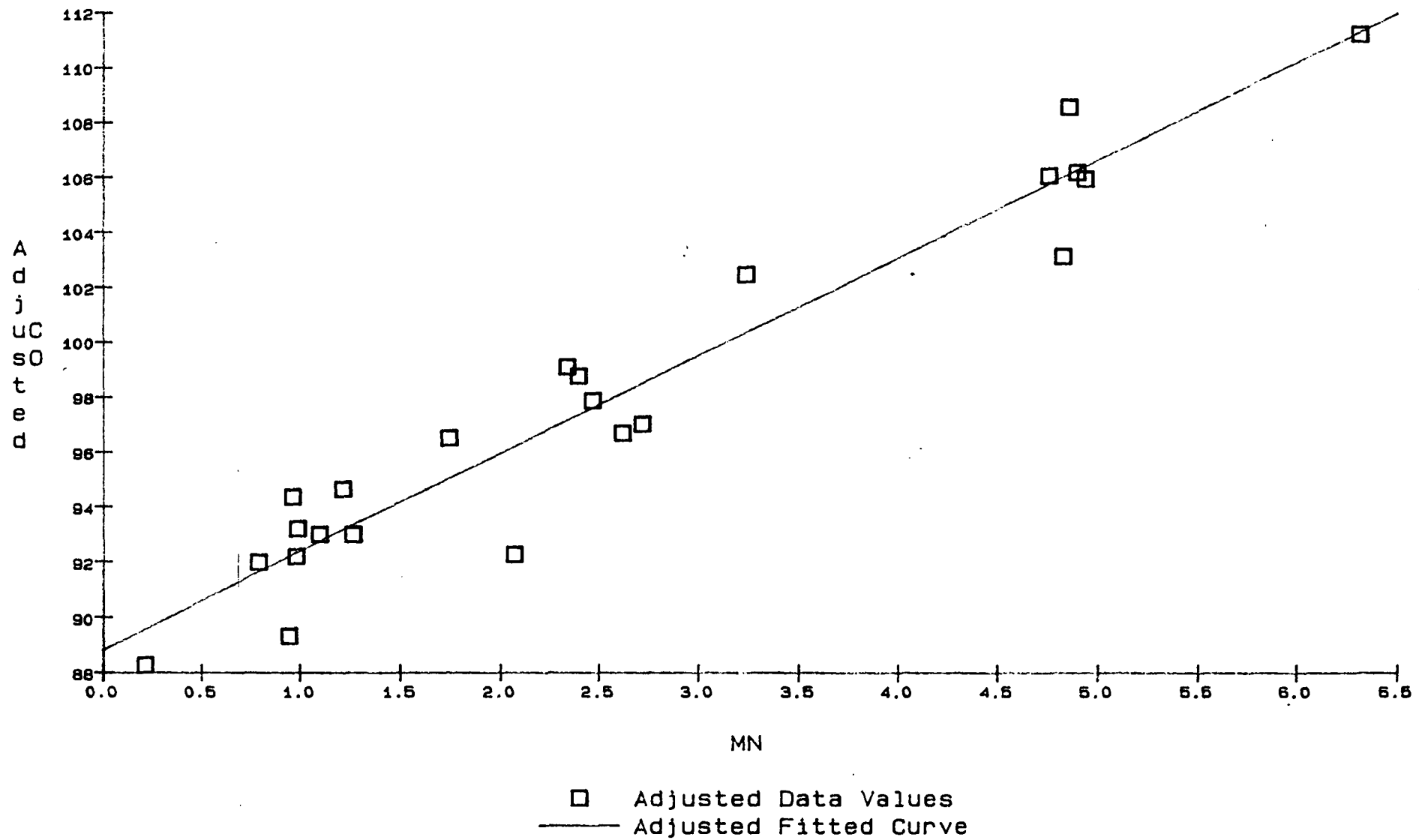


FIGURE 11

Graph: 49397

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CO vs CE, Adjusted for Remaining Predictors
Using Mulreg FORT1233, Model FORT12333

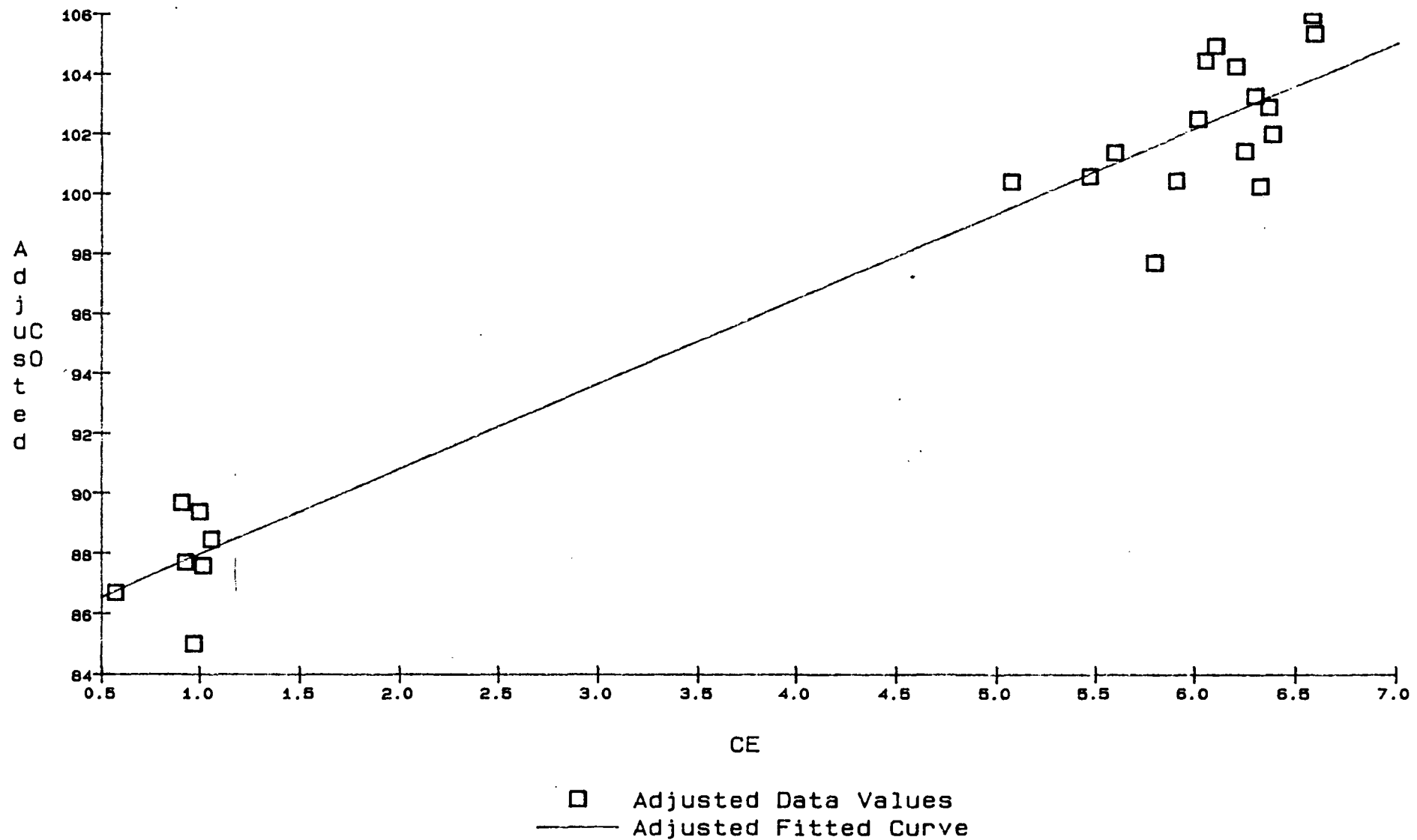


FIGURE 12

Graph: 49297

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CO vs M2_G, Adjusted for Remaining Predictors
Using Mulreg FORT1233, Model FORT12333

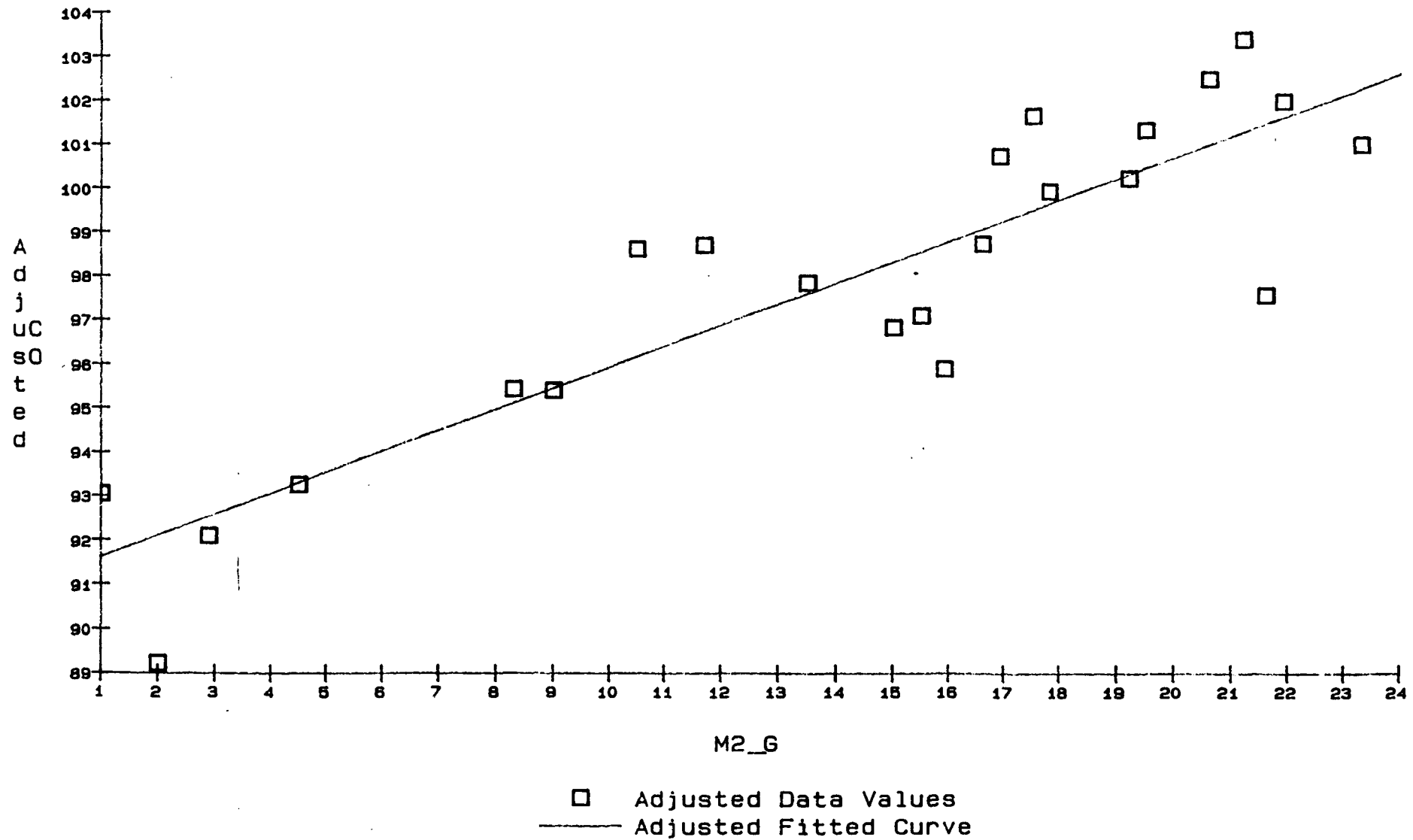


FIGURE 13

Graph: 49333

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CO vs FE, Adjusted for Remaining Predictors
Using Mulreg FORT1233, Model FORT12333

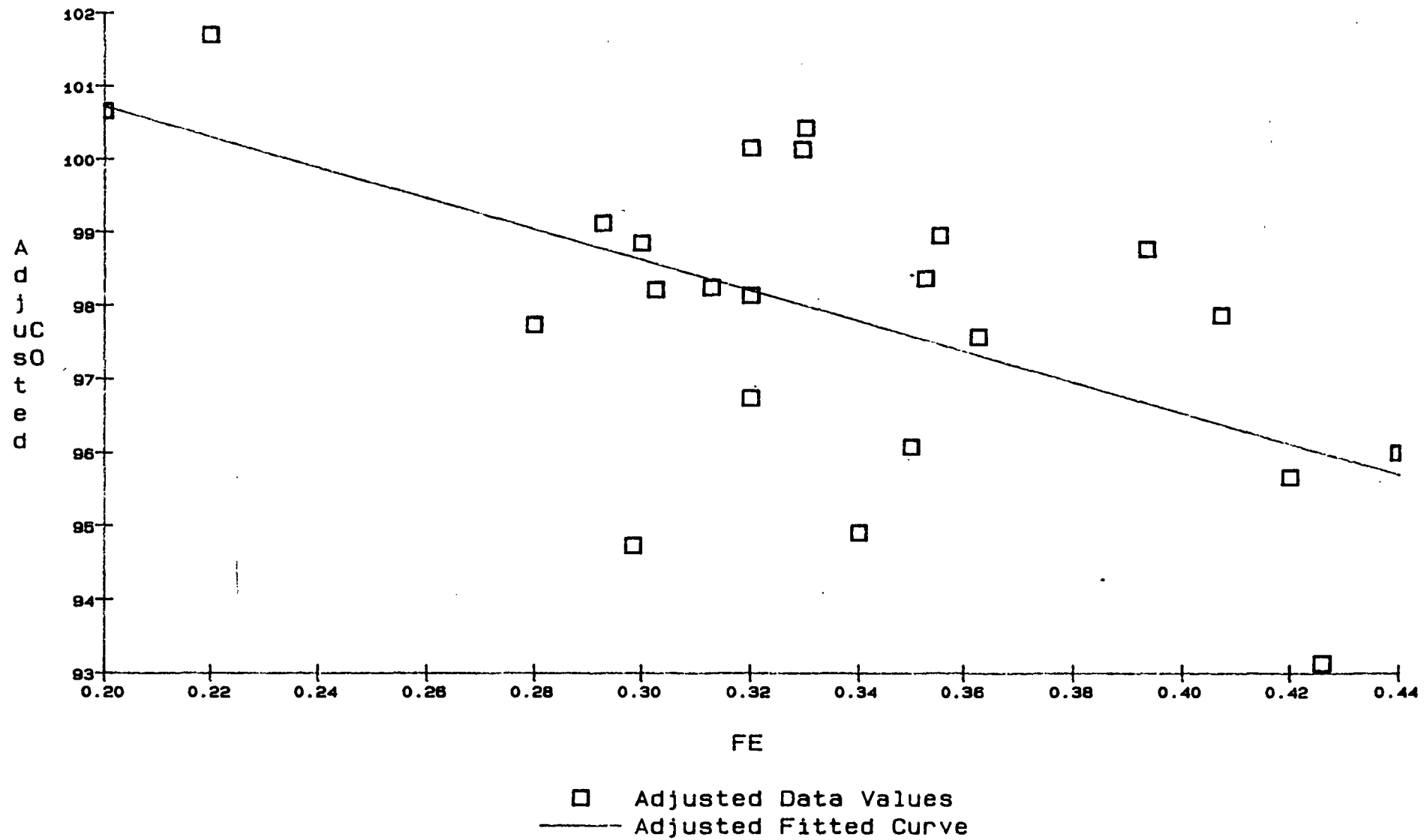


FIGURE 14

Graph: 49342

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CO vs ZN, Adjusted for Remaining Predictors
Using Mulreg FORT1233, Model FORT1233

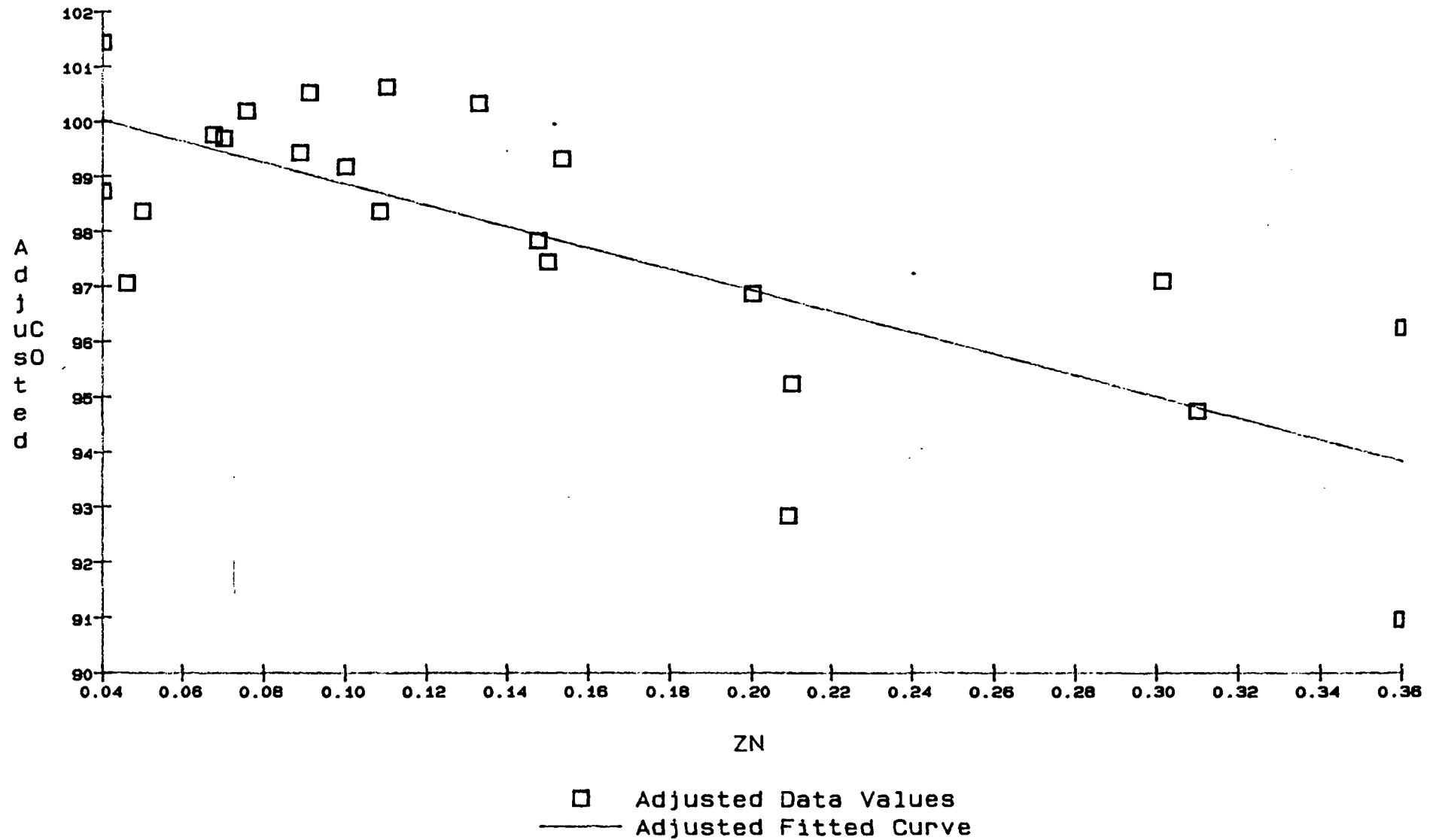


FIGURE 15

Graph: 49324

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CO vs BA, Adjusted for Remaining Predictors
Using Mulreg FORT1233, Model FORT12333

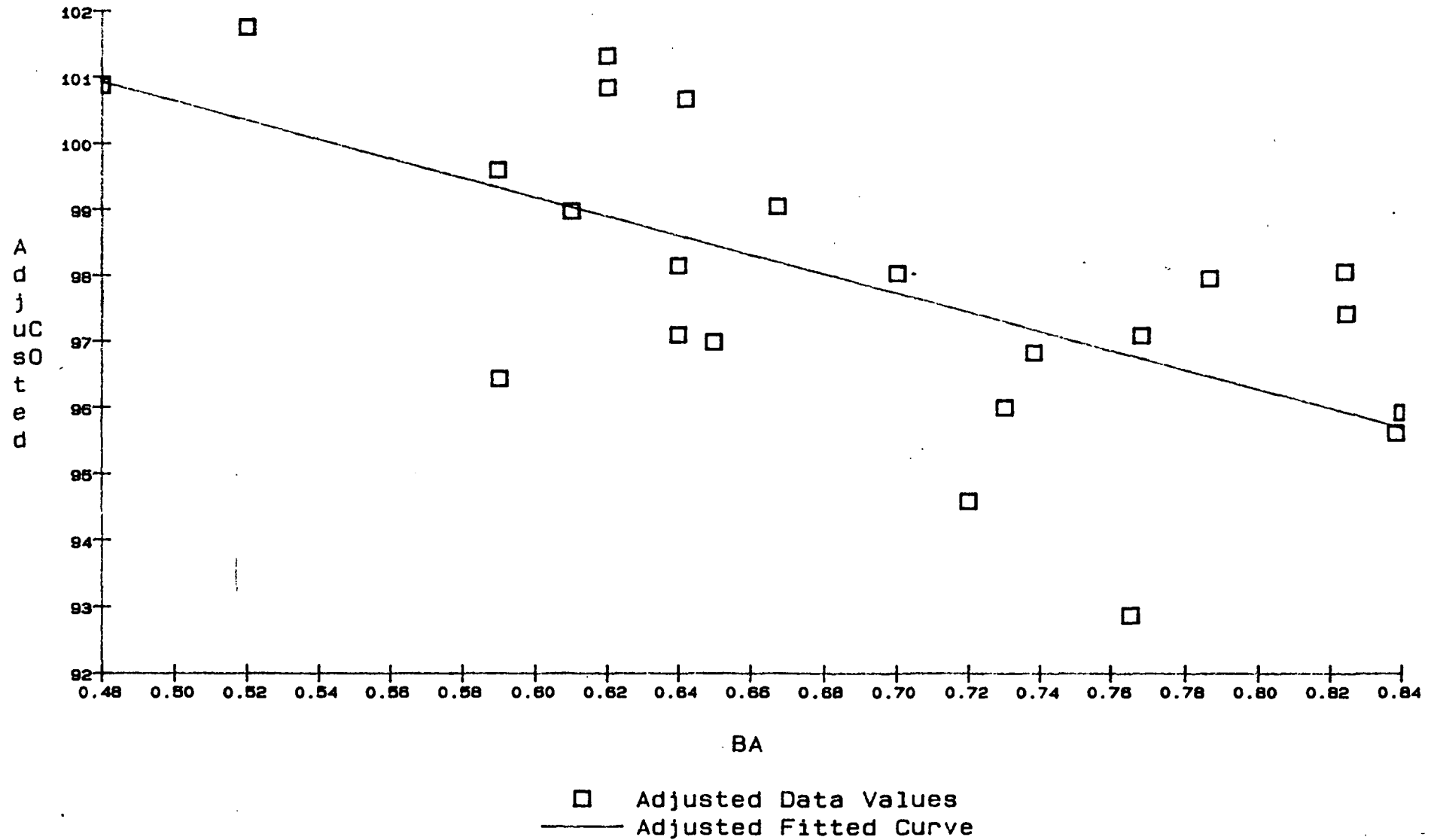


FIGURE 16

Graph: 49325

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NOX vs PB, Adjusted for Remaining Predictors
Using Mulreg FORT1233, Model FORT12334

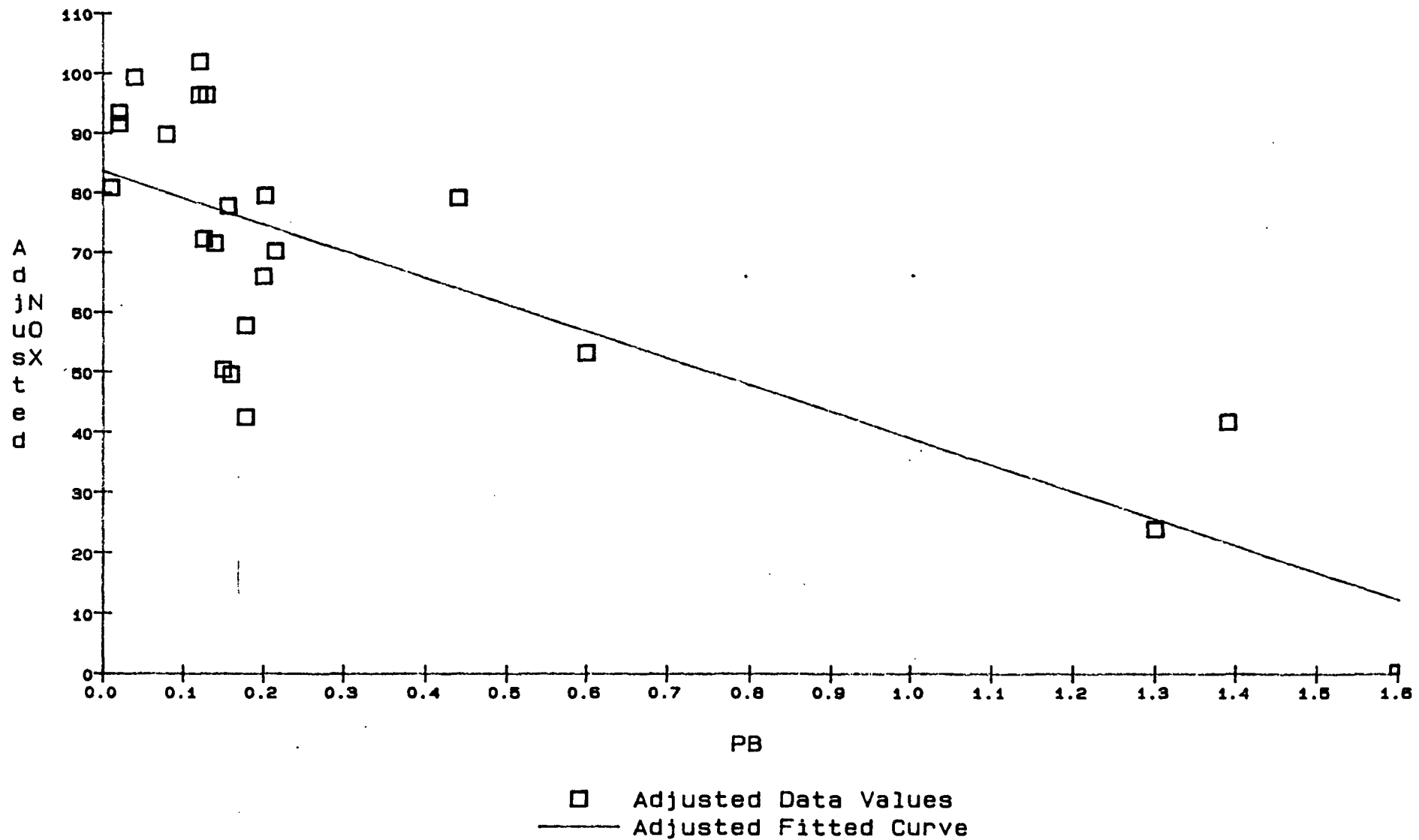


FIGURE 17

Graph: 49307

08-AUG-90 13: 27 Page 1

NOX vs NI. Adjusted for Remaining Predictors
Using Mulreg FORT1233, Model FORT12334

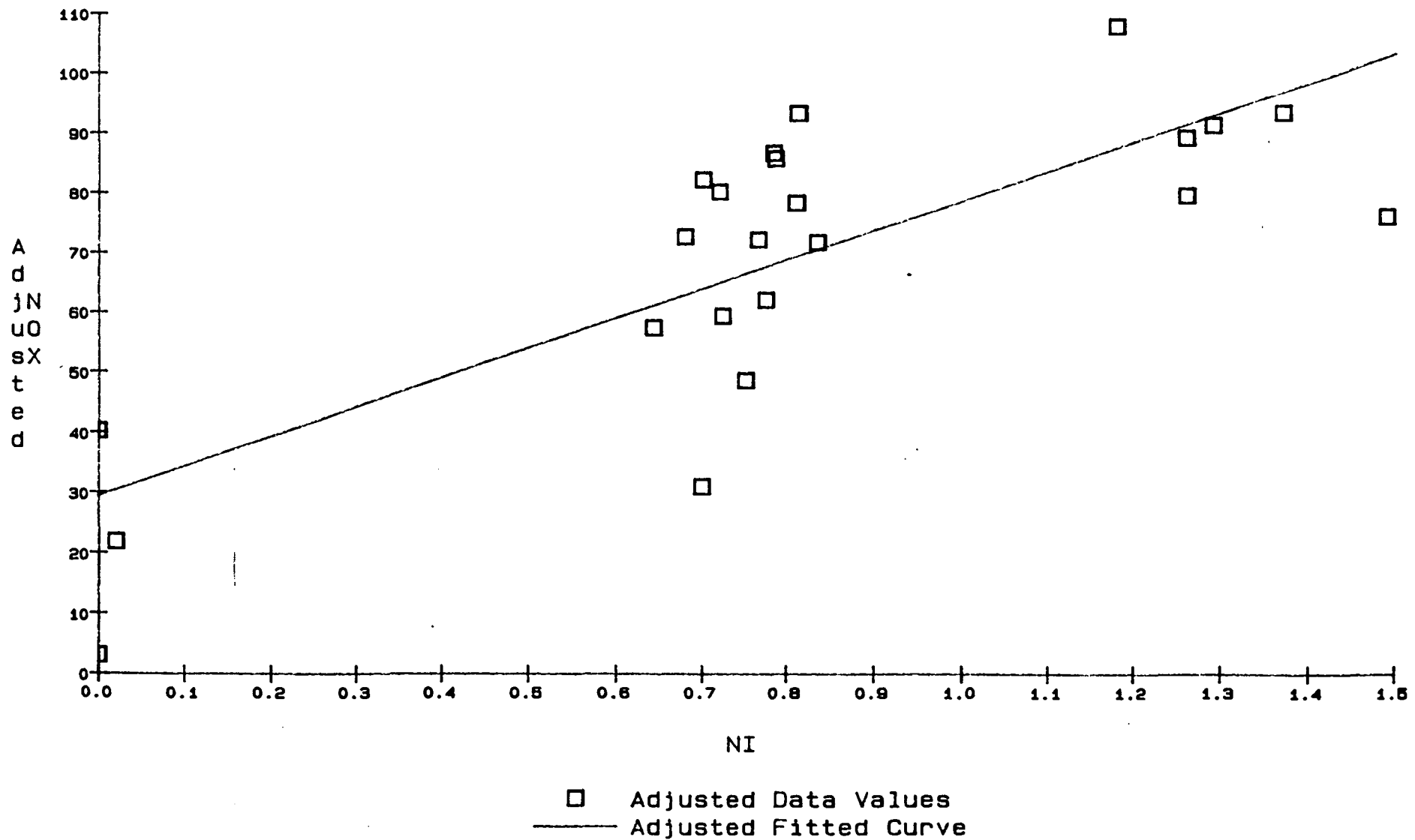


FIGURE 10

Graph: 49298

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NOX vs M2_G, Adjusted for Remaining Predictors
Using Mulreg FORT1233, Model FORT12334

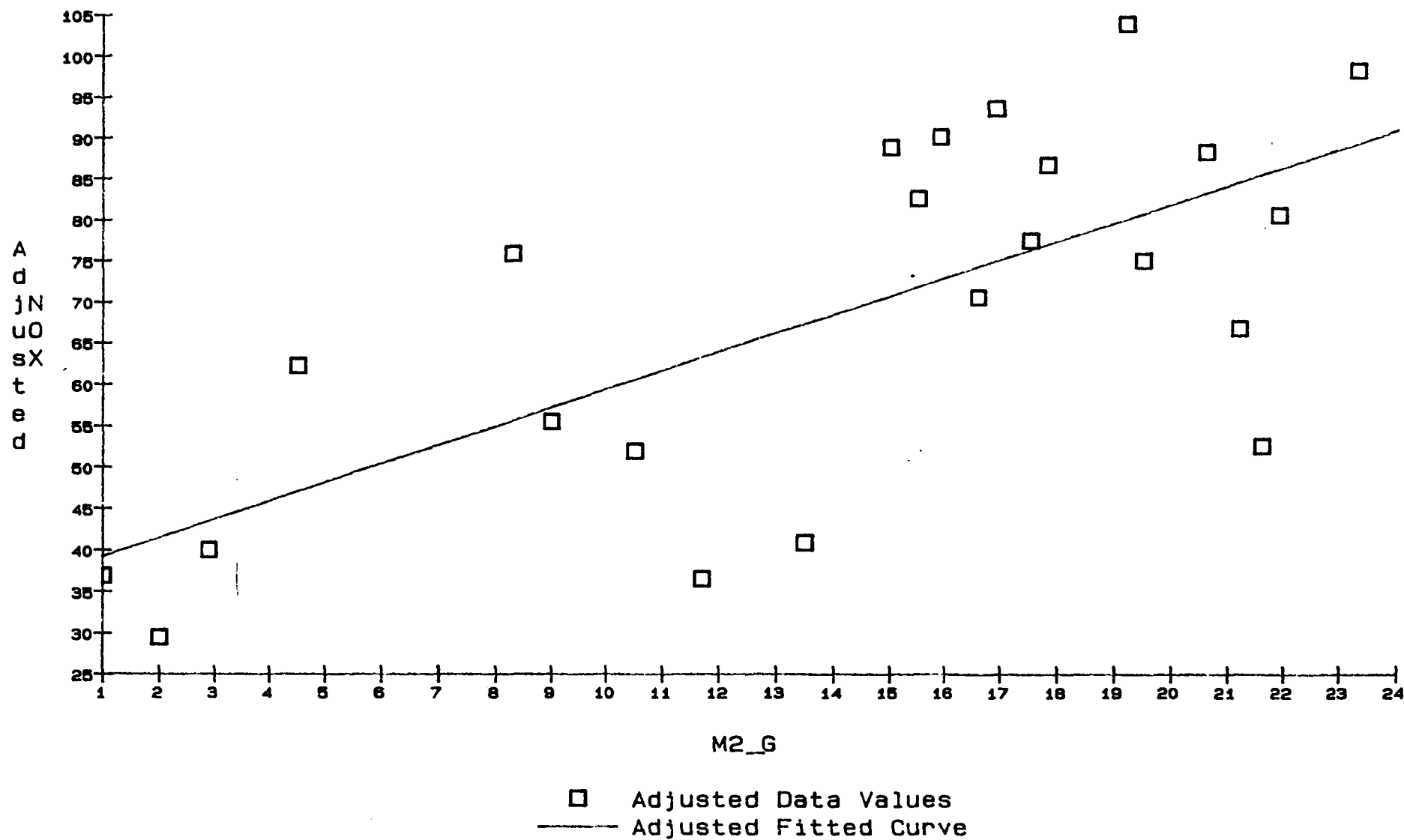


FIGURE 19

Graph: 49316

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NOX vs BA, Adjusted for Remaining Predictors
Using Mulreg FORT1233, Model FORT12334

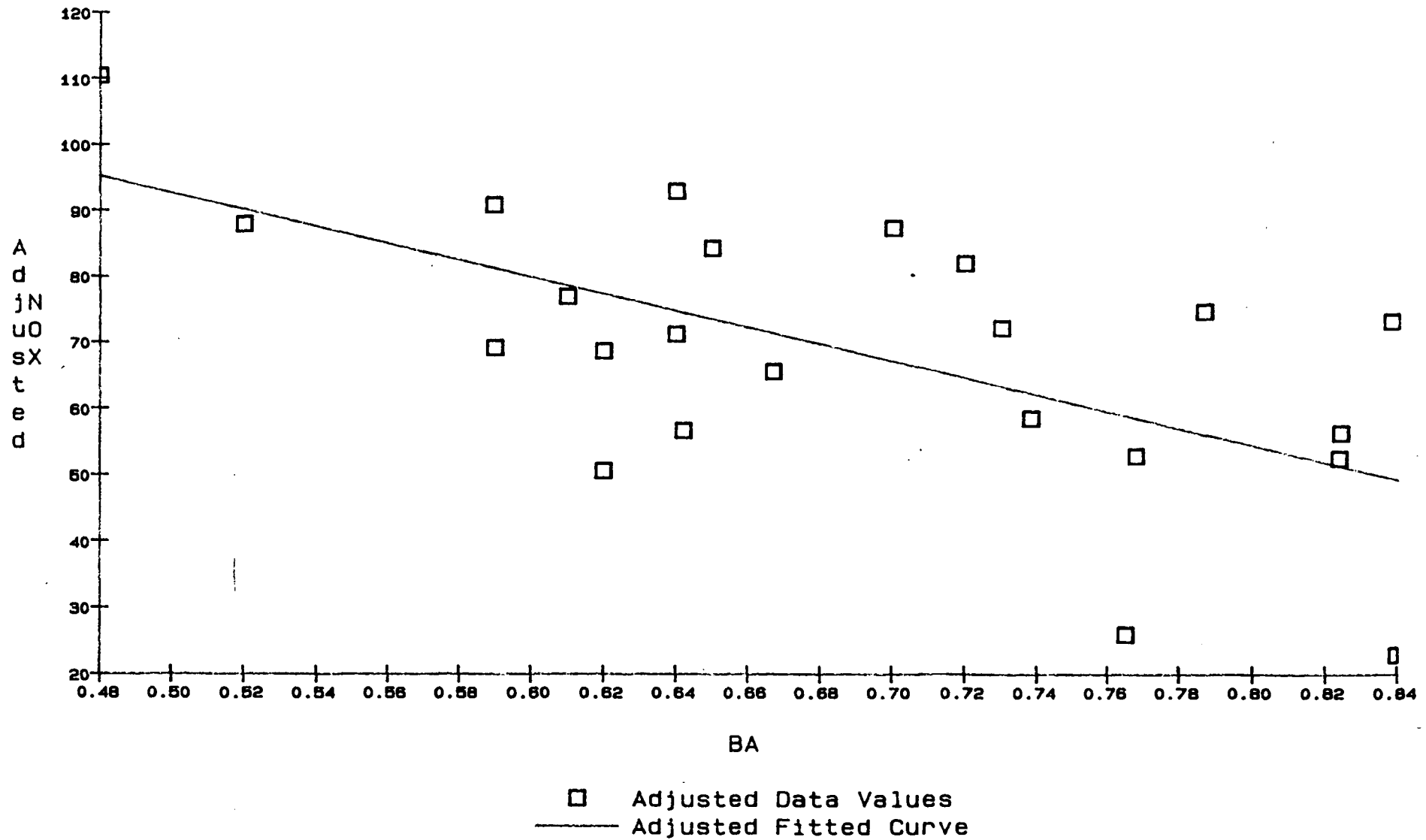
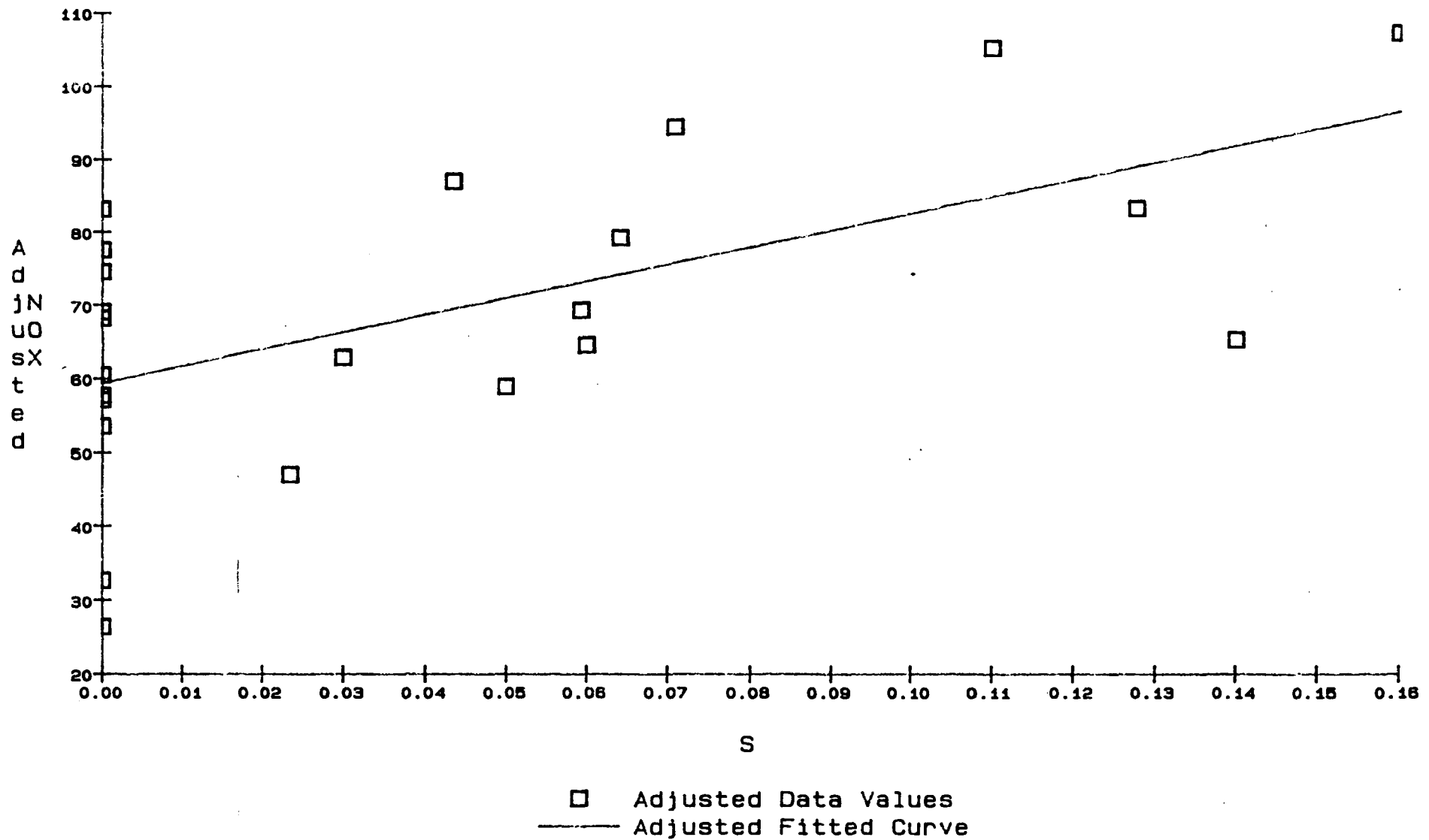


FIGURE 20

Graph: 49334

08-AUG-90 13:31 Page 1

NOX vs S. Adjusted for Remaining Predictors
Using Mulreg FORT1233, Model FORT12334



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Response to MECA Comments on Ethyl's Waiver Request for HiTec 3000

Prepared by Charles M. Heinen, Consultant

Comments were submitted by MECA on July 19, 1990 to the honorable William Reilly EPA Administrator on the subject of a fuel additive containing methylcyclopentadienyl manganese tricarbonyl (MMT) at the manganese level of 1/32 gram/gallon of unleaded gasoline. Ethyl Corp. has requested a waiver to market this fuel additive for unleaded gasoline under the trade name of HiTec 3000.

MECA indicated that there are five adverse effects from the combustion products of manganese which apparently worry their "catalyst experts".

1. Coating of active catalyst sites
2. Plugging or clogging of the small flow channels of a monolith catalyst.
3. Chemical reactions which reduce the catalyst surface area.
4. Deterioration and reduced thermal durability of ceramic substrates
5. Interference with improvements in precious metal/support interactions.

These fears include those expressed by other submitters in writing, and this response will include portions of their documents where appropriate.

Subjects 1 and 2 will be combined under the title of "Plugging of Active Catalyst Sites". Subjects 3 and 4 also will be combined under "Chemical Reactions, including those of Mn, which could affect catalysts".

Subject 5 is difficult for me since I am not gifted at clairvoyance or necromancy, but perhaps my views of "The future" will interest MECA and EPA.

Plugging of Active Catalyst Sites

The MECA comments on this subject are general and vague. For technical back-up they submitted a recent paper by Hurley et.al.¹

Response to MECA Comments on Ethyl's Waiver Request for HiTec 3000

— Prepared by Charles M. Heinen, Consultant

Abstract

A response to the MECA comment was prepared using industry data submitted to E.P.A. on the subject of HiTec 3000 and additional published information from the technical literature.

The analysis reported herein shows that at the exhaust temperatures of operation of the vehicles which were analyzed, the Mn exhausted from HiTec 3000 is in the form of Mn_3O_4 . In this form it does not enter into chemical reactions with catalyst components. It forms a randomly distributed coating which becomes modestly thicker linearly with mileage. The deposit is porous and does not affect exhaust reactions. The vehicles used for calculations were all Canadian, and all contained manganese, therefore, it was assumed that the level used for fueling was 1/16 gram per gallon or twice the level proposed in the HiTec 3000 waiver request.

Several reactions of Mn_3O_4 with catalyst components were postulated by MECA. All occurred at temperatures above which the catalysts suffer drastic decreases in surface area and catalyst activity so these reactions were not explained.

Several catalyst showed drastic losses in surface area and reactivity. The general subject of thermal reactions and their causes that might have resulted in the failures is discussed.

Some speculation on the future using appropriate obfuscation is included.

Response to MECA Comments on Ethyl's Waiver Request for HiTec 3000

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Plugging of Active Catalyst Sites

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from the Ford Motor Co. Their paper contains much of the type of technical information required to assess the role of the MMT additive in actual field operation. With the exception of the voluminous work by Ford reported in their submission of July 23, 1990 to docket no. A-90-16, there is little in the literature that permits analysis of the role, if any, of MMT in catalyst failures. These papers are a treasure trove for anyone interested in the subject.

Attachment 1 of the Ford submission details the test performed on 11 catalysts from ten vehicles driven normally by Ford of Canada employees. None had reported operational or mechanical problems. The vehicles were fueled with commercially available Canadian fuel presumably containing about 1/16 g Mn/Gal. In accordance with levels allowed by Canadian law (the Ethyl waiver request is for 1/32g Mn/Gal.) Ford states, and we agree that the contaminants in deposits on the catalysts, such as Pb, S, P, and Zn are within normal ranges. None of the catalyst showed any sign of thermal distress, in short this should be a normal customer fleet. It will be referred to as "11 Catalyst Fleet".

The second fleet contained 9 vehicles, some with single and others with double brick configurations. As a result it yielded 15 catalysts. Nevertheless, it is referred to as the "9-Catalysts Fleet" in this document. The catalysts in this fleet were removed because of suspected catalyst defects. No information was submitted on the fueling characteristics of the fleet. Therefore, it was concluded by the authors, and necessarily by me that normal Canadian fuel containing 1/16 gMn/gal as MMT was used. The fleet was the subject of the paper by Hurley et.al. referred to above. One apparent over temperature condition was observed in one catalyst, but no other signs of catalyst damage were observed. Compared to Fleet Eleven, the catalysts appear to have suffered moderately severe treatment.

The third fleet contained 26 catalysts from 13 vehicles. All were of the two brick configuration. (Each brick is treated separately.) It is referred to in this document as the "26 Catalyst Fleet".

The converters in this fleet were sent in because of "poor performance" and/or driveability problems. As in the previous vehicle set, no information on fuels used was available so 1/16 g Mn

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was assumed. In one catalyst (#100) there were indications of severe over-temperature conditions. The rear portions of bricks 1 and 2 were broken and melted according to the Ford report. In another, there was only one brick and it had been reduced to baseball size, presumably as the result of abrasion. A third (#103) had an incomplete data set. A fourth catalyst (#106) had all the indications of a nearly new catalyst even though the vehicle had 33,000 mile. Consequently, the data from 102,103 and 106 were not used in our data analysis. The conditions in this fleet appear to have been severe.

All reports from the auto companies and others agree that the catalysts are covered with a reddish coating of varying thickness which sometimes leads to erroneous first impressions. The Hurley et.al report on page 5 is more detailed, specifically they state:

These results confirm earlier experimental results (3,5) in that the Mn derived from MMT is converted in the combustion process exclusively to Mn_3O_4

Optical micrographs (figures 3 and 4) of catalysts, 301G and 301I, show a heavy residual layer covering the washcoat. X-Ray fluorescence results indicate that these two samples, contain approximately 4 and 6 wt% of Mn, respectively and are from vehicles with 22,000 and 33,000 accumulated in-use miles. As is evident in both of the high magnification micrographs, from 301G and 301I, the Mn_3O_4 is on layered on the surface of the washcoat. It does not appear to penetrate or have reacted with the washcoat but simply adheres to the surface. This deposit of Mn_3O_4 on the washcoat may cause physical pore plugging and thus result in mass-transfer problems.

Scanning Electron Microscopic and Electron Probe analysis show the thickness of the Mn_3O_4 residual layer to range from approximately 5 microns to a maximum of approximately 20 microns. The thickest layer is observed on catalyst 301I which had 33,000 accumulated

miles. SEM micrographs (figure 5) of cross-sections of 301G and 301I show this layer quite distinctly. Also shown in this figure is a Mn x-ray elemental map pattern to confirm that the layer is indeed rich in Mn. This elemental map is used to determine the actual thickness of the Mn rich region on the washcoat. This micrographs also indicate little if any penetration into the washcoat by the Mn rich layer. Indications from the surface morphology study is that the Mn rich layer does simply adhere to the surface of the washcoat. An example of the surface morphology of the Mn rich layer is shown in figure 6. As is shown in the micrograph the surface is covered with a layer of fluffy, porous material. This material was confirmed by XRD to consist exclusively of Mn_3O_4 .

The underlining is not in the original text. These comments were valuable for evaluating the qualitative information supplied by Ford and others. The comments and quantitative data supplied by Ford were used extensively in order to answer the following questions:

- A. Do the Mn_3O_4 deposits continue to grow with exhaust flow or do they reach an equilibrium level?
- B. Are the deposits stable (on the surface) or do they react?
- C. Are the deposits truly porous or do they restrict the the catalyst effectiveness?

Question A

Ford did extensive X-ray fluorescence analyses of the components and the contaminants. They sectioned the various bricks and obtained the composition of each, so that 3 analyses are available for each brick of the 9-catalyst fleet and the 26 catalyst fleet. The data were analyzed to determine whether averaging the three sections yielded substantially different results than the averages when compared with other variables. They did not. Apparently, Ford reached the same conclusion because the 11 Catalyst Fleet paper reported only single numbers for consistency and simplicity. All graphs in this presentation use only averages where more that one number is available for a single brick.

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Graphs 1,2, and 3 show the result of plotting Mn (weight percent) found on the catalyst against vehicle mileage. There is considerable evidence of an increase of weight percent Mn increase with mileage. There was too much data scatter to make reasonably quantitative estimates of the rate of increase.

This is not too surprising when within the three fleets we find variables in engine sizes for each fleet and therefore in probable variations in exhaust flow rates, and in number of bricks in the systems (1 or 2). Finally, the three fleets have different mileages.

In order to reduce the number of variables, the following steps were applied:

1. All Mn (weight percent) values for each catalyst car in each fleet were averaged.
2. Where a one brick system is used its value is divided by 2 in order to compare it with 2 brick systems.
3. Since the bulk of the vehicles contained 2.3 Liter engines the entire fleet was made to simulate a 2.3 Liter engine by multiplying the value of the ratio 2.3 Liters/X where X is the value in liters of the engine involved.

When these admittedly rough corrections were made linear relationships of catalyst Mn concentration versus miles were established for each fleet. This is shown in graphs 4,5, and 6. The values for these graphs were combined into graph #7.

This graph shows two very significant facts:

1. The rate of increase of wt% Mn is approximately constant.
2. Even with many unknowns a rate of the deposit can be quantitatively estimated for ceramic monolith catalysts such as are used in the Ford systems studied. For the values plotted the percent increase in weight percent of Mn is between 0.03 and 0.05 per 10,000 miles.

Question B

The next important question is whether this material lays on the surface or whether it reacts with the substrate or the washcoat. Since no specific information was available on these reactions, the

approach used was to attempt to find a "tracer" and to compare the ratio of this tracer to Mn at various locations to see if the ratios change substantially. If there was a major change in ratio a reaction would be suspected or established. If not, a reaction of the Mn_3O_4 with the rest of the catalyst would appear unlikely. Of the tracer possibilities available in the data, lead and phosphorous appeared the most useful. Graphs 8,9, and 10 represent the ratios between Mn and Pb contents in the various catalysts. A good relationship exists but there is considerable scatter. Graphs 11,12, and 13 show less scatter for Phosphorous so this was used in the ratio comparison. Table 1 shows the ratios of Mn weight percentage to P weight Percentage multiplied by 10 for convenience. This table covers the 9 car fleet. Table 2 shows the ratios for the 26 catalyst group. No statistical analysis of the ratios was performed because observation shows that any variation in the ratios is within the analytical accuracy of the methods used. Variations in the ratio occur randomly in the front middle or back of the first brick where Mn concentrations are highest. they also occur randomly in the front middle or back of the second brick where Mn concentrations are lower. This established that the Mn_3O_4 , a very stable compound, does not take part in any reactions.

Question C

The third question to be answered is: Are the deposits truly porous or do they restrict the exhaust gas reactions that should occur in the catalyst?

Extensive surface area measurements were made by Ford using the B.E.T. surface area technique. It is reasonable to conclude that if the Mn_3O_4 is not porous, there should be a relationship between Mn_3O_4 and B.E.T. values. In other words, the higher the Mn weight percentage values, the lower the B.E.T. should be. Chart 14 is a comparison of all the points available in the reports. There are many points since Mn and B.E.T. were taken on the brick slices. In this case the profusion of data is not very enlightening as far as establishing a relationship is concerned. In fact a lack of correlation is shown.

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The various groups of data were then analyzed. Graphs 15, 16, and 17 show the result. Again there was no correlation but an interesting fact emerged. The 11 Car group showed exceptionally high B.E.T. surface areas. The observations on Page 4 of Ford Attachment 2 led me to draw a line at B.E.T. values of $5.0 \text{ M}^2/\text{g}$ to indicate an unacceptable catalyst as defined by the Ford investigators².

Graphs 18, 19, and 20 show the relations between mileage and B.E.T. They bring no enlightenment on the cause or catalyst deterioration. It is clear from those graphs Mn_3O_4 does not cause macro or micro plugging which affects catalyst reactions at the Canadian concentrations of 1/16 gram of Manganese per gallon. Since there is no correlation between B.E.T. area and Mn concentration.

Based on the foregoing data it seems that:

1. The Mn_3O_4 formed, apparently at some point prior to the catalyst, slowly forms deposits on the catalyst at a constant rate.
2. There is no indication, however, that Mn_3O_4 enters into any chemical reactions within the catalyst.
3. The Mn_3O_4 coating is apparently porous, and does not appear to interfere with the area on which the chemical reactions of exhaust pollutants occur.

If Mn_3O_4 does not cause the reduction of chemical activity, what does?

CHEMICAL REACTIONS INCLUDING THOSE OF Mn, WHICH COULD AFFECT CATALYSTS.

Perhaps the best place to start is with the full quote of the paragraph on page 4 of Ford attachment 2 referenced earlier.

X-ray diffraction analysis of samples from vehicles with accumulated mileage in the ranges of 10K to 40K, 21K to 30K, 31K to 40K, and 41K to 50K showed that samples

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#107, #108, and #109 had the α -alumina phase present. This α -phase indicates that these catalyst had undergone exposure to temperatures $>1000^{\circ}\text{C}$ at some time during their operation. Sample #112 from the 31-41K mileage range did not show the α -alumina phase present. X-Ray diffraction analysis also confirms the rust colored residue to be Mn_3O_4 .

B.E.T. surface activity measurements on the second series (Table 3) range between 1.25 and 22.56 m^2/g for the first brick and between 0.61 and 21.61 m^2/g for the second brick. Catalysts #100, #108, and #110 have B.E.T. values below 5 m^2/g which indicates their exposure to operating temperatures greater than 1000°C . These values confirm the XRD results. Catalyst #103 had only one brick which had been abraded to the size of a baseball but still had a B.E.T. value of 9 m^2/g . In comparison, in-use vehicles having BET's greater than 5 m^2/g are considered acceptable and BET's for fresh catalyst fall in the range of 25 m^2/g .

The underlining has been added to emphasize certain points.

The reactions in a catalytic converter are, generally, strongly exothermic, since both carbon monoxide and hydrocarbons give off considerable heat in their oxidation as can be seen by consulting any standard reference. Actually NO formation requires a small amount of heat. As can be seen from reading exhaust analyses reported by various authors it is apparent that the HC contents of exhaust gas are small compared to the CO content, therefore the temperature of the exhaust gas is dependent on: inlet temperature to the reactor and combustion of percent CO X 155°F temperature loss through the reactor.

The derivation of the factor of 155°F per percent CO combusted is described in SAE paper 486J³. The "reactor" could be the manifold as is the case with thermal reactors, the catalyst or even the engine itself.

We will not discuss engine exhaust temperatures, but starting with the engine exhaust there will be some additional clean-up in the muffler if the time and temperature conditions are right. SAE paper 486G⁴ deals with these reactions. According to this reference a minimum of 1200° F is required to initiate this reaction, and about 4% CO is required to maintain it.

SAE paper 486J describes the thermal conditions for 1.5% by volume of CO (the then existing California standards) and shows that they ranged on the average from 950° F at the manifold to 700° F for catalytic muffler inlets 100 inches removed from the manifold outlets. This is in good agreement with data presented in SAE paper 760781⁵ where exhaust outlet compositions average at least 1% CO less so that about 155° F should be removed from these values. In other words about 800° F to 650° F should be the current inlet temperatures. Experience has shown that average catalyst intake temperatures range around 650° F. this then is the gas with which the catalytic converter operates.

Catalysts of the types described usually consist of a ceramic substrate of Cordierite ($4(\text{Mg,Fe}) 0.4 \text{ Al}_2\text{O}_3 \cdot 10 \text{ SiO}_2 \cdot \text{H}_2\text{O}$). The surface area is insufficient so a "wash-coat" of Gamma alumina is washed over and through the Cordierite to provide very large surface areas of the order of 100-200 square meters per gram. The precious metal catalyst is distributed throughout the wash coat and has general access to the exhaust gases.

For thermodynamic reasons nature abhors large surface areas and under various conditions will move to decrease them. Well known examples of this phenomenon are grain growth in metallurgy and crystal growth in solutions. Gamma Alumina is no exception. At temperatures ranging somewhere from 950° F to 1800° F (1000° C) the gamma alumina converts to alpha alumina which has a much lower surface area. The extent of conversion depends on temperature and time at this temperature. The catalytic effect depends on the rate of reaction.

Figure 21 compares the average B.E.T. values with light-off temperature values derived from graphs submitted by Ford for the

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11-Catalyst Fleet and the 26-Catalyst Fleet. The light-off point was an estimate which attempted to show where a change in the rising concentration occurred. Since each of the curves in the 26-Catalyst fleet had different shapes the points could vary somewhat. The values at the light-off point for the HC and NO conversion are shown under the estimated "light-off" point for the 26-Catalyst Fleet and one doubtful point on the 11-Catalyst fleet. Other conversion values were not shown for the 11 Catalyst fleet because all were about 80% for HC and 90%+ for NO.

None of the CO points were recorded, since they were in the 90%+ range for both fleets at the light-off points. Figure 21 shows that the vehicles from the 11-Catalyst Fleet have little loss in reactivity or surface area, whereas both the 9-Catalyst Fleet and the 26-Catalyst Fleet show extensive loss in surface area and reactivity. This is presumably because of over-temperature conditions since it has been established that MMT is not a factor in the loss of surface area.

From previous data cited above it can be concluded that the catalysts were operating in CO concentrations of 2-6% for considerable periods of time to accomplish the temperature deterioration shown.

The MECA submissions on page 3 shows some concerns about reaction with the cordierite which occur at temperatures ranging from 1475° F to 2456° F (800° C to 1347° C). These appear to be technically interesting but also to be non sequiturs because of the fact that the active surface of the catalyst would have been fatally altered before these temperatures were reached.

The question that arises from all of this, is what caused the excessive temperatures? Was there some other cause of catalyst failure? There can be no serious suggestion that abnormal catalysts were at fault for the catastrophic results reported by Ford. First of all, there was no general pattern of distribution of the area of operation and no indication that they were all from the same time of manufacture. Furthermore, the 11 Catalyst Fleet and the Ethyl Waiver Fleet along with extensive other testing has demonstrated consistently good performance when all of the factors that affect

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engine and engine controls performance are according to specification. This includes particularly the oxygen sensors.

Unfortunately, the oxygen sensors for the 26 Catalyst and 9 Catalyst Fleets were not examined. They were not available for the 26 Catalyst Fleet which is probably the case with the 9 Catalyst fleet. The sensors for the 11 Catalyst Fleet were sent to Robert Bosch Co. for detailed analysis. According to Bosch all were within specification for functioning oxygen sensors, but two showed "abnormal behavior" (unspecified type). They were from vehicles BK7 and BK9. BK7 also showed a loss in B.E.T. level. Two questions arise:

1. Is the "abnormal behavior" in any way related to MMT?
(Probably not in view of the excellent performance of oxygen sensors in the Ethyl Waiver Fleet.)
2. Are the specification limits for what constitutes a functioning oxygen sensor too broad?

Detailed clarification of these two questions from Robert Bosch Co. would certainly be helpful.

Similar questions about field failures of oxygen sensors should be asked of Bosch and the automobile manufacturer. Finally, MECA should be asked to elaborate on "undesirable reactions" which concern their "catalyst engineers"?

I wish to express my thanks to the various submitters, and particularly to the Ford Motor Company for their extensive and detailed evaluation of field vehicles. Their data made it possible to answer the MECA concerns scientifically rather than add more oratory to the docket.

The Future

The speculation about future standards is difficult to address because they have been in the discussion phase for about ten years.

There are two possible effects on the exhaust reaction conditions that may result from lowering present standards:

1. The catalysts may be coupled directly to the exhaust manifold. Since catalysts are currently coupled as closely as 8 inches from the manifold, temperature increases of not more than 25° F could be experienced, based on the temperature reductions along the exhaust system shown in the references cited. This is well within the variations in temperature that will occur as a result of operational variables such as ambient temperature or traffic conditions.
2. As cited previously, the only other theoretical effect would be from more combustion in the catalyst as a result of lowering the standards. As has been pointed out the only important factor in raising catalyst temperature is the CO combustion. Since well over 95% conversion of this compound is currently being accomplished the difference of a couple of percentage points is all that we are talking about. Converted to catalyst temperatures this will not be more than 5° F.

Thus, it is quite obvious that no substantial increase in catalyst temperature can be expected. In a way, this is unfortunate, because higher temperatures promote higher conversion rates. Even such desperation moves as heated catalysts have been proposed, but when you are at 95% or more conversion additional improvement becomes very difficult to accomplish or even measure.

I expect that further improvement in the engine output as a result of modifications of the injection systems and the oxygen sensors and other engine components will result in cleaner exhaust stream to the catalysts. The catalysts themselves will probably be improved as a result of continuing production control efforts. The combination will possibly result in meeting some of the more reasonable proposed reductions.

At this point the evaluation techniques will probably need to be revised. New traffic cycle studies will have to be made since the ones on which present evaluations are made are 25 years old and undoubtedly outmoded. New instrumentation may need to be developed. Even though the atmosphere may only experience a 5% reduction or less in pollutants as a result of a proposed new

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regulation, the instrumentation will be asked to analyze a 50% reduction of the concentration in tailpipe emissions that it is presently analyzing.

Atmospheric measurements are currently incapable of evaluating the major changes that have been made, so a large program in this area is called for.

These seem like huge programs, and they are, but the new standards proposed involve expenditures of billions of dollars per year, and these steps will be required to see if the American public is getting its money's worth.

These then are some of my speculations on the future. Consulting Nostradamus may be more productive.

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S.A.E. Paper 486J "Thermal Considerations in Exhaust Emission Control Systems," C.M. Heinen. March 1962.

S.A.E. Paper 486G "Development of Flame Type Afterburner," J.W. Schnabel, J.E. Yingst, L.M. Heinen and W.S. Fagley. March 1962.

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Graph 1

9-Catalyst Fleet

4.0

3.0

2.0

1.0

0

10

20

30

40

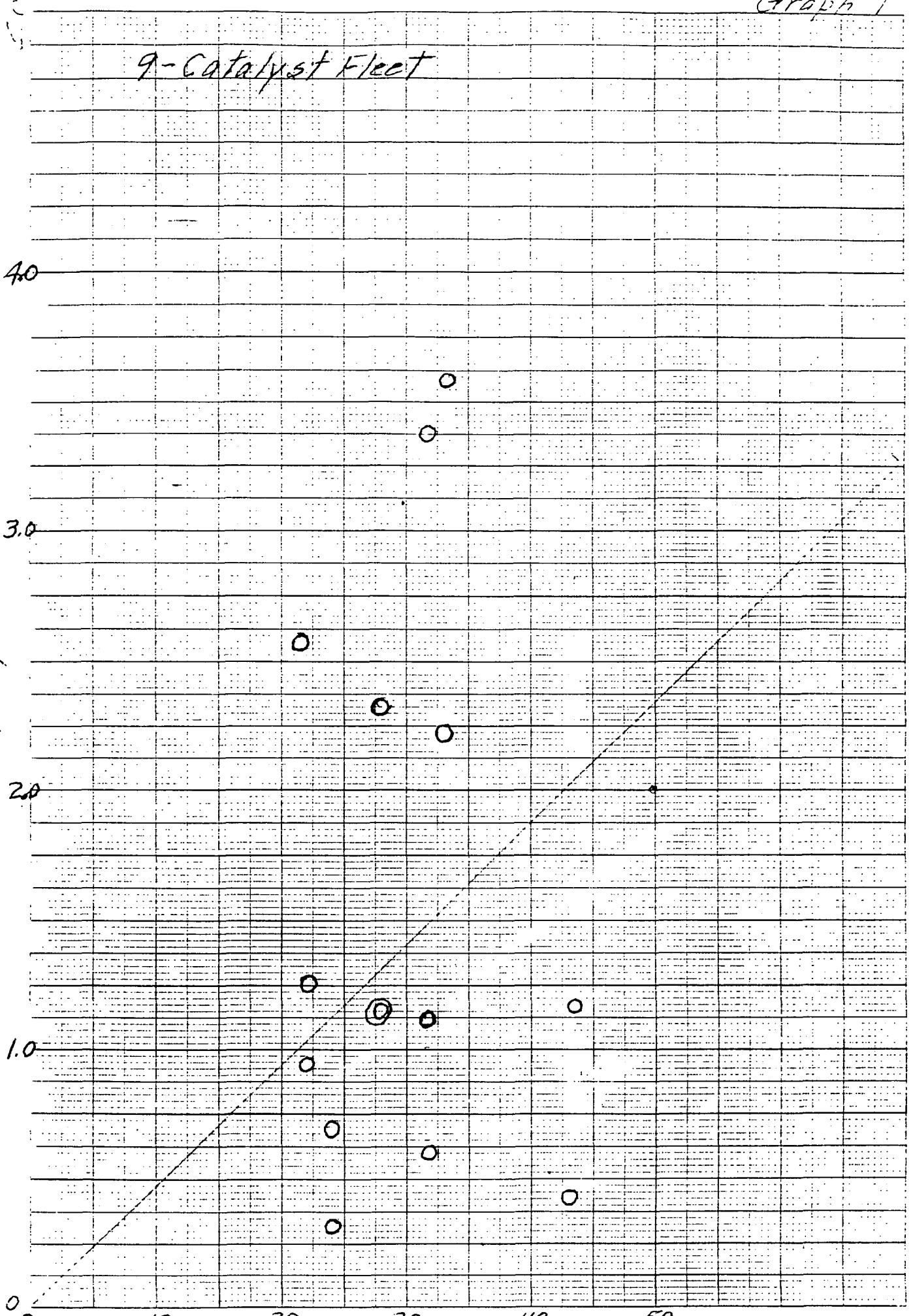
50

Miles ÷ 1000

Mn, wt of

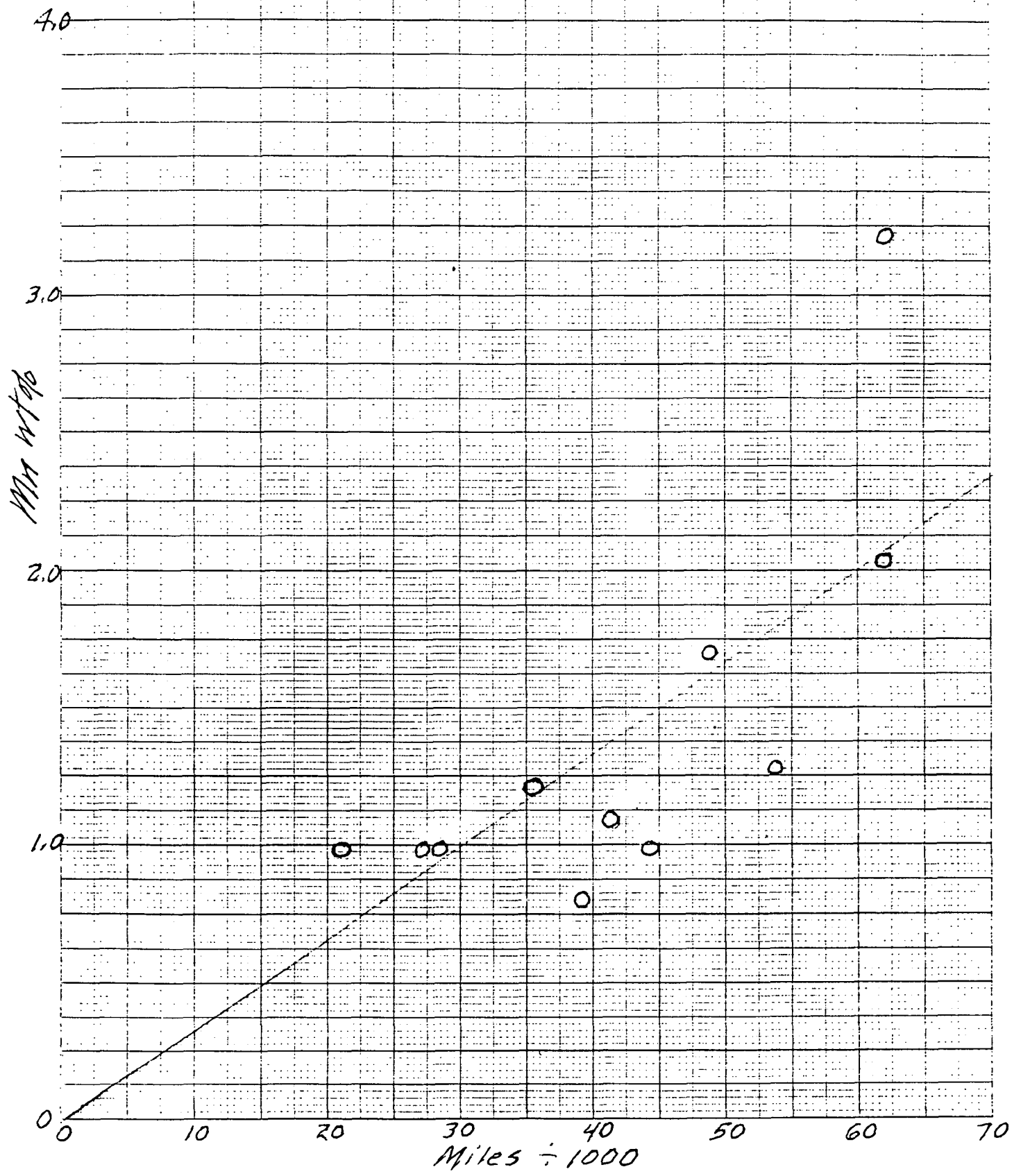
46 1320

K&E 10 X 10 TO 1 INCH
KEUFFEL & ESSER CO



Graph 2

11-Catalyst Fleet



46 1320

K&S 10 X 10 TO 1 INCH
KLUFFEL & ESSER CO. MADE IN U.S.A.

Graph 3

26-Catalyst Fleet

46 1320

Mr. Wtols

K-E 10 X 10 TO 1/2 INCH 25 INCH 100 INCH
NEUFEL & LESSER CO. MADE IN U.S.A.

4.0

3.0

2.0

1.0

0

10

20

30

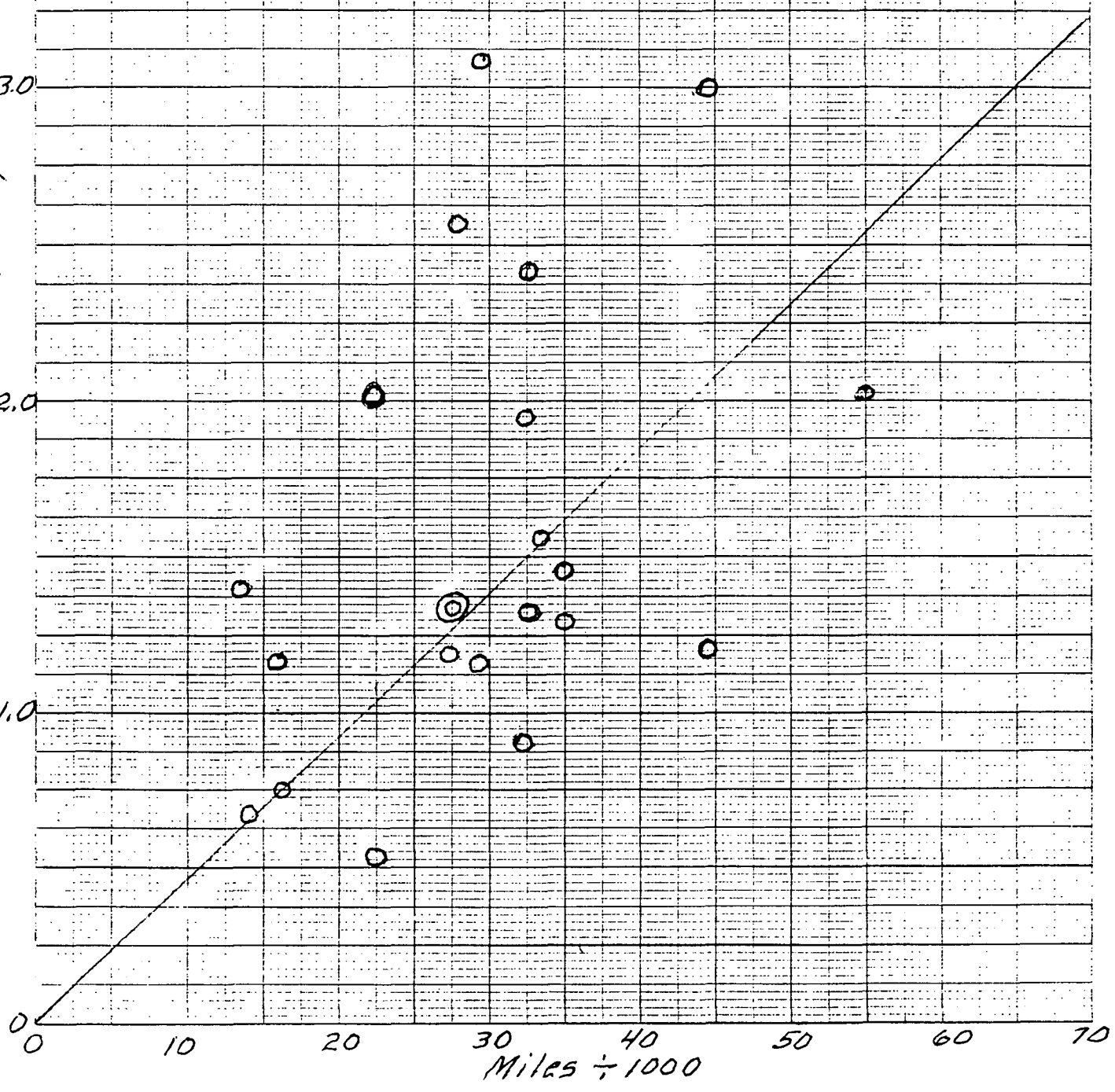
40

50

60

70

Miles ÷ 1000



Graph 4

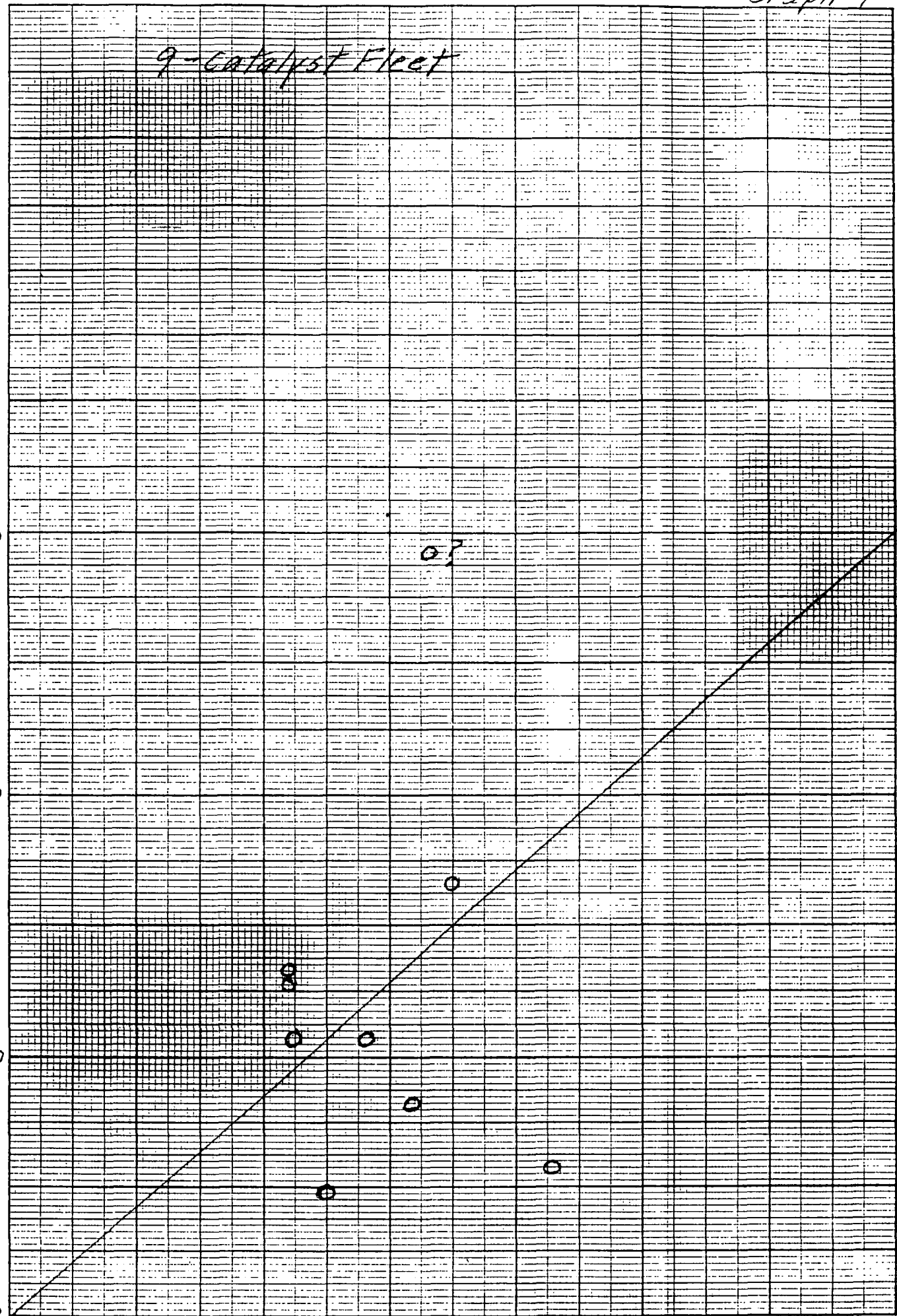
9-Catalyst Fleet

3.0

2.0

1.0

0



Miles + 1000

K&E 10 X 10 TO 1/2 INCH 46 1323
7 X 10 INCHES
MADE IN U.S.A.
KEUFFEL & ESSER CO.

Mn wt of

Graph 5

K-E 10 X 10 TO 1/2 INCH 46 1323
7 X 10 INCHES
MADE IN U.S.A.
KEUFFEL & ESSLER CO.

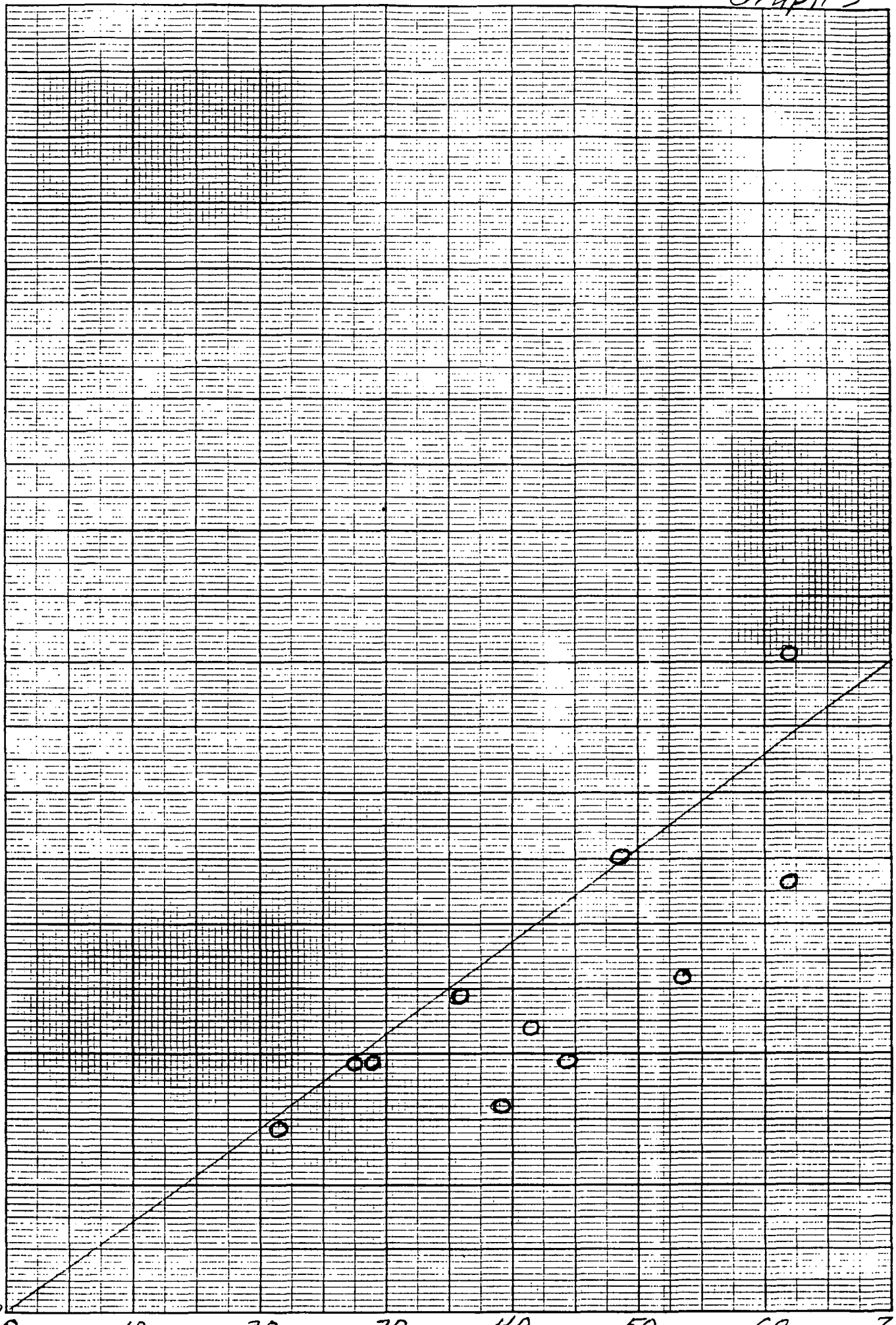
MM wtofo

3.0

2.0

1.0

1.0



Miles / 1000